

# MIKE 3 Flow Model FM

## Hydrodynamic and Transport Module

### Scientific Documentation



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## APPENDICES

### APPENDIX A – Governing equations in spherical coordinates

# 1 Introduction

This document presents the scientific background for the MIKE 3 Flow Model FM. The objective is to provide the user with a detailed description of the governing equations, numerical discretization and solution methods.

MIKE 3 Flow Model FM has been developed for applications within oceanographic, coastal and estuarine environments. The model is applicable to the study of a wide range of phenomena related to hydraulics wherever the three-dimensional flow structure is important

- tidal exchange and currents
- stratified flows at various scales (lakes, reservoirs, estuaries, regional oceans)
- oceanographic circulation
- heat and salt recirculation
- internal waves e.g. on the continental shelf
- jets and plumes, mixing, entrainment (e.g. cooling water, brine, waste water, sediment spill)

The model is based on the numerical solution of the three-dimensional incompressible Reynolds-averaged Navier-Stokes equations. Both the full 3D Navier-Stokes equations and the 3D shallow water equations can be applied. Thus, the model consists of continuity and momentum equations, and it is closed by a turbulent closure scheme. The free surface is taken into account using a sigma coordinate transformation approach. The spatial discretization of the governing equations in conserved form is performed using a cell-centered finite volume method. The time integration is performed using a semi-implicit scheme. The vertical convective and diffusion terms are discretized using an implicit scheme to remove the stability limitations associated with the vertical resolution. The remaining terms are discretized using either a first-order Euler method or a second-order explicit Runge-Kutta scheme. For the Navier-Stokes equations the projection method is employed for the non-hydrostatic pressure. The interface convective fluxes are calculated using an approximate Riemann solver. This shock-capturing scheme enables robust and stable simulation of flows involving shocks or discontinuities such as bores and hydraulic jumps.





## 2 Governing equations

The governing equations are solved in a sigma coordinate system or a combination of sigma coordinate system and a Cartesian coordinate system. For the hybrid system sigma coordinate is used from the free surface to a specified depth, and z-coordinate is used below. The most important advantage using sigma coordinate is the ability to accurately represent the bathymetry and provide consistent resolution near the bed. However, sigma coordinates can suffer from significant errors in the horizontal pressure gradients, advection and mixing terms in areas with sharp topographic changes (steep slopes). These errors can give rise to unrealistic flows. The use of z-level coordinate allows a simple calculation of the horizontal pressure gradients, advection and mixing terms, but the disadvantages are their inaccuracy in representing the bathymetry and that the stair-step representation of the bathymetry can result in unrealistic flow velocities near the bottom.

The governing equations can also be formulated in a spherical coordinate system. For more details, see Appendix A1.

### 2.1 Governing equations in a Cartesian coordinate system

#### 2.1.1 Navier-Stokes equations

The non-hydrostatic model is based on the incompressible Navier-Stokes equations subject to the assumptions of Boussinesq and with the free surface described by a height function. In a Cartesian coordinate system the local continuity equation is written as

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad (2.1)$$

and the conservative form of the momentum equation can be written

$$\begin{aligned} \frac{\partial u}{\partial t} + \frac{\partial u^2}{\partial x} + \frac{\partial vu}{\partial y} + \frac{\partial wu}{\partial z} \\ = fv - \frac{1}{\rho_0} \frac{\partial q}{\partial x} - g \frac{\partial \eta}{\partial x} - \frac{1}{\rho_0} \frac{\partial p_A}{\partial x} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial x} + F_u - F_{vx} + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial u}{\partial z} \right) \end{aligned} \quad (2.2)$$

$$\begin{aligned} \frac{\partial v}{\partial t} + \frac{\partial uv}{\partial x} + \frac{\partial v^2}{\partial y} + \frac{\partial wv}{\partial z} \\ = -fu - \frac{1}{\rho_0} \frac{\partial q}{\partial y} - g \frac{\partial \eta}{\partial y} - \frac{1}{\rho_0} \frac{\partial p_A}{\partial y} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial y} + F_v - F_{vy} + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial v}{\partial z} \right) \end{aligned} \quad (2.3)$$

$$\frac{\partial w}{\partial t} + \frac{\partial uw}{\partial x} + \frac{\partial vw}{\partial y} + \frac{\partial w^2}{\partial z} = -\frac{1}{\rho_0} \frac{\partial q}{\partial z} + F_w - F_{vz} + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial w}{\partial z} \right) \quad (2.4)$$

Here  $t$  is the time;  $x$ ,  $y$  and  $z$  are the Cartesian coordinates;  $\eta$  is the surface elevation;  $u$ ,  $v$  and  $w$  are the velocity components in the  $x$ ,  $y$  and  $z$  direction;  $q$  is the non-hydrostatic pressure;  $f = 2\Omega \sin \phi$  is the Coriolis parameter ( $\Omega$  is the angular rate of revolution and  $\phi$  the geographic latitude);  $\nu_t^v$  is the vertical eddy viscosity;  $g$  is the gravitational acceleration;  $p_A$  is the atmospheric pressure at the free surface;  $\rho$  is the density of water;  $\rho_0$  is the reference density of water;  $F_v = (F_{vx}, F_{vy}, F_{vz})$  is the drag force due to vegetation

(see section 4.4). Eqs. (2.2)-(2.4) are obtained by splitting the total pressure,  $p$ , into a non-hydrostatic and a hydrostatic component,  $p_H$ , where

$$p_H = p_A + \rho_0 g(\eta - z) + g \int_z^\eta (\rho - \rho_0) dz \quad (2.5)$$

The fluid is assumed to be incompressible. Hence, the density does not depend on the pressure, but only on the temperature,  $T$ , and the salinity,  $S$ , via the equation of state

$$\rho = \rho(T, S) \quad (2.6)$$

Here the UNESCO equation of state is used (see UNESCO, 1981).

The horizontal diffusion terms are described using a gradient-stress relation, which is simplified to

$$F_u = \frac{\partial}{\partial x} \left( 2\nu_t^h \frac{\partial u}{\partial x} \right) + \frac{\partial}{\partial y} \left( \nu_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \right) \quad (2.7)$$

$$F_v = \frac{\partial}{\partial x} \left( \nu_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \right) + \frac{\partial}{\partial y} \left( 2\nu_t^h \frac{\partial v}{\partial y} \right) \quad (2.8)$$

$$F_w = \frac{\partial}{\partial x} \left( \nu_t^h \frac{\partial w}{\partial x} \right) + \frac{\partial}{\partial y} \left( \nu_t^h \frac{\partial w}{\partial y} \right) \quad (2.9)$$

where  $\nu_t^h$  is the horizontal eddy viscosity.

The surface and bottom boundary conditions for  $u$ ,  $v$  and  $w$  are

at  $z = \eta$

$$\frac{\partial \eta}{\partial t} + u \frac{\partial \eta}{\partial x} + v \frac{\partial \eta}{\partial y} - w = 0, \quad \left( \frac{\partial u}{\partial z}, \frac{\partial v}{\partial z} \right) = \frac{1}{\rho_0 \nu_t^v} (\tau_{sx}, \tau_{sy}) \quad (2.10)$$

at  $z = -d$

$$u \frac{\partial d}{\partial x} + v \frac{\partial d}{\partial y} + w = 0, \quad \left( \frac{\partial u}{\partial z}, \frac{\partial v}{\partial z} \right) = \frac{1}{\rho_0 \nu_t^v} (\tau_{bx}, \tau_{by}) \quad (2.11)$$

Here  $d$  is the still water depth,  $(\tau_{bx}, \tau_{by})$  are the  $x$ - and  $y$ -components of the bottom stresses (see section 4.2), and  $(\tau_{sx}, \tau_{sy})$  are the  $x$ - and  $y$ -components of the surface stresses due to the wind (see section **Error! Reference source not found.** or ice coverage (see section 4.).

The total water depth,  $h = \eta + d$ , is obtained by vertical integration of the local continuity equation and taking into account the boundary condition at the surface and the bottom

$$\frac{\partial h}{\partial t} + \frac{\partial h \bar{u}}{\partial x} + \frac{\partial h \bar{v}}{\partial y} = 0 \quad (2.12)$$

Where  $\bar{u}$  and  $\bar{v}$  are the depth-averaged velocities

$$h\bar{u} = \int_{-d}^{\eta} u dz, \quad h\bar{v} = \int_{-d}^{\eta} v dz \quad (2.13)$$

In matrix form the continuity equation and the momentum equations may be written

$$\frac{\partial h}{\partial t} + \nabla \cdot \mathbf{F}^c = 0 \quad (2.14)$$

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}^m = \mathbf{S}_h + \mathbf{S}_q \quad (2.15)$$

Here  $\mathbf{F}^c = (F_x^c, F_y^c)^T = (h\bar{u}, h\bar{v})^T$ ,  $\mathbf{U} = (u, v, w)^T$  and  $\mathbf{F}^m = \mathbf{F}^{mc} - \mathbf{F}^{md} = (\mathbf{F}_x^m, \mathbf{F}_y^m, \mathbf{F}_z^m)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^{mc} = \begin{pmatrix} uu + g\eta \\ uv \\ uw \end{pmatrix} \quad \mathbf{F}_y^{mc} = \begin{pmatrix} uv \\ vv + g\eta \\ vw \end{pmatrix} \quad \mathbf{F}_z^{mc} = \begin{pmatrix} uw \\ vw \\ ww \end{pmatrix} \quad (2.16)$$

$$\mathbf{F}_x^{md} = \begin{pmatrix} 2v_t^h \frac{\partial u}{\partial x} \\ v_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ v_t^h \frac{\partial w}{\partial x} \end{pmatrix} \quad \mathbf{F}_y^{md} = \begin{pmatrix} v_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ 2v_t^h \frac{\partial v}{\partial y} \\ v_t^h \frac{\partial w}{\partial y} \end{pmatrix} \quad \mathbf{F}_z^{md} = \begin{pmatrix} v_t^v \frac{\partial u}{\partial z} \\ v_t^v \frac{\partial v}{\partial z} \\ v_t^v \frac{\partial w}{\partial z} \end{pmatrix} \quad (2.17)$$

$$\mathbf{S}_h = \begin{pmatrix} fv - \frac{1}{\rho_0} \frac{\partial p_A}{\partial x} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial x} - F_{vx} \\ -fu - \frac{1}{\rho_0} \frac{\partial p_A}{\partial y} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial y} - F_{vy} \\ -F_{vz} \end{pmatrix} \quad \mathbf{S}_q = -\frac{1}{\rho_0} \begin{pmatrix} \frac{\partial q}{\partial x} \\ \frac{\partial q}{\partial y} \\ \frac{\partial q}{\partial w} \end{pmatrix} \quad (2.18)$$

### 2.1.2 Shallow water equations

If the hydrostatic pressure assumption is applied, the non-hydrostatic pressure will be zero. With this assumption, a three-dimensional, hydrodynamic model can be significantly simplified because the momentum equation in the vertical direction (Eq. (2.4)) can be neglected.

In matrix form the continuity equations and the momentum equations may be written

$$\frac{\partial h}{\partial t} + \nabla \cdot \mathbf{F}^c = 0 \quad (2.19)$$

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F}^m = \mathbf{S}_h \quad (2.20)$$

Here  $\mathbf{F}^c = (F_x^c, F_y^c)^T = (h\bar{u}, h\bar{v})^T$ ,  $\mathbf{U} = (u, v)^T$  and  $\mathbf{F}^m = \mathbf{F}^{mc} - \mathbf{F}^{md} = (\mathbf{F}_x^m, \mathbf{F}_y^m, \mathbf{F}_z^m)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^{mc} = \begin{pmatrix} uu + g\eta \\ uv \end{pmatrix} \quad \mathbf{F}_y^{mc} = \begin{pmatrix} uv \\ vv + g\eta \end{pmatrix} \quad \mathbf{F}_z^{mc} = \begin{pmatrix} uw \\ vw \end{pmatrix} \quad (2.21)$$

$$\mathbf{F}_x^{md} = \begin{pmatrix} 2v_t^h \frac{\partial u}{\partial x} \\ v_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \end{pmatrix} \quad \mathbf{F}_y^{md} = \begin{pmatrix} v_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ 2v_t^h \frac{\partial v}{\partial y} \end{pmatrix} \quad \mathbf{F}_z^{md} = \begin{pmatrix} v_t^v \frac{\partial u}{\partial z} \\ v_t^v \frac{\partial v}{\partial z} \end{pmatrix} \quad (2.22)$$

$$\mathbf{S}_h = \begin{pmatrix} fv - \frac{1}{\rho_0} \frac{\partial p_A}{\partial x} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial x} - F_{vx} \\ -fu - \frac{1}{\rho_0} \frac{\partial p_A}{\partial y} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial y} - F_{vy} \end{pmatrix} \quad (2.23)$$

### 2.1.3 Transport equations for temperature and salinity

The transport of temperature,  $T$ , and salinity,  $S$ , follows the general transport-diffusion equation as

$$\frac{\partial T}{\partial t} + \frac{\partial uT}{\partial x} + \frac{\partial vT}{\partial y} + \frac{\partial wT}{\partial z} = F_t + \frac{\partial}{\partial z} \left( D_{ts}^v \frac{\partial T}{\partial z} \right) + \hat{H} \quad (2.24)$$

$$\frac{\partial S}{\partial t} + \frac{\partial uS}{\partial x} + \frac{\partial vS}{\partial y} + \frac{\partial wS}{\partial z} = F_s + \frac{\partial}{\partial z} \left( D_{ts}^v \frac{\partial S}{\partial z} \right) \quad (2.25)$$

where  $D_{ts}^v$  is the vertical turbulent (eddy) diffusion coefficient and  $\hat{H}$  is a source term due to heat exchange with the atmosphere (see section 4.11).  $F_t$  and  $F_s$  are the horizontal diffusion terms defined by

$$F_t = \frac{\partial}{\partial x} \left( D_{ts}^h \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( D_{ts}^h \frac{\partial T}{\partial y} \right) \quad (2.26)$$

$$F_s = \frac{\partial}{\partial x} \left( D_{ts}^h \frac{\partial S}{\partial x} \right) + \frac{\partial}{\partial y} \left( D_{ts}^h \frac{\partial S}{\partial y} \right) \quad (2.27)$$

where  $D_{ts}^h$  is the horizontal turbulent (eddy) diffusion coefficient. The horizontal and vertical diffusion coefficients can be a constant value or determined as the scaled eddy viscosity.

At the surface, the boundary conditions for the temperature and salinity are

at  $z = \eta$

$$D_{ts}^v \frac{\partial T}{\partial z} = \frac{Q_n}{\rho_0 c_p} \quad \frac{\partial S}{\partial z} = 0 \quad (2.28)$$

At the seabed the boundary conditions are

at  $z = -d$

$$\frac{\partial T}{\partial z} = 0 \quad \frac{\partial S}{\partial z} = 0 \quad (2.29)$$

Here  $Q_n$  is the surface net heat flux and  $c_p = 4217 \text{ J/(kg}^\circ\text{K)}$  is the specific heat of the water. A detailed description for determination of  $\hat{H}$  and  $Q_n$  is given in Section 4.12.

In matrix form the transport equations for  $T$  and  $s$  may be written

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.30)$$

where  $\mathbf{U} = (T, S)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_z)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^c = \begin{pmatrix} uT \\ uS \end{pmatrix} \quad \mathbf{F}_y^c = \begin{pmatrix} vT \\ vS \end{pmatrix} \quad \mathbf{F}_z^c = \begin{pmatrix} wT \\ wS \end{pmatrix} \quad (2.31)$$

$$\mathbf{F}_x^d = \begin{pmatrix} D_{ts}^h \frac{\partial T}{\partial x} \\ D_{ts}^h \frac{\partial S}{\partial x} \end{pmatrix} \quad \mathbf{F}_y^d = \begin{pmatrix} D_{ts}^h \frac{\partial T}{\partial y} \\ D_{ts}^h \frac{\partial S}{\partial y} \end{pmatrix} \quad \mathbf{F}_z^d = \begin{pmatrix} D_{ts}^v \frac{\partial T}{\partial z} \\ D_{ts}^v \frac{\partial S}{\partial z} \end{pmatrix} \quad (2.32)$$

$$\mathbf{S} = \begin{pmatrix} \hat{H} \\ 0 \end{pmatrix} \quad (2.33)$$

#### 2.1.4 Turbulence model

The turbulence is modelled using an eddy viscosity concept. The eddy viscosity can be described using empirical formula (see section 4.1) or solving a turbulence closure model. In the MIKE 3 Flow Model FM, there are two turbulence models available, namely the  $k$ - $\varepsilon$  model and the  $k$ - $\omega$  model; both are two-equations models. The  $k$ - $\varepsilon$  turbulence model can be used with both the Navier-Stokes equations and the shallow water equations. The  $k$ - $\omega$  turbulence model can only be used with the Navier-Stokes equations.

##### The k-epsilon model

The  $k$ - $\varepsilon$  model presented here follows Rodi (1980,1984) and has an additional limiter from Larsen and Fuhrman (2018). The model describes  $k$ , the specific turbulent kinetic energy and  $\varepsilon$ , the dissipation rate of turbulent kinetic energy (turbulent dissipation). The eddy viscosity,  $\nu_t$ , is defined as

$$\nu_t = c_\mu \frac{k^2}{\tilde{\varepsilon}} \quad (2.34)$$

where  $c_\mu$  is an empirical constant and  $\tilde{\varepsilon}$  is a limited version of  $\varepsilon$ . Solving a system of equations for  $k$  and  $\varepsilon$  results in the eddy viscosity in eq. (2.34) and this value can be used in the momentum equations for the horizontal and/or vertical eddy viscosity,  $\nu_t^h$  and  $\nu_t^v$ .

The turbulent kinetic energy,  $k$ , and the turbulent dissipation,  $\varepsilon$ , are obtained from the following transport equations.

$$\frac{\partial k}{\partial t} + \frac{\partial uk}{\partial x} + \frac{\partial vk}{\partial y} + \frac{\partial wk}{\partial z} = F_k + \frac{\partial}{\partial z} \left( \frac{\nu_{t0}^v}{\sigma_k^v} \frac{\partial k}{\partial z} \right) + P_k + B_k - \varepsilon \quad (2.35)$$

$$\frac{\partial \varepsilon}{\partial t} + \frac{\partial u\varepsilon}{\partial x} + \frac{\partial v\varepsilon}{\partial y} + \frac{\partial w\varepsilon}{\partial z} = F_\varepsilon + \frac{\partial}{\partial z} \left( \frac{\nu_{t0}^v}{\sigma_\varepsilon^v} \frac{\partial \varepsilon}{\partial z} \right) + P_\varepsilon + B_\varepsilon - c_{2\varepsilon} \frac{\varepsilon^2}{k} \quad (2.36)$$

Here,  $P_k$  and  $P_\varepsilon$  are production terms,  $B_k$  and  $B_\varepsilon$  are buoyancy production terms and  $F_k$  and  $F_\varepsilon$  are horizontal diffusion terms. The details of the various terms are presented in the following.

The production terms are given as

$$P_k = \nu_t p_0 + c_{fk} P_v \quad (2.37)$$

$$P_\varepsilon = c_{1\varepsilon} c_\mu k p_0 + c_{f\varepsilon} \frac{\tilde{\varepsilon}}{k} P_v \quad (2.38)$$

where,  $c_{1\varepsilon}$  is a closure coefficient. Furthermore,

$$p_0 = 2 \sum_{i=1}^3 \sum_{j=1}^3 S_{ij} S_{ij} \quad (2.39)$$

where  $S_{ij}$  is the mean strain rate tensor defined as

$$S_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right), \text{ for } i, j = 1, 2, 3 \quad (2.40)$$

Here, is used the following notation

$$u_1 = u, \quad u_2 = v, \quad u_3 = w \quad (2.41)$$

$$x_1 = x, \quad x_2 = y, \quad x_3 = z \quad (2.42)$$

For the shallow water equations, it is assumed the horizontal gradients are much smaller than the vertical gradients and the following approximation is made.

$$p_0 \approx \left( \frac{\partial u}{\partial z} \right)^2 + \left( \frac{\partial v}{\partial z} \right)^2 \quad (2.43)$$

$P_v$  is the production term due to vegetation and  $c_{fk}$  and  $c_{f\varepsilon}$  are two weighting coefficients (see section 4.4).

The buoyancy production terms are given as

$$B_k = \nu_t p_b \quad (2.44)$$

$$B_\varepsilon = c_{3\varepsilon} c_\mu k p_b \quad (2.45)$$

where  $c_{3\varepsilon}$  is a closure coefficient and  $p_b$  is defined from the Brunt-Väisälä frequency  $N$  as

$$p_b = -\frac{1}{\sigma_t} N^2, \quad N^2 = -\frac{g}{\rho_0} \frac{\partial \rho}{\partial z} \quad (2.46)$$

Here,  $\sigma_t$  is the turbulent Prandtl number. The Prandtl number can be modified explicitly following the empirical expression of Munk and Anderson (1948) (see section 4.1).

The vertical diffusion terms are given directly in the transport equations for  $k$  and  $\varepsilon$ . The horizontal diffusion terms have a similar form and are given by

$$F_k = \frac{\partial}{\partial x} \left( \frac{\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \right) \quad (2.47)$$

$$F_\varepsilon = \frac{\partial}{\partial x} \left( \frac{\nu_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{\nu_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial y} \right) \quad (2.48)$$

The coefficients  $\sigma_k^h$ ,  $\sigma_k^v$ ,  $\sigma_\varepsilon^h$  and  $\sigma_\varepsilon^v$  are closure coefficients. For the diffusion terms is used an unlimited version of the eddy viscosity

$$\nu_{t0}^h = c_\mu \frac{k^2}{\varepsilon}, \quad \nu_{t0}^v = c_\mu \frac{k^2}{\varepsilon} \quad (2.49)$$

If the momentum equations use an empirical formula for either the horizontal or vertical eddy viscosity, that value is also used in the diffusion terms in the turbulence model. This means, that  $\nu_{t0}^h = \nu_t^h$  or  $\nu_{t0}^v = \nu_t^v$  is used instead of the corresponding expression in eq. (2.49).

To limit the eddy viscosity in regions with nearly-potential flow and stabilize the model, Larsen and Fuhrman (2018) introduced a limited value of the turbulent dissipation  $\varepsilon$ ,

$$\tilde{\varepsilon} = \max \left[ \varepsilon, \lambda_2 \frac{c_{2\varepsilon} p_0}{c_{1\varepsilon} p_\Omega} \varepsilon \right] \quad (2.50)$$

Here,  $\lambda_2 = 0.05$  is a limiter coefficient and

$$p_\Omega = 2 \sum_{i=1}^3 \sum_{j=1}^3 \Omega_{ij} \Omega_{ij} \quad (2.51)$$

where  $\Omega_{ij}$  is the rotation tensor,

$$\Omega_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right), \quad \text{for } i, j = 1, 2, 3 \quad (2.52)$$

For the shallow water equations, the value  $\lambda_2 = 0$  is used, corresponding to no limiter.

Several carefully calibrated empirical coefficients enter the  $k$ - $\varepsilon$  turbulence model. In the standard  $k$ - $\varepsilon$  model (Rodi (1984)), they are

$$c_\mu = 0.09, \quad c_{1\varepsilon} = 1.44, \quad c_{2\varepsilon} = 1.92, \quad c_{3\varepsilon} = 0 \quad (2.53)$$

$$\sigma_t = 0.9, \quad \sigma_k^h = \sigma_k^v = 1.0, \quad \sigma_\varepsilon^h = \sigma_\varepsilon^v = 1.3 \quad (2.54)$$

In matrix form, the transport equations for  $k$  and  $\varepsilon$  may be written

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.55)$$

where  $\mathbf{U} = (k, \varepsilon)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_z)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^c = \begin{pmatrix} uk \\ u\varepsilon \end{pmatrix}, \quad \mathbf{F}_y^c = \begin{pmatrix} vk \\ v\varepsilon \end{pmatrix}, \quad \mathbf{F}_z^c = \begin{pmatrix} wk \\ w\varepsilon \end{pmatrix} \quad (2.56)$$

$$\mathbf{F}_x^d = \begin{pmatrix} \frac{v_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \\ \frac{v_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial x} \end{pmatrix}, \quad \mathbf{F}_y^d = \begin{pmatrix} \frac{v_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \\ \frac{v_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial y} \end{pmatrix}, \quad \mathbf{F}_z^d = \begin{pmatrix} \frac{v_{t0}^v}{\sigma_k^v} \frac{\partial k}{\partial z} \\ \frac{v_{t0}^v}{\sigma_\varepsilon^v} \frac{\partial \varepsilon}{\partial z} \end{pmatrix} \quad (2.57)$$

$$\mathbf{S} = \begin{pmatrix} P_k + B_k - \varepsilon \\ P_\varepsilon + B_\varepsilon - c_{2\varepsilon} \frac{\varepsilon^2}{k} \end{pmatrix} \quad (2.58)$$

## The k-omega model

The  $k$ - $\omega$  model presented here is following Larsen and Fuhrman (2018). It extends the model in Wilcox (2008) with a buoyancy term and an additional limiter. The model describes the specific turbulent kinetic energy,  $k$ , and the specific dissipation rate,  $\omega$ . The eddy viscosity,  $\nu_t$ , is defined as

$$\nu_t = \frac{k}{\tilde{\omega}} \quad (2.59)$$

where  $\tilde{\omega}$  is a limited version of  $\omega$ . This value of the eddy viscosity can be used in the momentum equations for the horizontal and/or vertical eddy viscosity,  $\nu_t^h$  and  $\nu_t^v$ .

The transport equations for the turbulent kinetic energy,  $k$ , and the specific dissipation rate,  $\omega$ , reads

$$\frac{\partial k}{\partial t} + \frac{\partial uk}{\partial x} + \frac{\partial vk}{\partial y} + \frac{\partial wk}{\partial z} = F_k + \frac{\partial}{\partial z} \left( \frac{v_{t0}^v}{\sigma_k^v} \frac{\partial k}{\partial z} \right) + P_k + B_k - \beta_k \omega k \quad (2.60)$$

$$\frac{\partial \omega}{\partial t} + \frac{\partial u\omega}{\partial x} + \frac{\partial v\omega}{\partial y} + \frac{\partial w\omega}{\partial z} = F_\omega + \frac{\partial}{\partial z} \left( \frac{v_{t0}^v}{\sigma_\omega^v} \frac{\partial \omega}{\partial z} \right) + F_{\omega c} + P_\omega - \beta_\omega \omega^2 \quad (2.61)$$

Here,  $F_k$  and  $F_\omega$  are horizontal diffusion terms,  $F_{\omega c}$  is a cross-diffusion term,  $P_k$  and  $P_\omega$  are production terms and  $B_k$  is buoyancy production. The details of the various terms are presented in the following.

The production terms are given by

$$P_k = \nu_t p_0 + c_{fk} P_v \quad (2.62)$$

$$P_\omega = \alpha \frac{\omega}{\tilde{\omega}} p_0 + \frac{c_{f\omega}}{\nu_t} P_v \quad (2.63)$$

where  $\tilde{\omega}$  is a limited version of the specific dissipation rate,  $\omega$ ,  $\alpha$  is a closure coefficient and  $p_0$  was defined in eq. (2.39). The buoyancy production  $B_k$  is defined in the same way as for the  $k$ - $\varepsilon$  model, see eq. (2.44), (2.46). Again, it depends on the Prandtl number  $\sigma_t$ .  $P_v$  is the production term due to vegetation and  $c_{fk}$  and  $c_{f\omega}$  are two weighting coefficients (see section 4.4).

The vertical diffusion terms are given directly in the transport equations for  $k$  and  $\omega$ . The horizontal diffusion terms have a similar form and are given by

$$F_k = \frac{\partial}{\partial x} \left( \frac{v_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{v_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \right) \quad (2.64)$$



$$F_{\omega} = \frac{\partial}{\partial x} \left( \frac{\nu_{t0}^h}{\sigma_{\omega}^h} \frac{\partial \omega}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{\nu_{t0}^h}{\sigma_{\omega}^h} \frac{\partial \omega}{\partial y} \right) \quad (2.65)$$

The coefficients  $\sigma_k^h$ ,  $\sigma_k^v$ ,  $\sigma_{\omega}^h$  and  $\sigma_{\omega}^v$  are closure coefficients. For the diffusion terms is used an unlimited version of the eddy viscosity

$$\nu_{t0}^h = \frac{k}{\omega}, \quad \nu_{t0}^v = \frac{k}{\omega} \quad (2.66)$$

If the momentum equations use an empirical formula for either the horizontal or vertical eddy viscosity, that value is also used in the diffusion terms in the turbulence model. This means, that  $\nu_{t0}^h = \nu_t^h$  or  $\nu_{t0}^v = \nu_t^v$  is used instead of the corresponding expression in eq. (2.66). The cross-diffusion term in the equation for  $\omega$  reads

$$F_{\omega c} = \frac{\sigma_{do}}{\omega} \max \left\{ 0, \frac{\partial k}{\partial x} \frac{\partial \omega}{\partial x} + \frac{\partial k}{\partial y} \frac{\partial \omega}{\partial y} + \frac{\partial k}{\partial z} \frac{\partial \omega}{\partial z} \right\} \quad (2.67)$$

To limit the eddy viscosity in regions with nearly-potential flow and stabilize the model, Larsen and Fuhrman (2018) introduced an additional limiter for  $\omega$  on top of the limiter already present in the  $k$ - $\omega$  model from Wilcox (2008). The limited versions of  $\omega$  are defined as

$$\hat{\omega} = \max \left[ \omega, \lambda_1 \sqrt{\frac{p_0 - p_b}{\beta_k}} \right] \quad (2.68)$$

$$\tilde{\omega} = \max \left[ \hat{\omega}, \lambda_2 \frac{\beta_{\omega}}{\beta_k \alpha} \frac{p_0}{p_{\Omega}} \omega \right] \quad (2.69)$$

The values of the limiter coefficients are  $\lambda_1 = 0.875$  and  $\lambda_2 = 0.05$  and  $p_{\Omega}$  was defined in eq. (2.51).

The system contains several empirically determined closure coefficients which have the following values,

$$\sigma_k^h = \sigma_k^v = \frac{5}{3}, \quad \sigma_{\omega}^h = \sigma_{\omega}^v = 2, \quad \sigma_{do} = \frac{1}{8} \quad (2.70)$$

$$\alpha = 0.52, \quad \sigma_t = 0.7 \quad (2.71)$$

$$\beta_k = 0.09, \quad \beta_{\omega} = \beta_0 f_{\beta}, \quad \beta_0 = 0.0708 \quad (2.72)$$

$$f_{\beta} = \frac{1 + 85\chi_{\omega}}{1 + 100\chi_{\omega}}, \quad \chi_{\omega} = \left| \frac{\sum_{i=1}^3 \sum_{j=1}^3 \sum_{k=1}^3 \Omega_{ij} \Omega_{jk} S_{ki}}{(\beta_k \omega)^3} \right| \quad (2.73)$$

These values are from Larsen and Fuhrmann (2018), except  $f_{\beta}$  which is from Wilcox (2008). Larsen and Fuhrman (2018) use  $f_{\beta} = 1$ , consistent with two-dimensional flow. Note that  $\beta_k$  corresponds to  $c_{\mu}$  in the  $k$ - $\varepsilon$  model. The mean strain rate tensor  $S_{ij}$  and the rotation tensor  $\Omega_{ij}$  were defined in eq. (2.40) and (2.52).

In matrix form, the transport equations for  $k$  and  $\omega$  may be written as

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F} - \mathbf{G} = \mathbf{S} \quad (2.74)$$

where  $\mathbf{U} = (k, \omega)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_z)^T$ . The flux components  $\mathbf{F}$ , the cross-diffusion  $\mathbf{G}$  and the source terms  $\mathbf{S}$  can be written

$$\mathbf{F}_x^c = \begin{pmatrix} uk \\ u\omega \end{pmatrix}, \quad \mathbf{F}_y^c = \begin{pmatrix} vk \\ v\omega \end{pmatrix}, \quad \mathbf{F}_z^c = \begin{pmatrix} wk \\ w\omega \end{pmatrix} \quad (2.75)$$

$$\mathbf{F}_x^d = \begin{pmatrix} \frac{\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \\ \frac{\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial x} \end{pmatrix}, \quad \mathbf{F}_y^d = \begin{pmatrix} \frac{\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \\ \frac{\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial y} \end{pmatrix}, \quad \mathbf{F}_z^d = \begin{pmatrix} \frac{\nu_{t0}^v}{\sigma_k^v} \frac{\partial k}{\partial z} \\ \frac{\nu_{t0}^v}{\sigma_\omega^v} \frac{\partial \omega}{\partial z} \end{pmatrix} \quad (2.76)$$

$$\mathbf{G} = \begin{pmatrix} \sigma_d \\ \omega \end{pmatrix} \max \left[ 0, \frac{\partial k}{\partial x} \frac{\partial \omega}{\partial x} + \frac{\partial k}{\partial y} \frac{\partial \omega}{\partial y} + \frac{\partial k}{\partial z} \frac{\partial \omega}{\partial z} \right] \quad (2.77)$$

$$\mathbf{S} = \begin{pmatrix} P_k + B_k - \beta_k \omega k \\ P_\omega - \beta_\omega \omega^2 \end{pmatrix} \quad (2.78)$$

### Boundary conditions at the surface and the seabed

At boundaries where there is a friction, the boundary conditions for  $k$ ,  $\varepsilon$  and  $\omega$  can be modelled with wall functions, Wilcox (1998),

$$k = \frac{1}{\sqrt{\beta_k}} U_\tau^2, \quad \varepsilon = \frac{U_\tau^3}{\kappa \Delta y}, \quad \omega = \frac{U_\tau}{\sqrt{\beta_k} \kappa \Delta y} \quad (2.79)$$

Here,  $U_\tau$  is the friction velocity associated with the boundary and  $\Delta y$  is the distance from the boundary to the point where the conditions are employed. Furthermore,  $\kappa = 0.41$  is the von Kármán constant.

At the seabed,  $z = -d$ , if there is a bed resistance, the boundary conditions are the wall functions in eq. (2.79) where  $\Delta y = \Delta z_b$  is the distance to the bottom and  $U_\tau = U_{\tau b}$  is the friction velocity associated with the bottom stress, see section 4.2.

At the surface,  $z = \eta$ , if there is a friction,  $U_{\tau s} > 0$ , the boundary conditions are the wall functions in eq. (2.79) where  $\Delta y = \Delta z_s$  is the distance to the surface and  $U_\tau = U_{\tau s}$  is the friction velocity associated with the surface stress, see section **Error! Reference source not found.** and 4.6. If there is no surface friction, the boundary conditions are

at  $z = \eta$

$$\frac{\partial k}{\partial z} = 0, \quad \varepsilon = \frac{(k \sqrt{c_\mu})^{3/2}}{\alpha_s \kappa h}, \quad \omega = \frac{\sqrt{k}}{\alpha_s \beta_k^{1/4} \kappa h} \quad \text{for } U_{\tau s} = 0 \quad (2.80)$$

where  $\alpha_s = 0.07$  is an empirical constant.

### 2.1.5 Transport equation for a scalar quantity

The conservation equation for a scalar quantity is given by

$$\frac{\partial C}{\partial t} + \frac{\partial uC}{\partial x} + \frac{\partial vC}{\partial y} + \frac{\partial wC}{\partial z} = F_c + \frac{\partial}{\partial z} \left( D_c^v \frac{\partial C}{\partial z} \right) - k_p C \quad (2.81)$$

where  $C$  is the concentration of the scalar quantity,  $k_p$  is the linear decay rate of the scalar quantity and  $D_c^v$  is the vertical turbulent (eddy) diffusion coefficient.  $F_c$  is the horizontal diffusion terms defined by

$$F_c = \frac{\partial}{\partial x} \left( D_c^h \frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial y} \left( D_c^h \frac{\partial C}{\partial y} \right) \quad (2.82)$$

where  $D_c^h$  is the horizontal turbulent (eddy) diffusion coefficient. The horizontal and vertical diffusion coefficients can be a constant value or determined as the scaled eddy viscosity.

The surface and bottom boundary conditions for  $C$  are

at  $z = \eta$

$$\frac{\partial C}{\partial z} = 0 \quad (2.83)$$

at  $z = -d$

$$\frac{\partial C}{\partial z} = 0 \quad (2.84)$$

In matrix form the transport equations for  $C$  may be written

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.85)$$

Where  $\mathbf{U} = (C)$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_z)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^c = (uC) \quad \mathbf{F}_y^c = (vC) \quad \mathbf{F}_z^c = (wC) \quad (2.86)$$

$$\mathbf{F}_x^d = \left( D_c^h \frac{\partial C}{\partial x} \right) \quad \mathbf{F}_y^d = \left( D_c^h \frac{\partial C}{\partial y} \right) \quad \mathbf{F}_z^d = \left( D_c^v \frac{\partial C}{\partial z} \right) \quad (2.87)$$

$$\mathbf{S} = -(k_p C) \quad (2.88)$$

## 2.2 Governing equations in a sigma coordinate system

The equations are solved using a vertical  $\sigma$ -transformation

$$t' = t, \quad x' = x, \quad y' = y, \quad \sigma = \frac{z + d}{h} \quad (2.89)$$

where  $\sigma$  varies between 0 at the bottom and 1 at the surface. The chain rule is applied to obtain partial derivatives of the function  $f = f(t, x, y, z)$

$$\frac{\partial f}{\partial t} = \frac{\partial f}{\partial t'} + \frac{\partial f}{\partial \sigma} \frac{\partial \sigma}{\partial t} \quad (2.90)$$

$$\frac{\partial f}{\partial x} = \frac{\partial f}{\partial x'} + \frac{\partial f}{\partial \sigma} \frac{\partial \sigma}{\partial x} \quad (2.91)$$

$$\frac{\partial f}{\partial y} = \frac{\partial f}{\partial y'} + \frac{\partial f}{\partial \sigma} \frac{\partial \sigma}{\partial y} \quad (2.92)$$

$$\frac{\partial f}{\partial z} = \frac{\partial f}{\partial \sigma} \frac{\partial \sigma}{\partial z} \quad (2.93)$$

where

$$\frac{\partial \sigma}{\partial t} = -\sigma \frac{1}{h} \frac{\partial h}{\partial t} \equiv A_t \quad (2.94)$$

$$\frac{\partial \sigma}{\partial x} = -\frac{1}{h} \left( \sigma \frac{\partial h}{\partial x} - \frac{\partial d}{\partial x} \right) \equiv A_x \quad (2.95)$$

$$\frac{\partial \sigma}{\partial y} = -\frac{1}{h} \left( \sigma \frac{\partial h}{\partial y} - \frac{\partial d}{\partial y} \right) \equiv A_y \quad (2.96)$$

$$\frac{\partial \sigma}{\partial z} = \frac{1}{h} \equiv A_z \quad (2.97)$$

## 2.2.1 Navier-Stokes equations

In the sigma coordinate system, the governing equations are given as

$$\frac{\partial h}{\partial t'} + \frac{\partial hu}{\partial x'} + \frac{\partial hv}{\partial y'} + \frac{\partial h\omega}{\partial \sigma} = 0 \quad (2.98)$$

$$\frac{\partial hu}{\partial t'} + \frac{\partial hu^2}{\partial x'} + \frac{\partial hvu}{\partial y'} + \frac{\partial h\omega u}{\partial \sigma} = \quad (2.99)$$

$$fhv - \frac{h}{\rho_0} \left( \frac{\partial q}{\partial x'} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial x} \right) - gh \frac{\partial \eta}{\partial x'} + hF_u - hF_{vx} + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial u}{\partial \sigma} \right)$$

$$\frac{\partial hv}{\partial t'} + \frac{\partial huv}{\partial x'} + \frac{\partial hv^2}{\partial y'} + \frac{\partial h\omega v}{\partial \sigma} = \quad (2.100)$$

$$-fhu - \frac{h}{\rho_0} \left( \frac{\partial q}{\partial y'} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial y} \right) - gh \frac{\partial \eta}{\partial y'} + hF_v - hF_{vy} + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial v}{\partial \sigma} \right)$$

$$\frac{\partial h\omega}{\partial t'} + \frac{\partial hu\omega}{\partial x'} + \frac{\partial hv\omega}{\partial y'} + \frac{\partial h\omega\omega}{\partial \sigma} = -\frac{1}{\rho_0} \frac{\partial q}{\partial \sigma} + hF_w - hF_{vz} + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial \omega}{\partial \sigma} \right) \quad (2.101)$$

The modified vertical velocity,  $\omega$ , in the sigma coordinate system is given by

$$\omega = \frac{1}{h} \left( w + u \frac{\partial d}{\partial x} + v \frac{\partial d}{\partial y} - \sigma \left( \frac{\partial h}{\partial t} + u \frac{\partial h}{\partial x} + v \frac{\partial h}{\partial y} \right) \right) \quad (2.102)$$

The modified vertical velocity is the velocity across a level of constant  $\sigma$ . The horizontal diffusion terms are approximated by

$$hF_u \approx \frac{\partial}{\partial x} \left( 2h\nu_t^h \frac{\partial u}{\partial x} \right) + \frac{\partial}{\partial y} \left( h\nu_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \right) \quad (2.103)$$

$$hF_v \approx \frac{\partial}{\partial x} \left( h\nu_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \right) + \frac{\partial}{\partial y} \left( 2h\nu_t^h \frac{\partial v}{\partial y} \right) \quad (2.104)$$

$$hF_w \approx \frac{\partial}{\partial x} \left( h\nu_t^h \frac{\partial w}{\partial x} \right) + \frac{\partial}{\partial y} \left( h\nu_t^h \frac{\partial w}{\partial y} \right) \quad (2.105)$$

The surface and bottom boundary conditions for  $u$ ,  $v$  and  $\omega$  are

at  $z = \eta$

$$\omega = 0, \quad \left( \frac{\partial u}{\partial \sigma}, \frac{\partial v}{\partial \sigma} \right) = \frac{h}{\rho_0 \nu_t^v} (\tau_{sx}, \tau_{sy}) \quad (2.106)$$

at  $z = -d$

$$\omega = 0, \quad \left( \frac{\partial u}{\partial \sigma}, \frac{\partial v}{\partial \sigma} \right) = \frac{h}{\rho_0 \nu_t^v} (\tau_{bx}, \tau_{by}) \quad (2.107)$$

The depth-averaged continuity equation becomes

$$\frac{\partial h}{\partial t'} + \frac{\partial h\bar{u}}{\partial x'} + \frac{\partial h\bar{v}}{\partial y'} = 0 \quad (2.108)$$

where  $\bar{u}$  and  $\bar{v}$  are the depth-averaged velocities

$$\bar{u} = \int_0^1 u d\sigma, \quad \bar{v} = \int_0^1 v d\sigma = 0 \quad (2.109)$$

In matrix form the continuity equations and the momentum equations may be written

$$\frac{\partial h}{\partial t'} + \nabla \cdot \mathbf{F}^c = 0 \quad (2.110)$$

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F}^m = \mathbf{S}_h + \mathbf{S}_q \quad (2.111)$$

where  $\mathbf{F}^c = (F_x^c, F_y^c)^T = (h\bar{u}, h\bar{v})^T$ ,  $\mathbf{U} = (hu, hv, hw)^T$  and  $\mathbf{F}^m = \mathbf{F}^{mc} - \mathbf{F}^{md} = (\mathbf{F}_x^m, \mathbf{F}_y^m, \mathbf{F}_\sigma^m)^T$ .

The flux components and the source terms can be written

$$\mathbf{F}_x^{mc} = \begin{pmatrix} hu u + \frac{1}{2}g(\eta^2 + 2\eta d) \\ huv \\ huw \end{pmatrix} \quad \mathbf{F}_y^{mc} = \begin{pmatrix} h v v + \frac{1}{2}g(\eta^2 + 2\eta d) \\ hvv \\ hvw \end{pmatrix} \quad \mathbf{F}_\sigma^{mc} = \begin{pmatrix} hu\omega \\ hv\omega \\ hw\omega \end{pmatrix} \quad (2.112)$$

$$\mathbf{F}_x^{md} = \begin{pmatrix} 2hv_t^h \frac{\partial u}{\partial x} \\ hv_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ hv_t^h \frac{\partial w}{\partial x} \end{pmatrix} \quad \mathbf{F}_y^{md} = \begin{pmatrix} hv_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ 2hv_t^h \frac{\partial v}{\partial y} \\ hv_t^h \frac{\partial w}{\partial y} \end{pmatrix} \quad \mathbf{F}_\sigma^{md} = \begin{pmatrix} \frac{v_t^v}{h} \frac{\partial u}{\partial \sigma} \\ \frac{v_t^v}{h} \frac{\partial v}{\partial \sigma} \\ \frac{v_t^v}{h} \frac{\partial w}{\partial \sigma} \end{pmatrix} \quad (2.113)$$

$$\mathbf{S}_h = \begin{pmatrix} g\eta \frac{\partial d}{\partial x'} + fhv - \frac{1}{\rho_0} \frac{\partial p_A}{\partial x} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial x} - hF_{vx} \\ g\eta \frac{\partial d}{\partial y'} - fhu - \frac{1}{\rho_0} \frac{\partial p_A}{\partial y} - \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial y} - hF_{vy} \\ -hF_{vz} \end{pmatrix} \quad \mathbf{S}_q = -\frac{1}{\rho_0} \begin{pmatrix} h \left( \frac{\partial q}{\partial x'} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial x} \right) \\ h \left( \frac{\partial q}{\partial y'} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial y} \right) \\ \frac{\partial q}{\partial \sigma} \end{pmatrix} \quad (2.114)$$

To give a conservative formulation, the gravity surface terms are split into two terms (see Chippada (1998), Rogers (2001), Quecedo (2002), Liang or Borthwick (2009))

$$gh \frac{\partial \eta}{\partial x'} = \frac{1}{2}g \frac{\partial(h^2 - d^2)}{\partial x'} - g\eta \frac{\partial d}{\partial x'} = \frac{1}{2}g \frac{\partial(\eta^2 + 2\eta d)}{\partial x'} - g\eta \frac{\partial d}{\partial x'} \quad (2.115)$$

$$gh \frac{\partial \eta}{\partial y'} = \frac{1}{2}g \frac{\partial(h^2 - d^2)}{\partial y'} - g\eta \frac{\partial d}{\partial y'} = \frac{1}{2}g \frac{\partial(\eta^2 + 2\eta d)}{\partial y'} - g\eta \frac{\partial d}{\partial y'} \quad (2.116)$$

It is easily seen that if  $\eta$  is constant, the two terms cancel exactly. In the discrete case, this is also true if the two derivatives are calculated using the same scheme.

## 2.2.2 Shallow water equations

In matrix form the continuity equations and the momentum equations may be written

$$\frac{\partial h}{\partial t'} + \nabla \cdot \mathbf{F}^c = 0 \quad (2.117)$$

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F}^m = \mathbf{S}_h + \mathbf{S}_q \quad (2.118)$$

where  $\mathbf{F}^c = (F_x^c, F_y^c)^T = (h\bar{u}, h\bar{v})^T$ ,  $\mathbf{U} = (hu, hv)^T$  and  $\mathbf{F}^m = \mathbf{F}^{mc} - \mathbf{F}^{md} = (\mathbf{F}_x^m, \mathbf{F}_y^m, \mathbf{F}_\sigma^m)^T$ .

The flux components and the source terms can be written

$$\mathbf{F}_x^{mc} = \begin{pmatrix} hu u + \frac{1}{2}g(\eta^2 + 2\eta d) \\ huv \\ huw \end{pmatrix} \quad \mathbf{F}_y^{mc} = \begin{pmatrix} h v v + \frac{1}{2}g(\eta^2 + 2\eta d) \\ hvv \\ hvw \end{pmatrix} \quad \mathbf{F}_\sigma^{mc} = \begin{pmatrix} hu\omega \\ hv\omega \\ hw\omega \end{pmatrix} \quad (2.119)$$

$$\mathbf{F}_x^{md} = \begin{pmatrix} 2hv_t^h \frac{\partial u}{\partial x} \\ hv_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ hv_t^h \frac{\partial w}{\partial x} \end{pmatrix} \quad \mathbf{F}_y^{md} = \begin{pmatrix} hv_t^h \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \\ 2hv_t^h \frac{\partial v}{\partial y} \\ hv_t^h \frac{\partial w}{\partial y} \end{pmatrix} \quad \mathbf{F}_\sigma^{md} = \begin{pmatrix} \frac{v_t^v}{h} \frac{\partial u}{\partial \sigma} \\ \frac{v_t^v}{h} \frac{\partial v}{\partial \sigma} \\ \frac{v_t^v}{h} \frac{\partial w}{\partial \sigma} \end{pmatrix} \quad (2.120)$$

$$\mathbf{S}_h = \begin{pmatrix} g\eta \frac{\partial d}{\partial x'} + fhv - \frac{h}{\rho_0} \frac{\partial p_A}{\partial x} - \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial x} - hF_{vx} \\ g\eta \frac{\partial d}{\partial y'} - fhu - \frac{h}{\rho_0} \frac{\partial p_A}{\partial y} - \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial y} - hF_{vy} \end{pmatrix} \quad (2.121)$$

### 2.2.3 Transport equations for temperature and salinity

In the sigma coordinate system the transport equations for the temperature and the salinity are given as

$$\frac{\partial hT}{\partial t'} + \frac{\partial huT}{\partial x'} + \frac{\partial hvk}{\partial y'} + \frac{\partial h\omega T}{\partial \sigma} = hF_t + \frac{\partial}{\partial \sigma} \left( \frac{D_{ts}^v}{h} \frac{\partial T}{\partial \sigma} \right) + h\hat{H} \quad (2.122)$$

$$\frac{\partial hS}{\partial t'} + \frac{\partial huS}{\partial x'} + \frac{\partial hvS}{\partial y'} + \frac{\partial h\omega S}{\partial \sigma} = hF_s + \frac{\partial}{\partial \sigma} \left( \frac{D_{ts}^v}{h} \frac{\partial S}{\partial \sigma} \right) \quad (2.123)$$

The horizontal diffusion terms are defined as

$$hF_t \approx \frac{\partial}{\partial x} \left( hD_{ts}^h \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( hD_{ts}^h \frac{\partial T}{\partial y} \right) \quad (2.124)$$

$$hF_s \approx \frac{\partial}{\partial x} \left( hD_{ts}^h \frac{\partial S}{\partial x} \right) + \frac{\partial}{\partial y} \left( hD_{ts}^h \frac{\partial S}{\partial y} \right) \quad (2.125)$$

In matrix form the transport equations for  $T$  and  $S$  may be written

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.126)$$

where  $\mathbf{U} = (hT, hS)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_\sigma)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^c = \begin{pmatrix} huT \\ huS \end{pmatrix} \quad \mathbf{F}_y^c = \begin{pmatrix} hvT \\ hvS \end{pmatrix} \quad \mathbf{F}_\sigma^c = \begin{pmatrix} h\omega T \\ h\omega S \end{pmatrix} \quad (2.127)$$

$$\mathbf{F}_x^d = \begin{pmatrix} hD_{ts}^h \frac{\partial T}{\partial x} \\ hD_{ts}^h \frac{\partial S}{\partial x} \end{pmatrix} \quad \mathbf{F}_y^d = \begin{pmatrix} hD_{ts}^h \frac{\partial T}{\partial y} \\ hD_{ts}^h \frac{\partial S}{\partial y} \end{pmatrix} \quad \mathbf{F}_\sigma^d = \begin{pmatrix} \frac{D_{ts}^v}{h} \frac{\partial T}{\partial \sigma} \\ \frac{D_{ts}^v}{h} \frac{\partial S}{\partial \sigma} \end{pmatrix} \quad (2.128)$$

$$\mathbf{S} = \begin{pmatrix} h\hat{H} \\ 0 \end{pmatrix} \quad (2.129)$$

### 2.2.4 Turbulence model

#### The k-epsilon model

In the sigma coordinate system, the transport equations for the  $k$ - $\varepsilon$  model are given as

$$\frac{\partial hk}{\partial t'} + \frac{\partial huk}{\partial x'} + \frac{\partial hvk}{\partial y'} + \frac{\partial h\omega k}{\partial \sigma} = hF_k + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \right) + h(P_k + B_k - \varepsilon) \quad (2.130)$$

$$\frac{\partial h\varepsilon}{\partial t'} + \frac{\partial hu\varepsilon}{\partial x'} + \frac{\partial hv\varepsilon}{\partial y'} + \frac{\partial h\omega\varepsilon}{\partial \sigma} = hF_\varepsilon + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_\varepsilon^v} \frac{\partial \varepsilon}{\partial \sigma} \right) + h \left( P_\varepsilon + B_\varepsilon - c_{2\varepsilon} \frac{\varepsilon^2}{k} \right) \quad (2.131)$$

The horizontal diffusion terms are defined as

$$hF_k \approx \frac{\partial}{\partial x} \left( \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \right) \quad (2.132)$$

$$hF_\varepsilon \approx \frac{\partial}{\partial x} \left( \frac{hv_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{hv_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial y} \right) \quad (2.133)$$

In matrix form, the transport equations for  $k$  and  $\varepsilon$  may be written

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.134)$$

where  $\mathbf{U} = (hk, h\varepsilon)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_\sigma)^T$ . The flux components and the source terms can be written

$$\mathbf{F}_x^c = \begin{pmatrix} huk \\ hu\varepsilon \end{pmatrix}, \quad \mathbf{F}_y^c = \begin{pmatrix} hvk \\ hv\varepsilon \end{pmatrix}, \quad \mathbf{F}_\sigma^c = \begin{pmatrix} h\omega k \\ h\omega\varepsilon \end{pmatrix} \quad (2.135)$$

$$\mathbf{F}_x^d = \begin{pmatrix} \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \\ \frac{hv_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial x} \end{pmatrix}, \quad \mathbf{F}_y^d = \begin{pmatrix} \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \\ \frac{hv_{t0}^h}{\sigma_\varepsilon^h} \frac{\partial \varepsilon}{\partial y} \end{pmatrix}, \quad \mathbf{F}_\sigma^d = \begin{pmatrix} \frac{v_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \\ \frac{v_{t0}^v}{h\sigma_\varepsilon^v} \frac{\partial \varepsilon}{\partial \sigma} \end{pmatrix} \quad (2.136)$$

$$\mathbf{S} = \begin{pmatrix} h(P_k + B_k - \varepsilon) \\ h \left( P_\varepsilon + B_\varepsilon - c_{2\varepsilon} \frac{\varepsilon^2}{k} \right) \end{pmatrix} \quad (2.137)$$

## The k-omega model

In this section, the modified vertical velocity in the sigma coordinate system is called  $w_s$  (instead of  $\omega$ ). This is to distinguish it from the specific dissipation rate,  $\omega$ , of turbulent kinetic energy which was introduced in section 2.1.4. In the sigma coordinate system, the transport equations for the  $k$ - $\omega$  model are given as

$$\frac{\partial hk}{\partial t'} + \frac{\partial huk}{\partial x'} + \frac{\partial hvk}{\partial y'} + \frac{\partial hw_s k}{\partial \sigma} = hF_k + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \right) + h(P_k + B_k - \beta_k \omega k) \quad (2.138)$$

$$\frac{\partial h\omega}{\partial t'} + \frac{\partial hu\omega}{\partial x'} + \frac{\partial hv\omega}{\partial y'} + \frac{\partial hw_s \omega}{\partial \sigma} = hF_\omega + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_\omega^v} \frac{\partial \omega}{\partial \sigma} \right) + hF_{\omega c} + h(P_\omega - \beta_\omega \omega^2) \quad (2.139)$$

The horizontal diffusion terms are defined as

$$hF_k \approx \frac{\partial}{\partial x} \left( \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{hv_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \right) \quad (2.140)$$



$$hF_\omega \approx \frac{\partial}{\partial x} \left( \frac{h\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial x} \right) + \frac{\partial}{\partial y} \left( \frac{h\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial y} \right) \quad (2.141)$$

In matrix form, the transport equations for  $k$  and  $\omega$  may be written

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F} - \mathbf{G} = \mathbf{S} \quad (2.142)$$

where  $\mathbf{U} = (hk, h\omega)^T$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_\sigma)^T$ . The flux components  $\mathbf{F}$ , the cross-diffusion  $\mathbf{G}$  and the source terms  $\mathbf{S}$  can be written

$$\mathbf{F}_x^c = \begin{pmatrix} huk \\ hu\omega \end{pmatrix}, \quad \mathbf{F}_y^c = \begin{pmatrix} hvk \\ hv\omega \end{pmatrix}, \quad \mathbf{F}_\sigma^c = \begin{pmatrix} hw_s k \\ hw_s \omega \end{pmatrix} \quad (2.143)$$

$$\mathbf{F}_x^d = \begin{pmatrix} \frac{h\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial x} \\ \frac{h\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial x} \end{pmatrix}, \quad \mathbf{F}_y^d = \begin{pmatrix} \frac{h\nu_{t0}^h}{\sigma_k^h} \frac{\partial k}{\partial y} \\ \frac{h\nu_{t0}^h}{\sigma_\omega^h} \frac{\partial \omega}{\partial y} \end{pmatrix}, \quad \mathbf{F}_\sigma^d = \begin{pmatrix} \frac{\nu_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \\ \frac{\nu_{t0}^v}{h\sigma_\omega^v} \frac{\partial \omega}{\partial \sigma} \end{pmatrix} \quad (2.144)$$

$$\mathbf{G} = \begin{pmatrix} 0 \\ hF_{\omega c} \end{pmatrix} \quad (2.145)$$

$$\mathbf{S} = \begin{pmatrix} h(P_k + B_k - \varepsilon) \\ h(P_\omega - \beta_\omega \omega^2) \end{pmatrix} \quad (2.146)$$

## 2.2.5 Transport equation for a scalar quantity

In the sigma coordinate system the transport equation for a scalar quantity is given as

$$\frac{\partial hC}{\partial t'} + \frac{\partial huC}{\partial x'} + \frac{\partial hvC}{\partial y'} + \frac{\partial h\omega C}{\partial \sigma} = hF_c + \frac{\partial}{\partial \sigma} \left( \frac{D_c^v}{h} \frac{\partial C}{\partial \sigma} \right) - hk_p C \quad (2.147)$$

The horizontal diffusion term is defined as

$$hF_c = \frac{\partial}{\partial x} \left( hD_c^h \frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial y} \left( hD_c^h \frac{\partial C}{\partial y} \right) \quad (2.148)$$

In matrix form the transport equation for  $C$  may be written

$$\frac{\partial \mathbf{U}}{\partial t'} + \nabla \cdot \mathbf{F} = \mathbf{S} \quad (2.149)$$

where  $\mathbf{U} = (hC)$  and  $\mathbf{F} = \mathbf{F}^c - \mathbf{F}^d = (\mathbf{F}_x, \mathbf{F}_y, \mathbf{F}_\sigma)^T$ . The flux components and the source term can be written

$$\mathbf{F}_x^c = (huC) \quad \mathbf{F}_y^c = (hvk) \quad \mathbf{F}_\sigma^c = (h\omega C) \quad (2.150)$$

$$\mathbf{F}_x^d = \left( hD_c^h \frac{\partial C}{\partial x} \right) \quad \mathbf{F}_y^d = \left( hD_c^h \frac{\partial C}{\partial y} \right) \quad \mathbf{F}_\sigma^d = \left( \frac{D_c^v}{h} \frac{\partial C}{\partial \sigma} \right) \quad (2.151)$$

$$\mathbf{S} = -(hk_p C) \quad (2.152)$$



### 3 Numerical method

The discretization in solution domain is performed using a cell-centered finite volume method (CCFV). The spatial domain is discretized by subdivision of the continuum into non-overlapping control volumes and by evaluating the field equations in integral form on these cells.

#### 3.1 Mesh and discretization scheme

##### 3.1.1 Mesh

The computational mesh is based on the unstructured meshes approach, which gives the maximum degree of flexibility. Control of node distribution allows for optimal usage of nodes and adaptation of mesh resolution to the relevant physical scales. The use of unstructured meshes also makes it possible to handle problems characterized by computational domains with complex boundaries.

The 3D mesh is a layered mesh. In the horizontal domain an unstructured mesh is used while in the vertical domain a structured mesh is used (see Figure 3.1). The elements are prisms with either a 3-sided or 4-sided polygonal base. Hence, the horizontal faces are either triangles or quadrilateral elements. The elements are perfectly vertical, and all layers have identical horizontal topology.

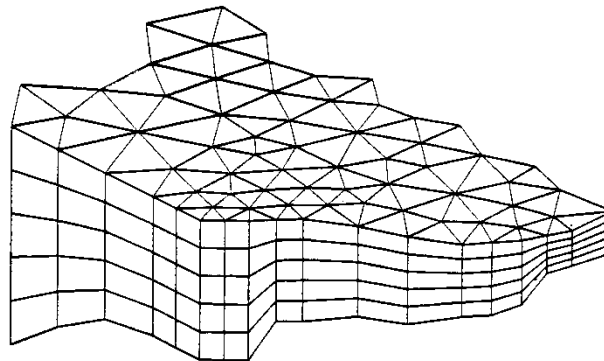


Figure 3.1 Principle of meshing

For the vertical discretization both a standard sigma discretization and a combined sigma/z-level discretization can be used. For the hybrid sigma/z-level discretization, sigma coordinates are used from the free surface to a specified depth,  $z_0$ , and z-level coordinates are used below. The different types of vertical discretization are illustrated in Figure 3.2. At least one sigma layer is needed using the sigma/z-level discretization to allow changes in the surface elevation.

##### Sigma

In the sigma domain a constant number of layers,  $N_\sigma$ , is used, and the height of each sigma layer is a fixed fraction of the total depth of the sigma domain,  $h_\sigma$ , where  $h_\sigma = \eta - \max(z_b, z_\sigma)$ . The discretization in the sigma domain is given by a number of discrete  $\sigma$ -levels  $\{\sigma_i, i = 1, (N_\sigma + 1)\}$ . Here  $\sigma$  varies from  $\sigma_1 = 0$  at the bottom interface of the lowest sigma layer to  $\sigma_{N_\sigma+1} = 1$  at the free surface.

Variable sigma coordinates can be obtained using a discrete formulation of the general vertical coordinate (s-coordinate) system proposed by Song and Haidvogel (1994). First an equidistant discretization in an s-coordinate system ( $-1 \leq s \leq 0$ ) is defined

$$s_i = -\frac{N_\sigma + 1 - i}{N_\sigma} \quad i = 1, (N_\sigma + 1) \quad (3.1)$$

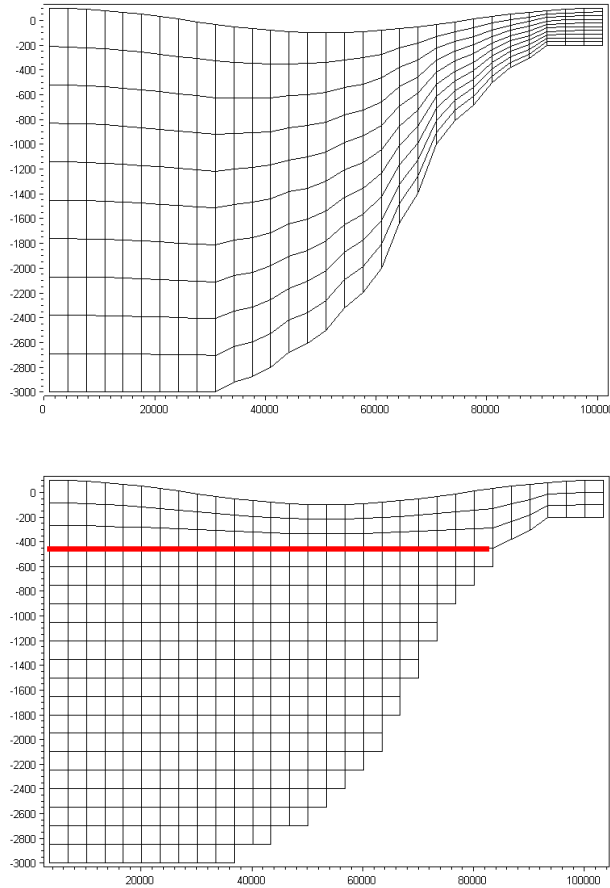


Figure 3.2 Illustrations of the different vertical grids. Upper: sigma mesh, Lower: combined sigma/z-level mesh with simple bathymetry adjustment. The red line shows the interface between the z-level domain and the sigma-level domain

The discrete sigma coordinates can then be determined by

$$\sigma_i = 1 + \sigma_c s_i + (1 - \sigma_c) c(s_i) \quad i = 1, (N_\sigma + 1) \quad (3.2)$$

where

$$c(s) = (1 - b) \frac{\sinh(\theta s)}{\sinh(\theta)} + b \frac{\tanh\left(\theta\left(s + \frac{1}{2}\right)\right) - \tanh\left(\frac{\theta}{2}\right)}{2 \tanh\left(\frac{\theta}{2}\right)} \quad (3.3)$$

Here  $\sigma_c$  is a weighting factor between the equidistant distribution and the stretch distribution,  $\theta$  is the surface control parameter, and  $b$  is the bottom control parameter. The

range for the weighting factor is  $0 < \sigma_c \leq 1$  where the value 1 corresponds to equidistant distribution, and 0 corresponds to stretched distribution. A small value of  $\sigma_c$  can result in linear instability. The range of the surface control parameter is  $0 < \theta < 20$ , and the range of the bottom control parameter is  $0 \leq b \leq 1$ . If  $\theta \ll 1$  and  $b = 0$ , an equidistant vertical resolution is obtained. By increasing the value of  $\theta$ , the highest resolution is achieved near the surface. If  $\theta > 0$  and  $b = 1$ , a high resolution is obtained both near the surface and near the bottom.

Examples of a mesh using variable vertical discretization are shown in Figure 3.3 and Figure 3.4.

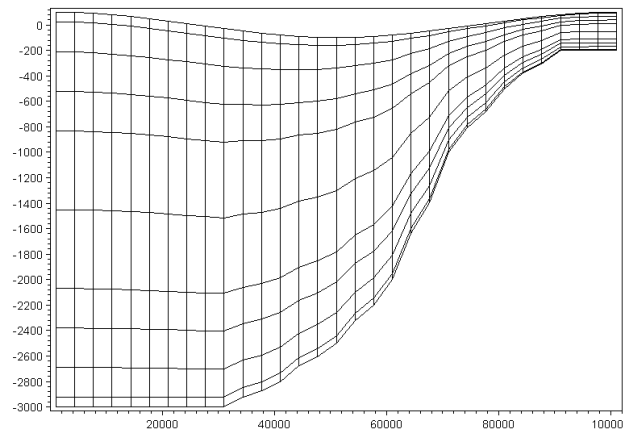


Figure 3.3 Example of vertical distribution using layer thickness distribution. Number of layers: 10, thickness of layers 1 to 10: .025, 0.075, 0.1, 0.01, 0.02, 0.02, 0.1, 0.1, 0.075, 0.025

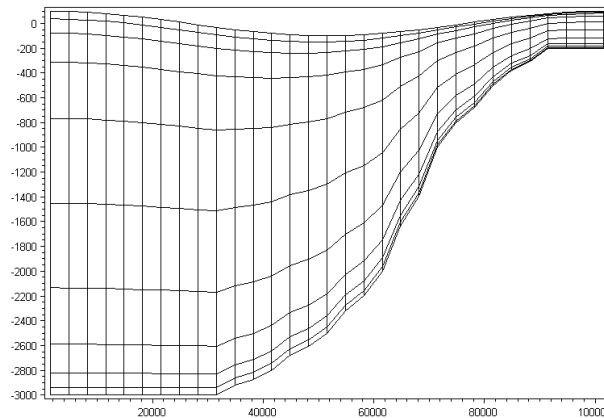


Figure 3.4 Example of vertical distribution using variable distribution. Number of layers: 10,  $\sigma_c = 0.1$ ,  $\theta = 5$ ,  $b = 1$

### Combined sigma/z-level

In the z-level domain the discretization is given by a number of discrete z-levels  $\{z_i, i = 1, (N_z + 1)\}$ , where  $N_z$  is the number of layers in the z-level domain.  $z_1$  is the minimum z-level, and  $z_{N_z+1}$  is the maximum z-level, which is equal to the sigma depth,  $z_\sigma$ . The corresponding layer thickness is given by

$$\Delta z_i = z_{i+1} - z_i \quad i = 1, N_z \quad (3.4)$$

The discretization is illustrated in Figure 3.5 and Figure 3.6.

Using standard z-level discretization the bottom depth is rounded to the nearest z-level. Hence, for a cell in the horizontal mesh with the cell-averaged depth,  $z_b$ , each cell in the corresponding column in the z-domain is only included if the following criterion is satisfied

$$z_{i+1} - z_b \geq \frac{1}{2}(z_{i+1} - z_i) \quad i = 1, N_z \quad (3.5)$$

The cell-averaged depth,  $z_b$ , is calculated as the mean value of the depth at the vertices of each cell in the horizontal mesh. To take into account the correct depth for the case where the bottom depth is below the minimum z-level ( $z_1 > z_b$ ) a bottom fitted approach is used. Here, a correction factor,  $f_1$ , for the layer thickness in the bottom cell is introduced. The correction factor is used in the calculation of the volume and vertical face integrals. The correction factor for the bottom cell is calculated by

$$f_1 = \frac{(z_2 - z_b)}{\Delta z_1} \quad (3.6)$$

The corrected layer thickness is given by  $\Delta z_1^* = f_1 \Delta z_1$ . The simple bathymetry adjustment approach is illustrated in Figure 3.5.

For a more accurate representation of the bottom depth an advanced bathymetry adjustment approach can be used. For a cell in the horizontal mesh with the cell-averaged depth,  $z_b$ , each cell in the corresponding column in the z-domain is included if the following criterion is satisfied

$$z_{i+1} > z_b \quad i = 1, N_z \quad (3.7)$$

A correction factor,  $f_i$ , is introduced for the layer thickness for these cells

$$f_i = \min \left( \max \left( \frac{(z_{i+1} - z_b)}{\Delta z_i}, \frac{z_{min}}{\Delta z_i} \right), 1 \right) \quad i = 2, N_z$$

$$f_i = \max \left( \frac{(z_{i+1} - z_b)}{\Delta z_i}, \frac{z_{min}}{\Delta z_i} \right) \quad i = 1 \quad (3.8)$$

A minimum layer thickness,  $\Delta z_{min}$ , is introduced to avoid very small values of the correction factor. The correction factor is used in the calculation of the volume and vertical face integrals. The corrected layer thicknesses are given by  $\{\Delta z_i^* = f_i \Delta z_i, i = 1, N_z\}$ . The advanced bathymetry adjustment approach is illustrated in Figure 3.6.

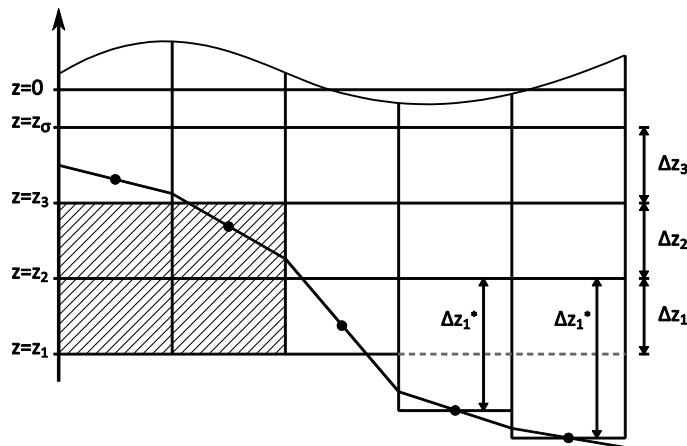


Figure 3.5 Simple bathymetry adjustment approach

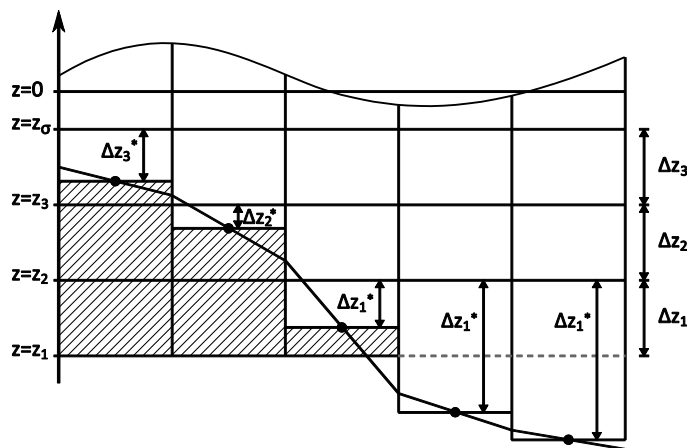


Figure 3.6 Advanced bathymetry adjustment approach

### 3.1.2 Discretization scheme

The discrete solution for the water depth,  $h$ , is defined at the centroid of the elements of the 2D horizontal mesh. The discrete solutions for the velocity components,  $u$ ,  $v$  and  $w$  and the transport variables,  $T$ ,  $S$ ,  $k$ ,  $\varepsilon$  and  $C$ , are defined at the centroid of the elements in the 3D mesh. The non-hydrostatic pressure,  $q$ , is positioned in the centroid of the horizontal cell faces as shown in Figure 3.7. The location of the discrete non-hydrostatic pressure secures an exact representation of the surface boundary condition. The modified vertical velocity,  $\omega$ , is also positioned in the centroid of the horizontal cell faces. The coordinates of the centroids are the averages of the coordinates of the cells vertices.

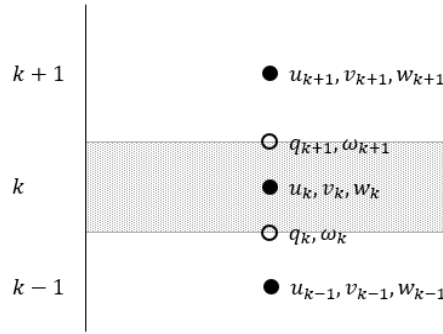


Figure 3.7 Vertical variable arrangement around layer  $k$ . Velocity components,  $u, v$  and  $w$ , are located in cell centers; non-hydrostatic pressure,  $q$ , is located in cell interfaces

## 3.2 Finite volume method

The matrix form of the governing equations presented in Chapter 2 can be written as

$$\frac{\partial \mathbf{W}}{\partial t} + \nabla \cdot \mathbf{F}(\mathbf{W}) = \mathbf{S} \quad (3.9)$$

Integrating Eq. (3.9) over the  $i$ th cell and using Gauss's theorem to rewrite the flux integral gives

$$\int_{V_i} \frac{\partial \mathbf{W}}{\partial t} d\Omega + \int_{\Gamma_i} (\mathbf{F}(\mathbf{W}) \cdot \mathbf{n}) d\Gamma = \int_{V_i} \mathbf{S}(\mathbf{W}) d\Omega \quad (3.10)$$

where  $V_i$  is the volume of the  $i$ th cell,  $\Omega$  is the integration variable defined on  $V_i$ ,  $\Gamma_i$  is the boundary of the  $i$ th cell and  $\Gamma$  is the integration variable along the boundary.  $\mathbf{n} = (n_x, n_y, n_z)^T$  is the unit outward normal vector along the boundary. Evaluating the volume integrals by a one-point quadrature rule, the quadrature point being the centroid of the cell, and evaluating the boundary integral using a mid-point quadrature rule, Eq. (3.10) can be written

$$\frac{\partial \mathbf{W}_i}{\partial t} + \frac{1}{V_i} \sum_j^{NF} \mathbf{F} \cdot \mathbf{n}_{ij} \Delta \Gamma_{ij} = \mathbf{S}_i \quad (3.11)$$

Here  $\mathbf{W}_i$  and  $\mathbf{S}_i$ , respectively, are average values of  $\mathbf{W}$  and  $\mathbf{S}$  over the  $i$ th cell and stored at the cell centre.  $NF$  is the number of faces of the cell and the face  $ij$  is common to the cells associated with  $\mathbf{W}_i$  and  $\mathbf{W}_j$ .  $\Delta \Gamma_{ij}$  is the area of the face  $ij$ , and  $\mathbf{n}_{ij}$  is the restriction of  $\mathbf{n}$  to the face  $ij$ .

The normal flux  $\mathbf{F}_n(\mathbf{W}_L, \mathbf{W}_R) = \mathbf{F}(\mathbf{W}_L, \mathbf{W}_R) \cdot \mathbf{n}_{ij}$  is determined from the variables,  $\mathbf{W}_L$  and  $\mathbf{W}_R$ , to the left and right of the face  $ij$ . Using a first order scheme  $\mathbf{W}_L = \mathbf{W}_i$  and  $\mathbf{W}_R = \mathbf{W}_j$ . Second-order spatial accuracy is achieved by employing a linear gradient-reconstruction technique. The face value at the vertical faces for the primitive variable  $v$  in cell  $i$  is obtained by

$$v(x, y) = v_i + \nabla v_i \cdot \mathbf{r} \quad (3.12)$$

where  $(x, y)$  is the point where the value is required,  $\mathbf{r}$  is the distance vector from the cell centre to the point  $(x, y)$  and  $\nabla v_i$  is the gradient vector. For estimation of the gradient



vector the Green-Gauss gradient approach is utilized. Here the procedure proposed by Jawahar and Kamath (2000) is used. This procedure is based on a wide computational stencil to improve accuracy also for meshes with poor connectivity. The vertex (node) value is computed using the pseudo-Laplacian procedure proposed by Holmes and Connell (1989).

### 3.3 Numerical solution of the flow equations

#### 3.3.1 Time integration of the Navier-Stokes equations

The time integration of the Navier-Stokes equations is performed using a semi-implicit scheme. The vertical convective and diffusive terms are discretized using an implicit scheme to remove the stability limitations associated with the vertical resolution. Here a second order implicit trapezoidal method is used (see Lambert (1973) and Hirsch (1990)). The remaining terms are discretized using a two-stage explicit second-order Runge-Kutta scheme (the midpoint method). The non-hydrostatic pressure is treated by a fractional step approach developed by Chorin (1968) called the projection method which is based on the Helmholtz-Hodge decomposition. In the sigma coordinate system, the integration procedure is

Stage 1:

$$\frac{h^{n+1/2} - h^n}{\Delta t/2} = - \left( \frac{\partial F_x^c}{\partial x'} + \frac{\partial F_y^c}{\partial y'} \right)^n \quad (3.13)$$

$$\frac{\mathbf{U}^* - \mathbf{U}^n}{\Delta t/2} = - \left( \frac{\partial \mathbf{F}_x^m}{\partial x'} + \frac{\partial \mathbf{F}_y^m}{\partial y'} \right)^n - \frac{1}{2} \left( \left( \frac{\partial \mathbf{F}_\sigma^m}{\partial \sigma} \right)^* + \left( \frac{\partial \mathbf{F}_\sigma^m}{\partial \sigma} \right)^n \right) + \mathbf{S}_h^n + \mathbf{S}_q^n \quad (3.14)$$

$$\frac{\mathbf{U}^{n+1/2} - \mathbf{U}^*}{\Delta t/2} = \mathbf{S}_q^* \quad (3.15)$$

Stage 2:

$$\frac{h^{n+1} - h^n}{\Delta t} = - \left( \frac{\partial F_x^c}{\partial x'} + \frac{\partial F_y^c}{\partial y'} \right)^{n+1/2} \quad (3.16)$$

$$\frac{\mathbf{U}^* - \mathbf{U}^n}{\Delta t} = - \left( \frac{\partial \mathbf{F}_x^m}{\partial x'} + \frac{\partial \mathbf{F}_y^m}{\partial y'} \right)^{n+1/2} - \frac{1}{2} \left( \left( \frac{\partial \mathbf{F}_\sigma^m}{\partial z} \right)^* + \left( \frac{\partial \mathbf{F}_\sigma^m}{\partial z} \right)^n \right) + \mathbf{S}_h^n + \mathbf{S}_q^n \quad (3.17)$$

$$\frac{\mathbf{U}^{n+1} - \mathbf{U}^*}{\Delta t} = \mathbf{S}_q^* \quad (3.18)$$

Calculating  $\mathbf{S}_q^*$  requires knowledge of the non-hydrostatic pressure,  $q$ . The pressure is calculated solving a Poisson equation. The modified vertical velocity is calculated after the update of the water depth from Eq. (2.102).

Due to the explicit scheme, the time step interval,  $\Delta t$ , is restricted by the Courant-Friedrichs-Lewy (CFL) condition

$$C = \Delta t \frac{(\sqrt{gh} + |u|) + (\sqrt{gh} + |v|)}{\Delta l} \leq C_{max} \quad (3.19)$$

where  $C$  is the Courant number and  $\Delta l$  is a characteristic length.  $C_{max}$  is the maximum Courant number and must be less than or equal to 1. A variable time step interval is used in the time integration of the Navier-Stokes equations and determined so that the Courant number is less than a maximum Courant number in all computational nodes. The characteristic length for a prism, where the horizontal face is a quadrilateral element, is determined as the area of the element divided by the longest edge length of the element. If the horizontal face is a triangular element, the characteristic length is two times the area divided by the longest edge length.

### 3.3.2 Poisson equation

The Poisson equation is derived by differentiating the three components of the vector Eq. (3.15) and (3.18) by  $x'$ ,  $y'$  and  $\sigma$  and substituting the resulting expressions back into the continuity equation

$$\frac{\partial u}{\partial x'} + \frac{\partial u}{\partial \sigma} \frac{\partial \sigma}{\partial x} + \frac{\partial v}{\partial y'} + \frac{\partial v}{\partial \sigma} \frac{\partial \sigma}{\partial y} + \frac{1}{h} \frac{\partial w}{\partial \sigma} = 0 \quad (3.20)$$

The resulting Poisson equation in sigma coordinates reads

$$\begin{aligned} \frac{\partial^2 q}{\partial x'^2} + \frac{\partial^2 q}{\partial y'^2} + (A_x^2 + A_y^2 + A_z^2) \frac{\partial^2 q}{\partial \sigma^2} + 2A_x \frac{\partial^2 q}{\partial x' \partial \sigma} + 2A_y \frac{\partial^2 q}{\partial y' \partial \sigma} + \\ \left( \frac{\partial A_x}{\partial x'} + \frac{\partial A_y}{\partial y'} \right) \frac{\partial q}{\partial \sigma} = \frac{\rho_0}{\Delta t^*} \left( \frac{\partial u^*}{\partial x'} + \frac{\partial v^*}{\partial y'} + A_x \frac{\partial u^*}{\partial \sigma} + A_y \frac{\partial v^*}{\partial \sigma} + A_z \frac{\partial w^*}{\partial \sigma} \right) \end{aligned} \quad (3.21)$$

In the first stage  $\Delta t^* = \Delta t/2$ , and in the second stage  $\Delta t^* = \Delta t$ . The Poisson equation in Cartesian coordinate reads

$$\frac{\partial^2 q}{\partial x^2} + \frac{\partial^2 q}{\partial y^2} + \frac{\partial^2 q}{\partial z^2} = \frac{\rho_0}{\Delta t^*} \left( \frac{\partial u^*}{\partial x} + \frac{\partial v^*}{\partial y} + \frac{\partial w^*}{\partial z} \right) \quad (3.22)$$

The surface and bottom boundary conditions for the non-hydrostatic pressure,  $q$ , in the sigma coordinate system are

at  $z = \eta$

$$q = 0 \quad (3.23)$$

at  $z = -d$

$$\frac{\partial q}{\partial \sigma} = 0 \quad (3.24)$$

For applications where the still water depth,  $d$ , is changing in time the following bottom boundary condition is used

$$\frac{\partial q}{\partial \sigma} = \rho_0 h \frac{\partial^2 d}{\partial t^2} \quad (3.25)$$

In a Cartesian coordinate system, the boundary condition at the bottom is

$$\frac{\partial q}{\partial z} = 0 \quad (3.26)$$

### 3.3.3 Time integration of the shallow water equations

The time integration of the shallow water equations is performed using a semi-implicit scheme. The vertical convective and diffusive terms are discretized using an implicit scheme to remove the stability limitations associated with the vertical resolution. Here a second order implicit trapezoidal method is used (see Lambert (1973) and Hirsch (1990)). The remaining terms are discretized using either a first-order explicit Euler scheme or a two-stage explicit second-order Runge-Kutta scheme (the midpoint method). In the sigma coordinate system, the integration procedure for the explicit Euler scheme is

$$\frac{h^{n+1} - h^n}{\Delta t} = - \left( \frac{\partial F_x^c}{\partial x'} + \frac{\partial F_y^c}{\partial y'} \right)^n \quad (3.27)$$

$$\frac{\mathbf{U}^{n+1} - \mathbf{U}^n}{\Delta t} = - \left( \frac{\partial \mathbf{F}_x^m}{\partial x'} + \frac{\partial \mathbf{F}_y^m}{\partial y'} \right)^n - \frac{1}{2} \left( \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^{n+1} + \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^n \right) + \mathbf{S}_h^n + \mathbf{S}_q^n \quad (3.28)$$

The integration procedure for the two-stage explicit Runge-Kutta scheme is

Stage 1:

$$\frac{h^{n+1/2} - h^n}{\Delta t/2} = - \left( \frac{\partial F_x^c}{\partial x'} + \frac{\partial F_y^c}{\partial y'} \right)^n \quad (3.29)$$

$$\frac{\mathbf{U}^{n+1/2} - \mathbf{U}^n}{\Delta t/2} = - \left( \frac{\partial \mathbf{F}_x^m}{\partial x'} + \frac{\partial \mathbf{F}_y^m}{\partial y'} \right)^n - \frac{1}{2} \left( \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^{n+1/2} + \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^n \right) + \mathbf{S}_h^n + \mathbf{S}_q^n \quad (3.30)$$

Stage 2:

$$\frac{h^{n+1} - h^n}{\Delta t} = - \left( \frac{\partial F_x^c}{\partial x'} + \frac{\partial F_y^c}{\partial y'} \right)^{n+1/2} \quad (3.31)$$

$$\frac{\mathbf{U}^{n+1} - \mathbf{U}^n}{\Delta t} = - \left( \frac{\partial \mathbf{F}_x^m}{\partial x'} + \frac{\partial \mathbf{F}_y^m}{\partial y'} \right)^{n+1/2} - \frac{1}{2} \left( \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^{n+1} + \left( \frac{\partial \mathbf{F}_z^m}{\partial \sigma} \right)^n \right) + \mathbf{S}_h^n + \mathbf{S}_q^n \quad (3.32)$$

### 3.3.4 Space discretization of Navier-Stokes equations

The space discretization is performed using the finite volume method as described in Section 3.2. In this section the focus is on the discretization for the equations in the sigma coordinate system.

The normal convective flux  $\mathbf{F}_n(\mathbf{U}) = (f_1, f_2, f_3, f_4)$  at the vertical faces in the sigma domain can be written

$$\mathbf{F}_n(\mathbf{U}) = \begin{pmatrix} hu_{\perp} \\ hu_{\perp} + \frac{1}{2}g(\eta^2 + 2\eta d)n_x \\ hvu_{\perp} + \frac{1}{2}g(\eta^2 + 2\eta d)n_y \\ h\omega u_{\perp} \end{pmatrix} \quad (3.33)$$

where  $\mathbf{U} = (h, hu, hv, h\omega)^T$  is the solution vector, and  $u_{\perp} = un_x + vn_y$  is the velocity perpendicular to the cell face. Here  $f_1$  is the contribution to the continuity equation, and  $f_2, f_3$  and  $f_4$  are the contributions to the three momentum equations. This flux is reconstructed at cell-interfaces using the HLLC scheme introduced by Toro et al. (1994) for solving the Euler equations. The shock-capturing scheme enables robust and stable simulation of flows involving shocks or discontinuities such as bores and hydraulic jumps. The interface flux is computed as follows (see Toro (2001))

$$\mathbf{F}(\mathbf{U}_L, \mathbf{U}_R) \cdot \mathbf{n} = \begin{cases} \mathbf{F}_L & \text{if } S_L \geq 0 \\ \mathbf{F}_{*L} & \text{if } S_L < 0 \leq S_* \\ \mathbf{F}_{*R} & \text{if } S_* < 0 \leq S_R \\ \mathbf{F}_R & \text{if } S_R \leq 0 \end{cases} \quad (3.34)$$

where  $\mathbf{F}_L = \mathbf{F}_n(\mathbf{U}_L)$  and  $\mathbf{F}_R = \mathbf{F}_n(\mathbf{U}_R)$  are calculated from Eq. (3.33), and the middle region fluxes,  $\mathbf{F}_{*L}$  and  $\mathbf{F}_{*R}$  are given by

$$\mathbf{F}_{*L} = \begin{pmatrix} e_1 \\ e_2 n_x - u_{\parallel L} e_1 n_y \\ e_2 n_y + u_{\parallel L} e_1 n_x \\ e_3 \end{pmatrix} \quad (3.35)$$

$$\mathbf{F}_{*R} = \begin{pmatrix} e_1 \\ e_2 n_x - u_{\parallel R} e_1 n_y \\ e_2 n_y + u_{\parallel R} e_1 n_x \\ e_3 \end{pmatrix} \quad (3.36)$$

Here  $u_{\parallel} = -un_y + vn_x$  is the velocity tangential to the cell face, and  $(e_1, e_2, e_3)$  is the component of the normal flux which is calculated using the HLL solver proposed by Harten et al. (1983)

$$\mathbf{E} = \frac{S_R \hat{\mathbf{E}}_L - S_L \hat{\mathbf{E}}_R + f_{HLLC} S_L S_R (\hat{\mathbf{U}}_R - \hat{\mathbf{U}}_L)}{S_R - S_L} \quad (3.37)$$

Here  $\hat{\mathbf{U}} = (h, hu_{\perp}, h\omega)^T$  and  $\hat{\mathbf{E}} = (hu_{\perp}, hu_{\perp}u_{\perp} + \frac{1}{2}g(\eta^2 + 2\eta d), h\omega)^T$ . To be able to scale the damping introduced by the HLLC solver a scaling factor  $f_{HLLC}$  has been introduced, where the factor must be in the interval  $[0, 1]$ . The scaling factor,  $f_{HLLC} = 1$ , corresponds to the standard HLLC solver.

An appropriate method for approximating the wave speeds is essential for the efficiency of the HLLC solver. Different approximations can be found in the literature, e.g. Fraccarollo and Toro (1994). Here the approach used by Song et al. (2011) is used

$$S_L = \begin{cases} u_{\perp R} - 2\sqrt{gh_R} & h_L = 0 \\ \min(u_{\perp L} - \sqrt{gh_L}, u_{\perp*} - \sqrt{gh_*}) & h_L > 0 \end{cases} \quad (3.38)$$

and

$$S_R = \begin{cases} u_{\perp L} + 2\sqrt{gh_L} & h_R = 0 \\ \max(u_{\perp R} + \sqrt{gh_R}, u_{\perp*} + \sqrt{gh_*}) & h_R > 0 \end{cases} \quad (3.39)$$

where the Roe-averaged quantities

$$u_{\perp*} = \frac{u_{\perp L}\sqrt{h_L} + u_{\perp R}\sqrt{h_R}}{\sqrt{h_L} + \sqrt{h_R}} \quad (3.40)$$

$$h_* = \frac{1}{2}(h_L + h_R) \quad (3.41)$$

The speed  $S_*$  is given by the

$$S_* = \frac{S_L h_R (u_{\perp R} - S_R) - S_R h_L (u_{\perp L} - S_L)}{h_R (u_{\perp R} - S_R) - h_L (u_{\perp L} - S_L)} \quad (3.42)$$

The convective flux at the horizontal faces is calculated using a second-order upwinding scheme. The diffusive flux at the cell interfaces is approximated by a central scheme. The vertical discretization of the convective and diffusive terms results in a linear five-diagonal system which has to be solved for each column of the discrete momentum equation.

Discretization of the Poisson pressure equation is performed by integrating over the individual control volumes. The procedure results in a large sparse linear system that needs to be solved in each of the two stages in the time integration procedure. This sparse linear system of equations is solved using an iterative solver from the PETSc library, Balay (2017). More specifically, the iterative solver is the restarted Generalized Minimal Residual method (GMRES), which for single-subdomain simulations is preconditioned with a two-level incomplete LU factorization, ILU(2). For multi-subdomain simulations the Block Jacobi preconditioner is used, where each block is solved with ILU(2). Each block coincides with the division of variables over the processors. See Chapter 6 for further details on single- and multi-subdomain simulations.

### 3.3.5 Space discretization of shallow water equations

The space discretization is performed using the finite volume method as described in Section 3.2. In this section the focus is on the discretization for the equations in the sigma coordinate system.

The normal convective flux  $\mathbf{F}_n(\mathbf{U}) = (f_1, f_2, f_3)$  at the vertical faces in the sigma domain can be written

$$\mathbf{F}_n(\mathbf{U}) = \begin{pmatrix} hu_{\perp} \\ hu u_{\perp} + \frac{1}{2}g(\eta^2 + 2\eta d)n_x \\ hv u_{\perp} + \frac{1}{2}g(\eta^2 + 2\eta d)n_y \end{pmatrix} \quad (3.43)$$

where  $\mathbf{U} = (h, hu, hv)^T$  is the solution vector, and  $u_{\perp} = un_x + vn_y$  is the velocity perpendicular to the cell face. Here  $f_1$  is the contribution to the continuity equation, and  $f_2$ , and  $f_3$  are the contributions to the two momentum equations. This flux is reconstructed at cell-interfaces using the Roe's scheme (see Roe (1981)). The shock-capturing scheme enables robust and stable simulation of flows involving shocks or discontinuities such as bores and hydraulic jumps.

The convective flux at the horizontal faces is calculated using a first-order upwinding scheme. The diffusive flux at the cell interfaces is approximated by a central scheme. The vertical discretization of the convective and diffusive terms results in a linear three-diagonal system, which has to be solved for each column of the discrete momentum equation.

To avoid numerical oscillations a second order TVD slope limiter (Van Leer limiter, see Hirsh, 1990 and Darwish, 2003) is used.

### 3.3.1 Explicit filtering

The collocated grid discretization in combination with unstructured triangular meshes is known to produce checkerboard oscillations in the horizontal velocity field, when the higher-order scheme is applied in space. A number of methods has been proposed to solve this problem (see Wolfram and Fringer (2013), Zhang et al. (2014)). Here, a filtering procedure is applied.

An explicit filtering of the horizontal velocity field is performed using the following simple approach

$$\begin{aligned} u_i &= (1 - f)u_i + f\bar{u}_i \\ v_i &= (1 - f)v_i + f\bar{v}_i \end{aligned} \tag{3.44}$$

where  $(u_i, v_i)$  is the horizontal velocity components in element  $i$ ,  $(\bar{u}_i, \bar{v}_i)$  is the mean velocity components calculated as an area-weighted mean value of the discrete velocity components in element  $i$  and the neighboring elements.  $f$  is a filter factor. A typical value of the filter factor is in the range from 0.001 to 0.02. The filtering is performed at each stage in the time integration.

### 3.3.2 Flooding and drying

The approach for treatment of the moving boundaries (flooding and drying fronts) problem is based on the work by Zhao et al. (1994) and Sleigh et al. (1998). When the depths are small the problem is reformulated, and only when the depths are very small the elements/cells are removed from the calculation. The reformulation is made by setting the momentum fluxes to zero and only taking the mass fluxes into consideration.

The depth in each element is monitored and the elements are classified as dry, partially dry or wet. Also, the element faces are monitored to identify flooded element faces.

- An element face is defined as flooded if the water depth at one side of a face is less than a tolerance depth,  $h_{dry}$ , and the water depth at the other side of the face is larger than a tolerance depth,  $h_{wet}$ .
- An element is dry if the water depth is less than a tolerance depth,  $h_{dry}$ , and none of the element faces are flooded faces. The element is removed from the calculation.
- An element is partially dry if the water depth is larger than  $h_{dry}$  and less than a tolerance depth,  $h_{wet}$ , or when the depth is less than  $h_{dry}$ , and one of the element faces is a flooded face. The momentum fluxes are set to zero, and only the mass fluxes are calculated.
- An element is wet if the water depth is bigger than  $h_{wet}$ . Both the mass flux and the momentum flux are calculated.

A non-physical flow across the face will be introduced for a flooded face when the surface elevation in the wet element on one side of the face is lower than the bed level in the

partially wet element on the other side. To overcome this problem the face will be treated as a closed boundary (Section 3.3.3).

In case the water depth becomes negative, the water depth is set to zero, and the water is subtracted from the adjacent elements to maintain mass balance. When this occurs the water depth at the adjacent elements may become negative. Therefore, an iterative correction of the water depth is applied (max. 100 iterations). Normally only one or a few correction steps are needed.

### 3.3.3 Boundary conditions

At the lateral closed (solid) boundaries, either a condition of zero velocity or a condition of zero normal velocity is imposed. A condition of zero velocity,  $u = v = w = 0$ , is also called a no-slip condition. For a condition with zero normal velocity,  $u_{\perp} = 0$ , the normal flux vector is

$$\mathbf{F}_n(\mathbf{U}) = \begin{pmatrix} 0 \\ \frac{1}{2}g(\eta^2 + 2\eta d)n_x \\ \frac{1}{2}g(\eta^2 + 2\eta d)n_y \\ 0 \end{pmatrix}, \quad \mathbf{F}_n(\mathbf{U}) = \begin{pmatrix} 0 \\ \frac{1}{2}g(\eta^2 + 2\eta d)n_x \\ \frac{1}{2}g(\eta^2 + 2\eta d)n_y \\ 0 \end{pmatrix} \quad (3.45)$$

for the Navier-stokes equations and the shallow water equations, respectively. For the zero normal velocity condition, a wall friction can be applied, see section 4.3. If the normal velocity is zero and there is no wall friction, the tangential stress is set to zero and this boundary condition is sometimes called a full-slip condition.

At the lateral open boundaries, a number of different boundary conditions can be applied.

The level boundary condition is imposed using a strong approach based on the characteristic theory (see e.g. Sleight et al., 1998).

The discharge boundary condition is imposed using both a strong approach based on the characteristic theory (see e.g. Sleight et al., 1998) and a weak formulation using ghost cell technique. For the ghost cell technique the primitive variables in the ghost cell are specified. The water level is evaluated based on the value of the adjacent interior cell, and the velocities are evaluated based on the boundary information. For a discharge boundary, the transverse velocity is set to zero for inflow and passively advected for outflow. The boundary flux is then calculated using an approximate Riemann solver. Note that using the weak formulation for a discharge boundary the effective discharge over the boundary may deviate from the specified discharge.

The free outflow boundary condition is also imposed using a weak approach. The primitive variables in the ghost cell are evaluated based on the value of the adjacent interior cell. A simple Neumann condition is applied where the gradient of the water level and velocities are zero.

The flux, velocity and Flather boundary conditions are all imposed using a weak approach. The Flather (1976) condition is one of the most efficient open boundary conditions. It is very efficient in connection with downscaling coarse model simulations to local areas (see Oddo and Pinardi (2007)). The instabilities, which are often observed when imposing stratified density at a water level boundary, can be avoided using Flather conditions.

At lateral closed boundaries and open boundaries the normal pressure gradient is zero.

## 3.4 Numerical solution of the transport equations

### 3.4.1 Time integration

The time integration is performed using either a first order explicit Euler method or a second-order explicit Runge-Kutta scheme (the midpoint method). However, to overcome the severe time step restriction due to small vertical grid spacing, the vertical convective and diffusive terms are treated implicitly. The vertical diffusion term is treated using a second order implicit trapezoidal method. The vertical convective term is treated either using the explicit method or an implicit Euler method, and the same method is used for all discrete equations in a column of the 3D mesh. The explicit method is used when the following criteria are satisfied

Sigma domain

$$\frac{\omega_i \Delta t}{\Delta \sigma_i} < \frac{1}{2} \quad (3.46)$$

z-level domain

$$\frac{w_i \Delta t}{\Delta z_i} < \frac{1}{2} \quad (3.47)$$

for all elements in the column. Here  $\omega_i$  is the modified vertical velocity and  $\Delta \sigma_i$  the vertical grid spacing in the sigma domain.  $w_i$  is the vertical velocity and  $\Delta z_i$  the vertical grid spacing in the z-level domain. Finally,  $\Delta t$  is the discrete time step interval. For details of the time integration methods, see Lambert (1973) and Hirsch (1990).

Due to the explicit scheme, the time step interval,  $\Delta t$ , is restricted by the Courant-Friedrichs-Lewy (CFL) condition

$$C = \Delta t \frac{|u| + |v|}{\Delta l} \leq C_{max} \quad (3.48)$$

where  $C$  is the Courant number and  $\Delta l$  is a characteristic length.  $C_{max}$  is the maximum Courant number and must be less than or equal to 1. A variable time step interval is used in the time integration of the transport equations for temperature and salinity and the transport equation for a scalar quantity and determined so that the Courant number is less than a maximum Courant number in all computational nodes. The characteristic length for a prism, where the horizontal face is a quadrilateral element, is determined as the area of the element divided by the longest edge length of the element. If the horizontal face is a triangular element, the characteristic length is two times the area divided by the longest edge length. The transport equations for the turbulence model are solved using the same time step as used for solving the flow equations.

### 3.4.2 Spatial discretization

Using the first-order scheme for the spatial discretization the normal flux due to the convective terms at the (vertical) faces is calculated using simple upwinding. It is calculated as the mass flux times the concentration at the element in the upwind direction. The numerical damping using the first order scheme is quite high. The advantage is that there is no overshooting or undershooting, which for some applications is very important.



Using the second-order scheme for the spatial discretization a higher-order upwind scheme is applied. The concentration at the (vertical) faces is determined using a linear gradient reconstruction technique based on the concentration and the gradient of the concentration at the element in the upwind direction. The gradient is determined using a wide computational stencil (see section 3.2). To provide stability and minimize oscillatory effects, the gradient limiter proposed by Barth and Jespersen (1989) is applied to limit the horizontal gradients. This approach significantly reduces the numerical damping compared to the first-order scheme.

When the explicit time integration approach is used for the vertical convective terms, the calculation of the normal flux due to the convective terms at the horizontal faces is performed using a 3<sup>rd</sup> order ENO procedure (Shu, 1997). When the implicit time integration approach is used for the vertical convective terms the normal flux is calculated using a first-order upwinding scheme.

### 3.4.3 Boundary conditions

For lateral closed (solid) boundaries the normal convective flux is zero, and the normal gradient of the transport variables is zero.

For lateral open boundaries either a specified value or a zero gradient can be given. For specified values, the boundary conditions are imposed by applying the specified concentrations for calculation of the boundary flux. For a zero gradient condition, the concentration at the boundary is assumed to be identical to the concentration at the adjacent interior cell.

Solving the transport equations for the turbulence model, the lateral closed boundary conditions depend on the boundary conditions for the flow equations. In case of no-slip condition or in case of zero normal velocity where wall friction is applied, a Dirichlet boundary condition is applied. The values in the elements at the wall are calculated using the wall functions in eq. (2.79). In this case,  $\Delta y = \Delta y_w$  is the distance to the wall from the center of the elements and  $U_\tau = U_{\tau w}$  is the friction velocity associated with the wall stress, see section 4.3. In case of zero normal velocity without wall friction, the normal convective flux is zero, and the normal gradient of the transport variables is zero.

## 3.5 Time stepping procedure

The solution is determined at a sequence of discrete times

$$t^k = t^0 + k\Delta t_{overall} \quad k = 0, 1, 2, 3 \dots \quad (3.49)$$

where  $\Delta t_{overall}$  is the overall time step interval. The time steps for the hydrodynamic (flow) calculations and the advection-dispersion (transport) calculations are dynamic. The time step procedure is illustrated in Figure 3.8.

For the advection-dispersion (AD) calculations the new time step interval,  $\Delta t_{AD}$ , is determined using the following procedure

$$\Delta t_{AD}^* = C_{max} \min \left( \frac{\Delta l}{(\sqrt{gh_i} + |u_i|) + (\sqrt{gh_i} + |v_i|)} \right) \quad (3.50)$$

$$\Delta t_{AD}^{**} = \min ( \max(\Delta t_{AD}^*, \Delta t_{AD,min}), \Delta t_{AD,max} ) \quad (3.51)$$

$$\Delta t_{AD} = \frac{t^k - t_{AD}}{\text{int}\left(\frac{(t^k - t_{AD})}{\Delta t_{AD}^{**}}\right) + 1} \quad (3.52)$$

Here  $t_{AD}$  is the actual time for the advection-dispersion calculations, where  $t^{k-1} < t_{AD} \leq t^k$ .  $\Delta t_{AD,min}$  and  $\Delta t_{AD,max}$  are the minimum and maximum time step intervals, respectively, and  $\text{int}$  is the whole number of  $(t^k - t_{AD})/\Delta t_{AD}^{**}$ . This procedure secures that the time steps for the advection-dispersion calculations are synchronized at the overall discrete time steps.

For the hydrodynamic (HD) calculations the new time step interval,  $\Delta t_{HD}$ , is determined using the following procedure

$$\Delta t_{HD}^* = C_{max} \min\left(\frac{\Delta l}{|u_i| + |v_i|}\right) \quad (3.53)$$

$$\Delta t_{HD}^{**} = \min(\max(\Delta t_{HD}^*, \Delta t_{HD,min}), \Delta t_{HD,max}) \quad (3.54)$$

$$\Delta t_{HD} = \frac{(t_{AD} + \Delta t_{AD}) - t_{HD}}{\text{int}\left(\frac{((t_{AD} + \Delta t_{AD}) - t_{HD})}{\Delta t_{HD}^{**}}\right) + 1} \quad (3.55)$$

Here  $t_{HD}$  is the actual time for the hydrodynamic calculations, where  $t_{AD} < t_{HD} \leq t_{AD} + \Delta t_{AD}$ .  $\Delta t_{HD,min}$  and  $\Delta t_{HD,max}$  are the minimum and maximum time step intervals, respectively. This procedure secures that the time steps for the hydrodynamic calculations are synchronized at the advection-dispersion time steps.

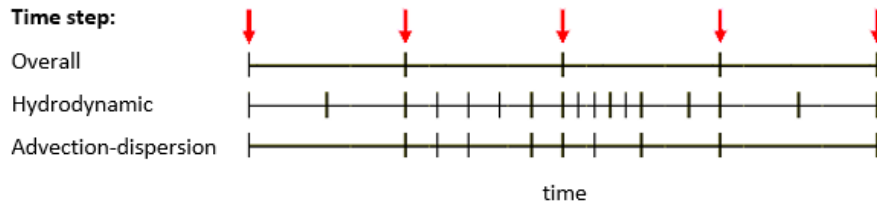


Figure 3.8 Time stepping procedure

## 4 Physics

### 4.1 Eddy viscosity

Both the vertical and horizontal eddy viscosity can be derived solving a turbulence closure model (see section 2.1.4). In that case the eddy viscosity is calculated using eq. (2.34) or (2.59). In some applications, a constant eddy viscosity can be used for the horizontal eddy viscosity. Alternatively, Smagorinsky (1963) proposed to express sub-grid scale transports by an effective eddy viscosity related to a characteristic length scale. The sub-grid scale eddy viscosity is given by

$$\nu_t^h = c_s^2 l^2 \sqrt{2(S_{xx}S_{xx} + 2S_{xy}S_{xy} + S_{yy}S_{yy})} \quad (4.1)$$

where  $c_s$  is a constant,  $l$  is a characteristic length and the deformation rate is given by

$$S_{xx} = \frac{\partial u}{\partial x} \quad S_{xy} = \frac{1}{2} \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \quad S_{yy} = \frac{\partial v}{\partial y} \quad (4.2)$$

For more details on this formulation, the reader is referred to Lilly (1967), Leonard (1974), Aupoix (1984), and Horiuti (1987).

The vertical eddy viscosity derived from the log-law can also in some cases be applied. Here the eddy viscosity is calculated by

$$\nu_t^v = U_\tau h \left( c_1 \frac{z+d}{h} + c_2 \left( \frac{z+d}{h} \right)^2 \right) \quad (4.3)$$

where  $U_\tau = \max(U_{\tau s}, U_{\tau b})$  and  $c_1$  and  $c_2$  are two constants.  $U_{\tau s}$  and  $U_{\tau b}$  are the friction velocities associated with the surface and bottom stresses,  $c_1 = 0.41$  and  $c_2 = -0.41$  give the standard parabolic profile.

In applications with stratification, the effects of buoyancy can be included explicitly. This is done through the introduction of a Richardson number dependent damping of the eddy viscosity coefficient, when a stable stratification occurs. The damping is a generalization of the Munk-Anderson formulation (Munk and Anderson, 1948)

$$\nu_t^v = (\nu^*)^v (1 + a Ri)^{-b} \quad (4.4)$$

where  $(\nu^*)^v$  is the undamped eddy viscosity and  $Ri$  is the local gradient Richardson number

$$Ri = -\frac{g}{\rho_0} \frac{\partial \rho}{\partial z} \left( \left( \frac{\partial u}{\partial z} \right)^2 + \left( \frac{\partial v}{\partial z} \right)^2 \right)^{-1} \quad (4.5)$$

and  $a = 10$  and  $b = 0.5$  are empirical constants.

### 4.2 Bed resistance

The bottom stress,  $\tau_b = (\tau_{bx}, \tau_{by})$  is determined by a quadratic friction law

$$\tau_b = \rho_0 c_f \mathbf{u}_b |\mathbf{u}_b| \quad (4.6)$$

where  $c_f$  is the drag coefficient, and,  $\mathbf{u}_b$  the flow velocity tangential to the seabed at a distance  $\Delta z_b$  above the bed. For the shallow water equations, the normal velocity at the bed is assumed to be zero. The drag coefficient is determined by assuming a logarithmic profile between the seabed and a point  $\Delta z_b$  above the seabed

$$c_f = \frac{1}{\left(\frac{1}{\kappa} \ln \left( \max \left( \frac{\Delta z_b}{z_0}, 2 \right) \right)\right)^2} \quad (4.7)$$

where  $\kappa = 0.41$  is the von Kármán constant, and  $z_0$  is the bed roughness length scale. When the boundary surface is rough,  $z_0$  depends on the roughness height,  $k_s$ , through

$$z_0 = mk_s \quad (4.8)$$

where  $m$  is approximately 1/30.

The friction velocity associated with the bottom stress is given by

$$U_{\tau b} = \sqrt{c_f |\mathbf{u}_b|^2} \quad (4.9)$$

The increase in bed resistance felt by the current due to the presence of the waves can be taken into account by calculating a Manning number,  $M$ , given the grain diameter and the relative density of the bed material. Here the model for the wave boundary layer in combined wave-current motion proposed by Fredsøe (1994) is applied. For a detailed description of the wave induced bed resistance see also Jones et. al (2014). The roughness height can then be estimated using the following expression

$$k_s = \left( \frac{25.4}{M} \right)^6 \quad (4.10)$$

A semi-implicit discretization is used to get a stable solution for small water depths, which for element  $i$  reads

First stage:

$$\frac{\tau_{bi}^{n+1/2}}{\rho_0} = c_f^n |\mathbf{u}_i^n| \mathbf{u}_i^* \quad (4.11)$$

Second stage:

$$\frac{\tau_{bi}^{n+1}}{\rho_0} = c_f^n |\mathbf{u}_i^{n+1/2}| \mathbf{u}_i^* \quad (4.12)$$

Here the \* indicates the provisional value of the velocity.

### 4.3 Wall friction

For closed lateral boundary with zero normal velocity and wall friction, the stress  $\tau_w$  tangential to the wall is determined by a quadratic friction law

$$\tau_w = \rho_0 c_f \mathbf{u}_{wall} |\mathbf{u}_{wall}| \quad (4.13)$$

Here,  $c_f$  is the drag coefficient and  $\mathbf{u}_{wall}$  is the velocity tangential to the wall at a distance  $\Delta y_w$  to the wall;  $\mathbf{u}_{wall}$  and  $\Delta y_w$  are evaluated at the cell center. The drag coefficient is given by

$$c_f = \frac{1}{\left( \frac{1}{\kappa} \ln \left( \max \left( \frac{\Delta y_w}{y_0}, 2 \right) \right) \right)^2} \quad (4.14)$$

where  $\kappa = 0.41$  is the von Kármán constant and  $y_0$  is the wall roughness length scale given by

$$y_0 = mk_s \quad (4.15)$$

The parameter  $k_s$  is a wall roughness height and  $m \approx 1/30$ . Furthermore, the friction velocity  $U_{\tau w}$  at the wall is determined as follows (Fuhrman et. al. (2014)).

$$U_{\tau w} = \sqrt{c_f |\mathbf{u}_{wall}|^2} \quad (4.16)$$

For a closed lateral boundary with zero velocity (i.e., a no-slip condition), the friction velocity can be determined using the law of the wall (Bredberg (2008), Wilcox (1998))

$$\frac{|\mathbf{u}_{wall}|}{U_{\tau w}} = \frac{1}{\kappa} \ln \left( \frac{U_{\tau w} \Delta y_w}{\nu} \right) + B \quad (4.17)$$

Here,  $\nu$  is the kinematic viscosity of water and  $B = 5.1$  is an empirically determined constant. Eq. (4.17) is solved iteratively to find  $U_{\tau w}$ , the friction velocity at the wall, and this value can be used in the boundary conditions of the turbulence models described in section 2.1.4.

## 4.4 Vegetation

The vegetation structure is modelled as rigid or flexible stems with stem diameter,  $d_s$ , or as flexible blades (leaves) with blade width,  $w_b$ , and blade thickness,  $t_b$ . The height of the vegetation is  $h_v$ .

The effect of the vegetation on the flow characteristics is modelled by inclusion of the following drag force in the momentum equations

$$\mathbf{F}_v = \frac{1}{2} C_D \lambda \mathbf{u} |\mathbf{u}| \quad (4.18)$$

where  $C_D$  is the drag coefficient,  $\lambda$  is the frontal area per volume and  $\mathbf{u}$  is the flow velocity vector. Here  $\lambda = b_v N_v$ , where  $b_v$  is the plant size, and  $N_v$  is the vegetation density. The plant size is either the stem diameter or the blade width. The vegetation density is the number of plants per unit area. For the Naier-Stokes equations the force in the vertical direction can be neglected when the vegetation structure is vertical stem or blades.

For rigid stems a layered approach can be used to take into account the vertical variation of the vegetation. The drag coefficient,  $C_{D,i}$ , the stem diameter,  $d_{s,i}$ , the vegetation height,  $h_{v,i}$ , and the vegetation density,  $N_{v,i}$ , is then specified for each vertical layer,  $i$ . The vegetation height is the distance from the bed to the top of the vegetation layer.

The reduction of the drag due to flexibility of the vegetation is taken into account using the approach by Luhar and Nepf (2011, 2013). They suggested the use of a deflected height,  $h_d$ , and an effective length,  $l_e$ . The effective length is defined as the length of a rigid vertical plant that generates the same drag as the total length of a flexible plant. The deflected height and the effective length are given by

$$\frac{h_d}{h_v} = 1 - \frac{1 - Ca^{-1/4}}{1 + Ca^{-3/5}(4 + B^{3/5}) + Ca^{-2}(8 + B^2)} \quad (4.19)$$

$$\frac{l_e}{h_v} = 1 - \frac{1 - 0.9Ca^{-1/3}}{1 + Ca^{-3/2}(8 + B^{3/2})} \quad (4.20)$$

where  $Ca$  is the Cauchy number and  $B$  is the buoyancy parameter

$$Ca = \frac{\rho A |\mathbf{u}_v|^2}{EI/h_v^2} \quad B = \frac{(\rho - \rho_v)gV_p}{EI/h_v^2} \quad (4.21)$$

Here  $g$  is the gravitational acceleration,  $\rho$  is the density of water,  $\rho_v$  is the density of the plant,  $E$  is the elastic modulus for the plant,  $A$  is the frontal area,  $V_p$  is the volume of the plant element and  $I$  is the second moment of the area. For a circular stem

$$A = d_s h_v \quad V_p = d_s^2 h_v / 4 \quad I = \pi d_s^4 / 64 \quad (4.22)$$

and for a blade

$$A = w_b h_v \quad V_p = w_b t_b h_v \quad I = w_b t_b^3 / 12 \quad (4.23)$$

The flexibility is taken into account by introducing a factor  $l_e/h_d$  in Eq. (4.18).

For the turbulence model the production term due to vegetation is given by

$$P_v = \frac{1}{2} C_D \lambda |\mathbf{u}|^3 \quad (4.24)$$

Following Lopez and Garcia (1998) the weighting coefficient using the k- $\epsilon$  model is set to  $c_{fk} = 1$  and  $c_{f\epsilon} = c_{2\epsilon}/c_{1\epsilon}$ . With the default values for  $c_{1\epsilon}$  and  $c_{2\epsilon}$  then  $c_{f\epsilon} = 1.33$ . Using the k- $\omega$  model the default values for both  $c_{fk}$  and  $c_{f\epsilon}$  are set to 1.

## 4.5 Wind forcing

In areas not covered by ice the surface stress,  $\boldsymbol{\tau}_s = (\tau_{sx}, \tau_{sy})$ , is determined by the winds above the surface. The stress is given by the following empirical relation

$$\boldsymbol{\tau}_s = \rho_a c_d \mathbf{u}_w |\mathbf{u}_w| \quad (4.25)$$

where  $\rho_a$  is the density of air,  $c_d$  is the drag coefficient of air, and  $\mathbf{u}_w = (u_w, v_w)$  is the wind speed 10 m above the sea surface. The friction velocity associated with the surface stress is given by

$$U_{\tau s} = \sqrt{\frac{\rho_a c_d |\mathbf{u}_w|^2}{\rho_0}} \quad (4.26)$$

The drag coefficient can either be a constant value or depend on the wind speed. The empirical formula proposed by Wu (1980, 1994) is used for the parameterization of the drag coefficient

$$c_d = \begin{cases} c_a & W_{10} < W_a \\ c_a + \frac{c_b - c_a}{W_b - W_a} (W_{10} - W_a) & W_a \leq W_{10} < W_b \\ c_b & W_{10} \geq W_b \end{cases} \quad (4.27)$$

where  $c_a$ ,  $c_b$ ,  $W_a$  and  $W_b$  are empirical factors and  $W_{10}$  is the wind velocity 10 m above the sea surface. The default values for the empirical factors are  $c_a = 1.255 \cdot 10^{-3}$ ,  $c_b = 2.425 \cdot 10^{-3}$ ,  $W_a = 7 \text{ m/s}$  and  $W_b = 25 \text{ m/s}$ . These give generally good results for open sea applications. Field measurements of the drag coefficient collected over lakes indicate that the drag coefficient is larger than open ocean data. For a detailed description of the drag coefficient see Geernaert and Plant (1990).

## 4.6 Ice coverage

It is possible to take into account the effects of ice coverage on the flow field.

In areas where the sea is covered by ice the wind stress is excluded. Instead, the surface stress is caused by the ice roughness. The surface stress,  $\tau_s = (\tau_{sx}, \tau_{sy})$ , is determined by a quadratic friction law

$$\tau_s = \rho_0 c_f \mathbf{u}_s |\mathbf{u}_s| \quad (4.28)$$

where  $c_f$  is the drag coefficient and  $\mathbf{u}_s = (u_s, v_s)$  is the flow velocity at a distance  $\Delta z_s$  below the surface. The drag coefficient is determined by assuming a logarithmic profile between the surface and a point  $\Delta z_s$  below the surface

$$c_f = \frac{1}{\left( \frac{1}{\kappa} \ln \left( \max \left( \frac{\Delta z_s}{z_0}, 2 \right) \right) \right)^2} \quad (4.29)$$

where  $\kappa = 0.41$  is the von Kármán constant, and  $z_0$  is the ice roughness length scale. When the boundary surface is rough,  $z_0$ , depends on the ice roughness height,  $k_s$ , through

$$z_0 = m k_s \quad (4.30)$$

where  $m$  is approximately 1/30.

The friction velocity associated with the surface stress is given by

$$U_{\tau s} = \sqrt{c_f |\mathbf{u}_s|^2} \quad (4.31)$$

A semi-implicit discretization is used to get a stable solution for small water depths, which for element  $i$  reads

First stage:

$$\frac{\tau_{si}^{n+1/2}}{\rho_0} = c_f^n |\mathbf{u}_i^n| \mathbf{u}_i^* \quad (4.32)$$

Second stage:

$$\frac{\tau_{si}^{n+1}}{\rho_0} = c_f^n |\mathbf{u}_i^{n+1/2}| \mathbf{u}_i^* \quad (4.33)$$

If ice thickness is specified, the water level is suppressed by  $\rho_{ice}/\rho_{water}$  of the ice thickness, where  $\rho_{ice} = 971 \text{ kg/m}^3$  and  $\rho_{water}$  is the actual density of the water.

## 4.7 Tidal potential

The tidal potential is a force, generated by the variations in gravity due to the relative motion of the earth, the moon and the sun that act throughout the computational domain. The forcing is expanded in frequency space and the potential considered as the sum of a number of terms each representing different tidal constituents. The forcing is implemented as a so-called equilibrium tide, which can be seen as the elevation that theoretically would occur, provided the earth was covered with water. The forcing enters the momentum equations as an additional term representing the gradient of the equilibrium tidal elevations, such that the elevation  $\eta$  can be seen as the sum of the actual elevation and the equilibrium tidal potential.

$$\eta = \eta_{actual} + \eta_T \quad (4.34)$$

The equilibrium tidal potential  $\eta_T$  is given as

$$\eta_T = \sum_i e_i H_i f_i L_i \cos\left(2\pi \frac{t}{T_i} + b_i + i_0 x\right) \quad (4.35)$$

where  $\eta_T$  is the equilibrium tidal potential,  $i$  refers to constituent number (note that the constituents here are numbered sequentially),  $e_i$  is a correction for earth tides based on Love numbers,  $H_i$ , is the amplitude,  $f_i$ , is a nodal factor,  $L_i$ , is given below,  $t$  is time,  $T_i$ , is the period of the constituent,  $b_i$ , is the phase and  $x$  is the longitude of the actual position.

The phase  $b$  is based on the motion of the moon and the sun relative to the earth and can be given by

$$b_i = (i_1 - i_0)s + (i_2 - i_0)h + i_3p + i_4N + i_5p_s + u_i \sin(N) \quad (4.36)$$

where  $i_0$  is the species,  $i_1$  to  $i_5$  are Doodson numbers,  $u$  is a nodal modulation factor (see Table 4.2) and the astronomical arguments  $s$ ,  $h$ ,  $p$ ,  $N$  and  $P_s$  are given in Table 4.1.

Table 4.1 Astronomical arguments (Pugh, 1987)

Mean longitude of the moon	$s$	$277.02+481267.89T+0.0011T^2$
Mean longitude of the sun	$h$	$280.19+36000.77T+0.0003T^2$
Longitude of lunar perigee	$p$	$334.39+4069.04T-0.0103T^2$
Longitude of lunar ascending node	$N$	$259.16-1934.14T+0.0021T^2$
Longitude of perihelion	$p_s$	$281.22+1.72T+0.0005T^2$



In Table 4.1 the time,  $T$ , is in Julian century from January 1 1900 UTC, thus  $T = (365(y - 1900) + (d - 1) + i)/36525$  and  $i = \text{int}(y - 1901)/4$ ,  $y$  is year and  $d$  is day number

$L$  depends on species number  $i_0$  and latitude  $\phi$  as

$$\begin{aligned} i_0 = 0: L &= 3\sin^2(\phi) - 1 \\ i_0 = 1: L &= \sin(2\phi) \\ i_0 = 2: L &= \cos^2(\phi) \end{aligned}$$

The nodal factor  $f_i$  represents modulations to the harmonic analysis and can for some constituents be given as shown in Table 4.2.

Table 4.2 Nodal modulation terms (Pugh, 1987)

Symbol	$f_i$	$u_i$
$M_m$	$1.000 - 0.130 \cos(N)$	$0$
$M_f$	$1.043 + 0.414 \cos(N)$	$-23.7 \sin(N)$
$Q_1, O_1$	$1.009 + 0.187 \cos(N)$	$10.8 \sin(N)$
$K_1$	$1.006 + 0.115 \cos(N)$	$-8.9 \sin(N)$
$2N_2, \mu_2, v_2, N_2, M_2$	$1.000 - 0.037 \cos(N)$	$-2.1 \sin(N)$
$K_2$	$1.024 + 0.286 \cos(N)$	$-17.7 \sin(N)$

## 4.8 Precipitation and evaporation

In applications where the rainfall is important for the flow, the precipitation rate,  $\hat{P}$ , can be specified. When heat exchange from the atmosphere is included, the evaporation rate is defined as

$$\hat{E} = \begin{cases} \frac{q_v}{\rho_0 l_v} & q_v > 0 \\ 0 & q_v \leq 0 \end{cases} \quad (4.37)$$

where  $q_v$  is the latent heat flux (see section 4.12.1) and  $l_v$  is the latent heat of vaporization of water.

Precipitation and evaporation are implemented as a simple source (see section 4.11) in all surface elements in the computational domain. The discharge in element  $i$  is calculated as

$$Q_i = A_i(\hat{P} - \hat{E}) \quad (4.38)$$

where  $A_i$  is the horizontal area of the element.

For the transport equations for temperature and salinity the water precipitated and evaporated is assumed to be fresh water at the ambient water temperature (the temperature in element  $i$ ). For the transport equations for a scalar quantity the concentration is assumed to be the ambient concentration. For precipitation it is also possible to specify the temperature and the concentration of the water flowing into the

computation domain. Precipitation and evaporation are not included in the transport equation for the  $k-\varepsilon$  model.

## 4.9 Infiltration

The effect of infiltration at the surface zone may be important in cases of flooding scenarios on otherwise dry land. It is possible to account for this in one of two ways: by net infiltration rates or by constant infiltration with capacity.

Infiltration is implemented as a simple source (see section 4.11) in all bottom elements in the computational domain. The discharge in element  $i$  is calculated as

$$Q_i = -A_i Q_{net} \quad (4.39)$$

where  $A_i$  is the horizontal area of the element and  $Q_{net}$  is the net infiltration rate.

For the transport equations for temperature and salinity the water infiltration is assumed to be fresh water at the ambient water temperature (the temperature in element  $i$ ). For the transport equations for a scalar quantity the concentration is assumed to be the ambient concentration. For positive discharge it is also possible to specify the temperature and the concentration of the water flowing into the computation domain. Precipitation and evaporation are not included in the transport equation for the  $k-\varepsilon$  model.

### 4.9.1 Net infiltration rates

The net infiltration rate is defined directly. When using net infiltration rate an unsaturated zone is never specified and thus has no capacity limits, so the specified infiltration rates will always be fully effectuated if there is enough water available in the element.

### 4.9.2 Constant infiltration with capacity

Constant infiltration with capacity describes the infiltration from the free surface zone to the unsaturated zone and from the unsaturated zone to the saturated zone by a simplified model (see Figure 4.1). The model assumes the following:

- The unsaturated zone is modelled as an infiltration zone with constant porosity over the full depth of the zone.
- The flow between the free surface zone and the infiltration zone is based on a constant flow rate,  $Q_i$ .
- The flow between the saturated and unsaturated zone is modelled as a leakage having a constant flow rate,  $Q_l$ .

The simplified model described above is solved through a one-dimensional continuity equation for the unsaturated zone. Feedback from the infiltration and leakage to the two-dimensional horizontal hydrodynamic calculations is based solely on changes to the depth of the free surface zone – the water depth.

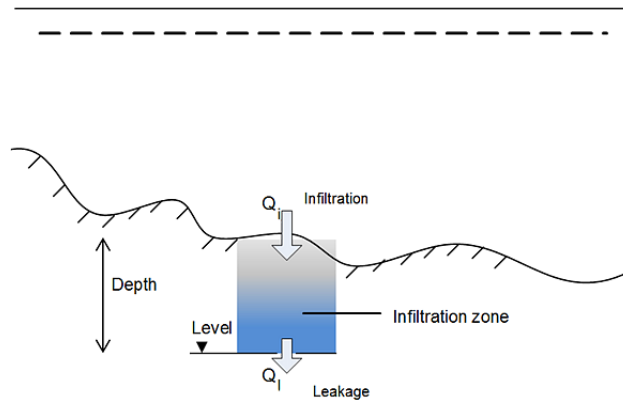


Figure 4.1 Illustration of infiltration process

## 4.10 Wave Radiation

The radiation stress is the depth-integrated excess momentum flux due to the breaking of the short period waves. The radiation stresses act as driving forces for the mean flow and can be used to calculate wave setup and wave induced currents. For 3D simulations a simple approach is used. Here a uniform variation is used for the vertical variation in radiation stress.

$$F_x = \frac{1}{\rho_0 h} \left( \frac{\partial S_{xx}}{\partial x} + \frac{\partial S_{xy}}{\partial y} \right) \quad F_y = \frac{1}{\rho_0 h} \left( \frac{\partial S_{xy}}{\partial x} + \frac{\partial S_{yy}}{\partial y} \right) \quad F_z = 0 \quad (4.40)$$

where  $S_{xx}$ ,  $S_{xy}$ , and  $S_{yy}$  are components of the second order radiation stress tensor.

## 4.11 Sources

There are four types of sources

- Simple source
- Standard source
- Connected source
- Jet source

For a simple source the discharge,  $Q$ , is specified. If the source is located in element  $i$  with the volume  $V_i$  the following source term is added to the discrete continuity equation

$$S_i = \frac{Q}{V_i} \quad (4.41)$$

A source where the discharge is negative is also called a sink. For a simple source the mass enters the flow without momentum. The mass will therefore have to be accelerated, and this may cause a drop in the local velocity. For a standard source a source of momentum is also included. The following terms are added to the discrete momentum equations

$$F_{x,i} = u_s \frac{Q}{V_i} \quad F_{y,i} = v_s \frac{Q}{V_i} \quad F_{z,i} = w_s \frac{Q}{V_i} \quad (4.42)$$

where  $u_s$  and  $v_s$  are the source velocities. The contribution to the momentum equation is only taken into account when the magnitude of the source is positive (water is discharge into the ambient). A connected source is a standard source where the magnitude of the discharge is obtained as the magnitude of the discharge specified for source which the source is connected to, but with opposite sign. The jet source is described in the next section.

For the transport equations a source term is also added to the discrete equation. The source term is  $S_i$  times a value for the transported variable. This can be a specified value or the value in the element where the source is located plus an excess value. Sources are not included in the transport equation for the  $k-\varepsilon$  model.

#### 4.11.1 Jet sources

The simulation of jets/plumes is based on dynamic coupling of a nearfield integrated jet solution and the farfield hydrodynamic flow model (MIKE 3 Flow Model FM).

##### Nearfield calculation

The nearfield solution is based on the integral jet model equations described by Jirka (2004). It determines the steady state solution of the jet/plume by solving conservation equations for flux and momentum, salinity and temperature (if included) under the given ambient conditions.

The velocity profile and distribution of state parameters and scalar mass is assumed to follow the Gaussian formulation. The jet model employs an entrainment closure approach that distinguishes between the separate contributions of transverse shear and of azimuthal shear mechanisms. It further contains a quadratic law turbulent drag force mechanism,  $F_D$ , as suggested by a number of recent detailed experimental investigations on the dynamics of transverse jets into crossflow. The conservation principles for volume (continuity), momentum components in the global directions, state parameters and scalar mass, follow Jirka (2004), lead to the following equations

$$\frac{dQ}{ds} = E \quad (4.43)$$

$$\frac{dM_x}{ds} = Eu_a + F_D \sqrt{1 - \cos^2 \theta \cos^2 \sigma} \quad (4.44)$$

$$\frac{dM_y}{ds} = -F_D \frac{\cos^2 \theta \sin \sigma \cos \sigma}{\sqrt{1 - \cos^2 \theta \cos^2 \sigma}} \quad (4.45)$$

$$\frac{dM_z}{ds} = \pi \lambda^2 b^2 g'_c - F_D \frac{\sin \theta \cos \theta \cos \sigma}{\sqrt{1 - \cos^2 \theta \cos^2 \sigma}} \quad (4.46)$$

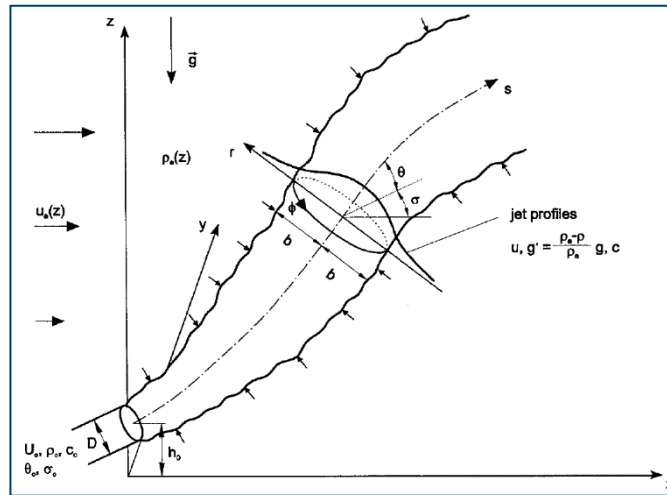


Figure 4.2 Nearfield jet integral model definition sketch

where  $s$  is the axial distance along the jet trajectory and  $E$  is the rate of entrainment, and  $b$  is the characteristic width of the jet, which is defined as the jet radius, where the jet excess velocity is  $e^{-1} = 37\%$ .  $\theta$  is the horizontal direction angle and  $\sigma$  is the vertical direction angle (relative to horizontal, with 90 degree indicating flow toward the surface).  $\lambda$  is an empirical constant which has the value 1.2. The centerline density is contained in the definition of centerline buoyancy  $g'_c$  and is calculated by the UNESCO equation of state, as function of salinity,  $s$ , and temperature,  $T$

$$\rho_{Jet} = \rho_{UNESCO}(T, s) \quad (4.47)$$

If sediments are present inside the jet, and their dynamics are included in the calculations, then the jet density will be corrected for the presence of sediments. This can be activated by defining the source in Mud Transport (MT) module and activating the MT-HD feedback.

$$\rho_{Jet} = (1 - C_{sed})\rho_{Jet} + C_{sed}\rho_{sed} \quad (4.48)$$

$C_{sed}$  is the volumetric sediment concentration derived from the sediment concentration provided by the user for the Jet source in MT module, and  $\rho_{sed}$  is the sediment density provided by the user for the MT-HD feedback in MT module. The buoyant acceleration is then defined as below, where  $\rho_a$  is the ambient density, and  $\rho_{ref}$  is the reference density calculated by the reference salinity and temperatures provided by the user in HD module.

$$g'_c = \frac{\rho_{Jet} - \rho_a}{\rho_{ref}} g \quad (4.49)$$

The two important physical processes influencing the jet trajectory and dilution rates are the entrainment rate,  $E$ , and the ambient drag force,  $F_D$ . The entrainment rate is calculated as being proportional to the streamwise contribution of the jet centerline velocity,  $u_c$ , plus the azimuthal contribution from the transverse component of the ambient velocity ( $u_a \sqrt{1 - \cos^2 \theta \cos^2 \sigma}$ ).

$$E = 2\pi b u_c \left( \alpha_1 + \alpha_2 \frac{\sin \theta}{F_l^2} + \alpha_3 \frac{u_a \cos \theta \cos \sigma}{u_c + u_a} \right) + 2\pi b u_a \sqrt{1 - \cos^2 \theta \cos^2 \sigma} \alpha_4 |\cos \theta \cos \sigma| \quad (4.50)$$

$F_l$  is the local densimetric Froude number, and is defined as:

$$F_l = \frac{u_c}{\sqrt{g'_c b}} \quad (4.51)$$

The first term in the streamwise part of the entrainment function represents the “pure jet” effects, the second term adds the effect of “pure plume” and the third term is for “pure wake”. The four coefficients defining the entrainment rate are given the empirical values suggested by Jirka (2004)

$$\alpha_1 = 0.055 \quad , \quad \alpha_2 = 0.6 \quad , \quad \alpha_3 = 0.055 \quad , \quad \alpha_4 = 0.5 \quad (4.52)$$

Deflection of the jet is a consequence of the pressure drag exerted on it by the cross flow,  $F_D$ , and of the entrainment by the jet of laterally moving fluid from the crossflow,  $E u_a$ . The drag force is parametrized as a quadratic law force mechanism (Jirka, 2004)

$$F_D = \frac{1}{2} C_D 2\sqrt{2} b u_a^2 (1 - \cos^2 \theta \cos^2 \sigma) \quad (4.53)$$

The jet diameter is calculated as  $2\sqrt{2}b$  and  $C_D$  is the drag coefficient as function of velocity ratio between jet and the ambient, following Chan et al. (1976).

Calculations of the jet trajectory are discretized based on the incremental distance along the jet trajectory ( $ds$ ). Following a recommendation from Lee and Cheung (1990), the spatial discretization of jet trajectory is calculated as below

$$\Delta s = \Delta t (u_c + u_a \cos \theta \cos \sigma) \quad (4.54)$$

where

$$\Delta t = \frac{0.1D}{u_c}$$

However, the value of  $\Delta t$  is set to have cut-off values of 0.001 seconds and 1.0 seconds.  $D$  is the initial jet diameter.

This jet (nearfield) model calculates the jet trajectory and dilution until it reaches the end of nearfield region. This is done at each hydrodynamic time step in the farfield flow model. Although the hydrodynamic time steps can be much smaller than the time it takes for the trajectory to reach the end of nearfield region, it is assumed that the temporal variations in the background flow (ambient) are slower than the time it takes for the jet to go from discharge point to the point of farfield release.

#### End of nearfield region

In general, where the jet loses its driving characteristics over the ambient flow (momentum and buoyancy), it has reached the end of its nearfield region and its volume and scalar mass can be transferred and dispersed by the ambient flow into the farfield region. This can happen under different circumstances:

- **Jet in cross-flow:** The jet momentum  $M$  is combination of its initial momentum at the diffuser, buoyancy and the ambient flow induced (co- or opposing) momentum  $M_a$ . It loses its driving characteristics over the ambient flow when the excess momentum becomes small, and close to the ambient flow momentum. This can be considered as the end of the nearfield region and the release into the farfield model by following the

condition:  $M - M_a < \varepsilon M_a$ , where epsilon  $\varepsilon$  is left as a user-defined/calibration parameter, with default value of 1%.

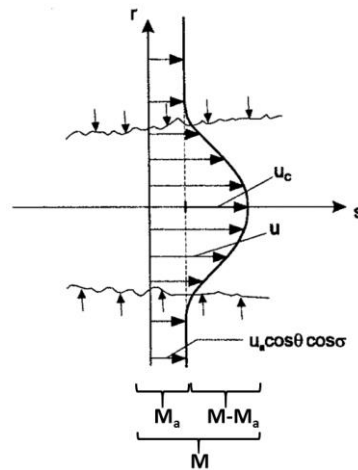


Figure 4.3 Illustration of the jet velocity field and the contribution from the ambient flow (Modified image from Jirka, 2004)

- Jet in stagnant environment:** Under stagnant conditions, the contribution from the ambient currents to the jet momentum is zero, and the nearfield region can extend until the point where the jet loses its own momentum due to dilution and buoyancy. Considering the modeling/numerical limitations, a minimum value for the jet excess velocity can be defined (gamma,  $\gamma$ ) to mark the end of nearfield region and the release into farfield model. The default value for gamma is set to 1 cm/s.
- Jet in stratified stagnant environment:** Non-horizontal jets (positively buoyant jets pointed downward or negatively buoyant jets pointed upward) in stagnant stratification create a complex situation. Depending on the stratification gradient and the jet initial momentum, the jet can either be trapped in a layer where its density equals the ambient density, or it overshoots and experiences a reversed buoyancy. In latter case, the jet experiences a lateral collapse in form of an internal density current formation in opposite direction and it ends up trapped in a terminal density level. These complex processes are not included in the integral jet model formulation and – in the absence of an adequate transition cut-off – it predicts (unrealistically) an infinite number of oscillations about the terminal level. Therefore, the second buoyancy reversal in the jet calculations is considered as the end of nearfield calculations and the release into the farfield model.
- Jet in strong opposing flow:** Jet integral models cannot be expected to hold for flow situations in which boundary layer behavior is no longer maintained. The boundary layer approximation implies a pressure within the jet equal to that in the outside ambient. This is violated whenever the jet exhibits strong curvature such as going into strong opposing ambient current. Therefore, the jet nearfield solution stops and releases into farfield model as soon as it experiences a strong opposing flow.

The other criterion that ends the nearfield calculations is when the jet reaches the bottom, surface or a lateral boundary. The dynamics of the jet approaching a solid boundary or water surface are not yet included in the nearfield calculations of the jet source. Among the impacts are variations in entrainment rates at the vicinity of the boundary. The nearfield calculations continue un-influenced until the jet reaches the boundary, and there it releases into the farfield model. Finally, the nearfield calculations are also stopped if the trajectory of the jet exceeds a maximum travel distance. The travel distance is here

defined as the distance in horizontal plane from the initial jet/plume position to the end position.

#### Nearfield-farfield model coupling

The coupling between the nearfield and farfield model concerns both the determination of ambient conditions as an input for the nearfield jet model, and the release of jet discharge into the farfield flow model at the end of the nearfield region.

The ambient flow conditions can be determined either as the local flow conditions at the jet location or as the upstream ambient flow conditions. The upstream option can be used to avoid unrealistic feedback between the jet solution and the ambient flow in cases with dominant advection effects on the released material from the ambient flow. For the upstream ambient flow condition, the conditions are obtained at a point defined by distance from the jet location in the upstream flow direction. The distance is the maximum of the characteristic length determined from the mesh and a user-specified minimum upstream distance. The characteristic length is here determined as 2.3 times the square root of the local element area at the initial release point.

At the end of nearfield region (determined by any of conditions described in previous section), the final jet discharge (which is diluted) is released into the farfield flow model by introducing a source at the final position of the trajectory. The increased jet discharge and (consequently) its dilution at the release point is a result of entrainment along its trajectory. Conservation of mass and volume in the farfield flow model then requires removing this excess mass and volume that have been inserted at the release point. This has been done by introducing entrainment sinks along the centerline of the jet trajectory (see Figure 4.4). This method follows the Distributed Entrainment Sink Approach (DESA) proposed by Choi and Lee (2007).

For each section in the jet calculation the entrainment of water (the volume flux) is calculated and is then introduced as a sink in the corresponding element in the far field model. If advection-dispersion calculation of temperature and salinity, passive substances, for cohesive or non-cohesive sediment transport or for ecological modelling (MIKE ECO Lab) is included in the simulation the tracer mass flux for the sinks is computed as the volume flux times the local solute concentration. The discharge of water at the final position of the jet is determined as the sum of the total entrained amount of ambient water and the specified effluent discharge. The tracer mass flux at the release point is determined as the sum of the entrainment tracer fluxes and the effluent discharge times the effluent tracer concentration. This approach for representing the jet/plume in the far field model secures conservation of water and tracer mass. A distribution of the released material in the far field model at the final position of the jet is applied to get the right dilution in the far field model. Here a Gaussian distribution is used covering a circular plane corresponding to the final jet radius and perpendicular to the jet trajectory at the final position of the jet. The number of sources depend on the mesh resolution in the farfield model. If the jet reaches the surface/bottom level, a uniform distribution is applied covering a circular area over the bed/surface corresponding to the final jet radius.

At the release point a forcing (momentum flux) is added to the momentum equation, in the direction of jet release into the ambient domain, calculated as

$$F_x = M \cos \theta \cos \sigma \quad F_y = M \cos \theta \sin \sigma \quad F_z = M \sin \theta \quad (4.55)$$

where  $M = \sqrt{M_x M_x + M_y M_y + M_z M_z}$ .



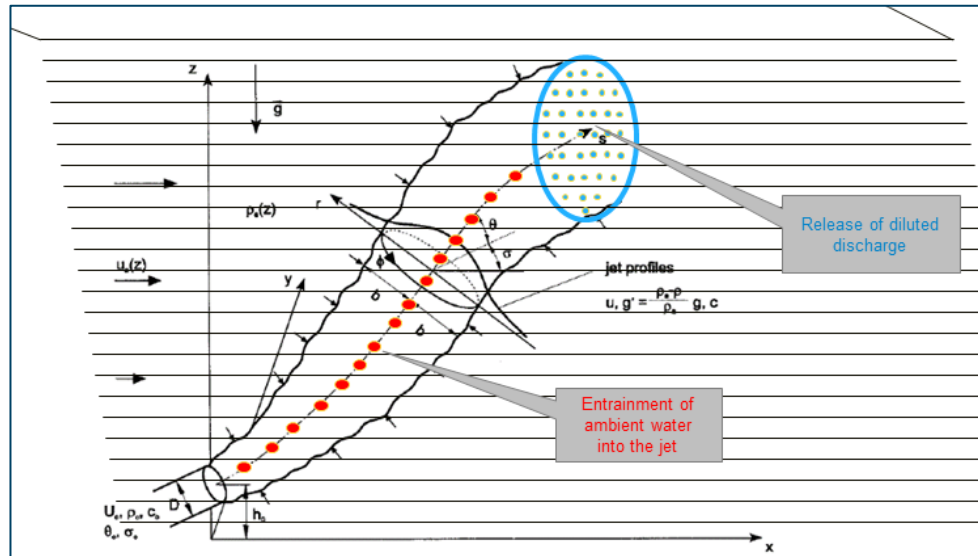


Figure 4.4 Illustration of positioning of entrainment sinks along the trajectory in a 3D domain, and the distributed source points at the release location

Correspondingly, at each sink point, a forcing (momentum flux), calculated as the product of sink rate,  $q_{sink}$ , and the ambient flow velocity,  $(u_a, v_a, w_a)$ , is added to the momentum balance with an opposing direction

$$m_x = -Q_{sink}u_a \quad m_y = -Q_{sink}v_a \quad m_z = -Q_{sink}w_a \quad (4.56)$$

## 4.12 Heat exchange

The heat exchange with the atmosphere is calculated on basis of the four physical processes

- Latent heat flux (or the heat loss due to vaporisation)
- Sensible heat flux (or the heat flux due to convection)
- Net short wave radiation
- Net long wave radiation

Latent and sensible heat fluxes and long wave radiation are assumed to occur at the water surface. A part of the net short wave radiation,  $q_{sr,net}$ , is absorbed at the surface and a part is absorbed in the water column. The short wave penetration in the water column depends on the visibility. The distribution of the net short wave radiation is approximated using Beer's law. The fraction of the short wave radiation that is absorbed near the surface is  $\beta q_{sr,net}$  and the remaining part  $(1 - \beta)q_{sr,net}$  is absorbed in the water column. The attenuation of the light intensity is described through the modified Beer's law as

$$I(d) = I_0 e^{-\lambda d} \quad (4.57)$$

where  $I(d)$  is the intensity at depth  $d$  below the surface,  $I_0$  is the intensity just below the water surface and  $\lambda$  is the light extinction coefficient. Typical values for  $\beta$  and  $\lambda$  are 0.2-0.6 and 0.5-1.4  $m^{-1}$ , respectively.  $\beta$  and  $\lambda$  are user-specified constants. The default values are  $\beta = 0.3$  and  $\lambda = 1.0 m^{-1}$ . Hence the surface net heat flux is given by

$$Q = q_v + q_c + \beta q_{sr,net} + q_{lr,net} \quad (4.58)$$

The calculation of the latent heat flux,  $q_v$ , sensible heat flux,  $q_c$ , net short wave radiation,  $q_{sr,net}$ , and net long wave radiation,  $q_{lr,net}$ , as described in the following sections. The absorption of heat in the water column is given by,  $H$ , is given by

$$H = \frac{\partial}{\partial z} \left( \frac{q_{sr,net}(1 - \beta)e^{-\lambda(\eta-z)}}{(1 - e^{-\lambda h})} \right) = \frac{q_{sr,net}(1 - \beta)\lambda e^{-\lambda(\eta-z)}}{(1 - e^{-\lambda h})} \quad (4.59)$$

where  $h$  is the total water depth.

In areas covered by ice the heat exchange with the atmosphere is excluded.

The heat in the water can also interact with the ground due to ground heat conduction.

#### 4.12.1 Vaporisation

Dalton's law yields the following relationship for the vaporative heat loss (or latent flux), see Sahlberg, 1984

$$q_v = LC_e(a_1 + b_1 W_{2m})(Q_{water} - Q_{air}) \quad (4.60)$$

where  $L = 2.5 \cdot 10^6 J/kg$  is the latent heat vaporisation (in the literature  $L = 2.5 \cdot 10^6 - 2300T_{water}$  is commonly used, where  $T_{water}$  is the temperature of the water);  $C_e = 1.32 \cdot 10^{-3}$  is the moisture transfer coefficient (or Dalton number);  $W_{2m}$  is the wind speed 2 m above the sea surface;  $Q_{water}$  is the water vapour density close to the surface;  $Q_{air}$  is the water vapour density in the atmosphere;  $a_1$  and  $b_1$  are user specified constants. The default values are  $a_1 = 0.5$  and  $b_1 = 0.9$ .

Measurements of  $Q_{water}$  and  $Q_{air}$  are not directly available but the vapour density can be related to the vapour pressure as

$$Q_i = \frac{0.2167}{T_i + T_k} e_i \quad (4.61)$$

in which subscript  $i$  refers to both water and air. The vapour pressure close to the sea,  $e_{water}$ , can be expressed in terms of the water temperature assuming that the air close to the surface is saturated and has the same temperature as the water

$$e_{water} = 6.11 \exp \left( k \left( \frac{1}{T_k} - \frac{1}{T_{water} + T_k} \right) \right) \quad (4.62)$$

where  $k = 5418^\circ K$  and  $T_k = 273.15^\circ K$  is the temperature at  $0^\circ C$ . Similarly the vapour pressure of the air,  $e_{air}$ , can be expressed in terms of the air temperature and the relative humidity,  $R$

$$e_{air} = R \cdot 6.11 \exp \left( k \left( \frac{1}{T_k} - \frac{1}{T_{air} + T_k} \right) \right) \quad (4.63)$$

Replacing  $Q_{water}$  and  $Q_{air}$  with these expressions the latent heat can be written as

$$q_v = -P_v(a_1 + b_1 W_{2m}) \left( \frac{\exp \left( k \left( \frac{1}{T_k} - \frac{1}{T_{water} + T_k} \right) \right)}{T_{water} + T_k} - \frac{R \cdot \exp \left( k \left( \frac{1}{T_k} - \frac{1}{T_{air} + T_k} \right) \right)}{T_{air} + T_k} \right) \quad (4.64)$$

where all constants have been included in a new latent constant  $P_v = 4370 J^\circ K/m^3$ . During cooling of the surface the latent heat loss has a major effect with typical values up to  $100 W/m^2$ .

The wind speed,  $W_2$ , 2 m above the sea surface is calculated from the wind speed,  $W_{10}$ , 10 m above the sea surface. Assuming a logarithmic profile the wind speed,  $u(z)$  at a distance  $z$  above the sea surface is given by

$$u(z) = \frac{u_*}{\kappa} \log \left( \frac{z}{z_0} \right) \quad (4.65)$$

where  $u_*$  is the wind friction velocity,  $z_0$  is the sea roughness and  $\kappa = 0.4$  is von Karman's constant.  $u_*$  and  $z_0$  are given by

$$z_0 = z_{Charnock} \frac{u_*}{g} \quad (4.66)$$

$$u_* = \frac{\kappa u(z)}{\log \left( \frac{z}{z_0} \right)} \quad (4.67)$$

where  $z_{Charnock}$  is the Charnock parameter. The default value is  $z_{Charnock} = 0.014$ . The wind speed,  $W_2$ , is then calculated from the wind speed,  $W_{10}$ , by first solving Eq. (4.65) and Eq. (4.66) iteratively for  $z_0$  with  $z = 10m$  and  $u(z) = W_{10}$ . Then  $W_2$  is given by

$$W_2 = W_{10} \frac{\log \left( \frac{2}{z_0} \right)}{\log \left( \frac{10}{z_0} \right)} \quad W_{10} > 0.5m/s \quad (4.68)$$

$$W_2 = W_{10} \quad W_{10} \leq 0.5m/s$$

The heat loss due to vaporization occurs both by wind driven forced convection and by free convection. The effect of free convection is taken into account by the parameter  $a_1$  in Eq. (4.60). The free convection is also taken into account by introducing a critical wind speed  $W_{critical}$  so that the wind speed used in Eq. (4.67) is obtained as  $W_{10} = \max(W_{10}, W_{critical})$ . The default value for the critical wind speed is 2 m/s.

#### 4.12.2 Convection

The sensible heat flux,  $q_c$ , measured in  $W/m^2$  (or the heat flux due to convection) depends on the type of boundary layer between the sea surface and the atmosphere. Generally, this boundary layer is turbulent implying the following relationship

$$q_c = \begin{cases} \rho_{air} c_{air} c_{heating} W_{10} (T_{air} - T_{water}) & T_{air} \geq T_{water} \\ \rho_{air} c_{air} c_{cooling} W_{10} (T_{air} - T_{water}) & T_{air} < T_{water} \end{cases} \quad (4.69)$$

where  $\rho_{air}$  is the air density  $1.225 \text{ kg/m}^3$ ;  $c_{air} = 1007 \text{ J/(kg} \cdot \text{°K)}$  is the specific heat of air;  $c_{heating} = 0.0011$  and  $c_{cooling} = 0.0011$ , respectively, is the sensible transfer coefficient (or Stanton number) for heating and cooling (see Kantha and Clayson, 2000);  $W_{10}$  is the wind speed 10 m above the sea surface;  $T_{water}$  is the temperature at the sea surface;  $T_{air}$  is the temperature of the air.

The convective heat flux typically varies between 0 and  $100 \text{ W/m}^2$ .

The heat loss due to convection occurs both by wind driven forced convection and by free convection. The free convection is taken into account by introducing a critical wind speed  $W_{critical}$  so that the wind speed used in Eq. (4.68) is obtained as  $W_{10} = \max(W_{10}, W_{critical})$ . The default value for the critical wind speed is  $2 \text{ m/s}$ .

### 4.12.3 Short wave radiation

Radiation from the sun consists of electromagnetic waves with wave lengths varying from 1,000 to 30,000 Å. Most of this is absorbed in the ozone layer, leaving only a fraction of the energy to reach the surface of the Earth. Furthermore, the spectrum changes when sunrays pass through the atmosphere. Most of the infrared and ultraviolet compound is absorbed such that the solar radiation on the Earth mainly consists of light with wave lengths between 4,000 and 9,000 Å. This radiation is normally termed short wave radiation. The intensity depends on the distance to the sun, declination angle and latitude, extraterrestrial radiation and the cloudiness and amount of water vapour in the atmosphere (see Iqbal, 1983).

The eccentricity in the solar orbit,  $E_0$ , is given by

$$E_0 = \left(\frac{r_0}{r}\right)^2 = 1.000110 + 0.034221 \cos(\Gamma) + 0.001280 \sin(\Gamma) + 0.000719 \cos(2\Gamma) + 0.000077 \sin(2\Gamma) \quad (4.70)$$

where  $r_0$  is the mean distance to the sun,  $r$  is the actual distance and the day angle  $\Gamma$  is defined by

$$\Gamma = \frac{2\pi(d_n - 1)}{356} \quad (4.71)$$

and  $d_n$  is the Julian day of the year.

The daily rotation of the Earth around the polar axes contributes to changes in the solar radiation. The seasonal radiation is governed by the declination angle,  $\delta$ , measured in *rad* which can be expressed by

$$\delta = 0.006918 - 0.399912 \cos(\Gamma) + 0.07257 \sin(\Gamma) - 0.006758 \cos(2\Gamma) + 0.000907 \sin(2\Gamma) - 0.002697 \cos(3\Gamma) + 0.00148 \sin(3\Gamma) \quad (4.72)$$

The day length,  $n_d$ , varies with  $\delta$ . For a given latitude,  $\phi$ , (positive on the northern hemisphere) the day length is given by

$$n_d = \frac{24}{\pi} \arccos(-\tan(\phi)\tan(\delta)) \quad (4.73)$$

and the sunrise angle,  $\omega_{sr}$ , and the sunset angle  $\omega_{ss}$  are

$$\omega_{sr} = \arccos(-\tan(\phi)\tan(\delta)) \quad \text{and} \quad \omega_{ss} = -\omega_{sr} \quad (4.74)$$

The intensity of short wave radiation on the surface parallel to the surface of the Earth changes with the angle of incidence. The highest intensity is in zenith and the lowest during sunrise and sunset. Integrated over one day the extraterrestrial intensity,  $H_0$ , measured in  $MJ/m^2/day$  in short wave radiation on the surface can be derived as

$$H_0 = \frac{24}{\pi} q_{sc} E_0 \cos(\phi) \cos(\delta) (\sin(\omega_{sr}) - \omega_{sr} \cos(\omega_{sr})) \quad (4.75)$$

where  $q_{sc} = 4.9212 MJ/m^2/h$  is the solar constant.

For determination of daily radiation under cloudy skies,  $H$ , measured in  $MJ/m^2/day$ , the following relation is used

$$\frac{H}{H_0} = a_2 + b_2 \frac{n}{n_d} \quad (4.76)$$

in which  $n$  is the number of sunshine hours and  $n_d$  is the maximum number of sunshine hours.  $a_2$  and  $b_2$  are user specified constants. The default values are  $a_2 = 0.295$  and  $b_2 = 0.371$ . The user-specified clearness coefficient corresponds to  $n/n_d$ . Thus the solar radiation,  $q_s$ , measured in  $W/m^2$  can be expressed as

$$q_s = \left(\frac{H}{H_0}\right) q_0 (a_3 + b_3 \cos(\omega_i)) \frac{10^6}{3600} \quad (4.77)$$

where

$$a_3 = 0.4090 + 0.5016 \sin\left(\omega_{sr} - \frac{\pi}{3}\right) \quad (4.78)$$

$$b_3 = 0.6609 + 0.4767 \sin\left(\omega_{sr} - \frac{\pi}{3}\right) \quad (4.79)$$

The extraterrestrial intensity,  $q_0$  ( $MJ/m^2/h$ ) and the hour angle  $\omega_i$  is given by

$$q_0 = q_{sc} E_0 \left( \sin(\phi) \sin(\delta) + \frac{24}{\pi} \cos(\phi) \cos(\delta) \cos(\omega_i) \right) \quad (4.80)$$

$$\omega_i = \frac{\pi}{12} \left( 12 + \Delta t_{displacement} + \frac{4}{60} (L_S - L_E) - \frac{E_t}{60} - t_{local} \right) \quad (4.81)$$

$\Delta t_{displacement}$  is the displacement hours due to summer time and the time meridian  $L_S$  is the standard longitude for the time zone.  $\Delta t_{displacement}$  and  $L_S$  are user specified constants. The default values are  $\Delta t_{displacement} = 0$  h and  $L_S = 0$  deg.  $L_E$  is the local longitude in degrees.  $E_t$  (s) is the discrepancy in time due to solar orbit and is varying during the year. It is given by

$$E_t = (0.000075 + 0.001868 \cos(\Gamma) - 0.032077 \sin(\Gamma) - 0.014615 \cos(2\Gamma) - 0.04089 \sin(2\Gamma)) \cdot 229.18 \quad (4.82)$$

Finally,  $t_{local}$  is the local time in hours.

Solar radiation that impinges on the sea surface does not all penetrate the water surface. Parts are reflected back and are lost unless they are backscattered from the surrounding atmosphere. This reflection of solar energy is termed the albedo. The amount of energy, which is lost due to albedo, depends on the angle of incidence and angle of refraction. For a smooth sea the reflection can be expressed as

$$\alpha = \frac{1}{2} \left( \frac{\sin^2(i - r)}{\sin^2(i + r)} + \frac{\tan^2(i - r)}{\tan^2(i + r)} \right) \quad (4.83)$$

Where  $i$  is the angle of incidence,  $r$  the refraction angle and  $\alpha$  the reflection coefficient, which typically varies from 5 to 40 %.  $\alpha$  can be approximated using

$$\alpha = \begin{cases} \frac{altitude}{5} \cdot 0.48 & altitude < 5 \\ \frac{30 - altitude}{25} (0.48 - 0.05) & 5 \leq altitude \leq 30 \\ 0.05 & altitude > 30 \end{cases} \quad (4.84)$$

where the altitude in degrees is given by

$$altitude = 90 - \left( \frac{180}{\pi} \arccos(\sin(\delta)\sin(\phi) + \cos(\delta)\cos(\phi)\cos(\omega_i)) \right) \quad (4.85)$$

Thus the net short wave radiation,  $q_{st,net}$  ( $W/m^2$ ), can possibly be expressed as

$$q_{sr,net} = (1 - \alpha)q_s \quad (4.86)$$

The net short wave radiation,  $q_{sr,net}$ , can be calculated using empirical formulae as described above. Alternatively, the net short wave radiation can be calculated using Eq. (4.86), where the solar radiation,  $q_s$ , is specified by the user or the net short wave radiation,  $q_{sr,net}$ , can be given by the user.

#### 4.12.4 Long wave radiation

A body or a surface emits electromagnetic energy at all wavelengths of the spectrum. The long wave radiation consists of waves with wavelengths between 9,000 and 25,000 Å. The radiation in this interval is termed infrared radiation and is emitted from the atmosphere and the sea surface. The long wave emittance from the surface to the atmosphere minus the long wave radiation from the atmosphere to the sea surface is called the net long wave radiation and is dependent on the cloudiness, the air temperature, the vapour pressure in the air and the relative humidity. The net outgoing long wave radiation,  $q_{lr,net}$ , measured in  $W/m^2$  is given by Brunt's equation (See Lind and Falkenmark, 1972)

$$q_{lr,net} = -\sigma_{sb}(T_{air} + T_k)^4(a - b\sqrt{e_d}) \left( c + d \frac{n}{n_d} \right) \quad (4.87)$$

where  $e_d$  is the vapour pressure at dew point temperature measured in  $mb$ ;  $n$  is the number of sunshine hours,  $n_d$  is the maximum number of sunshine hours;  $\sigma_{sb} = 5.6697 \cdot 10^{-8} W/(m^2 \cdot ^\circ K^4)$  is Stefan Boltzman's constant;  $T_{air}$  ( $^\circ C$ ) is the air temperature. The coefficients  $a$ ,  $b$ ,  $c$  and  $d$  are given as

$$a = 0.56 \quad b = 0.077 mb^{-\frac{1}{2}} \quad c = 0.1 \quad d = 0.9 \quad (4.88)$$

The vapour pressure is determined as

$$e_d = 10 \cdot R \cdot e_{saturated} \quad (4.89)$$

where  $R$  is the relative humidity and the saturated vapour pressure,  $e_{saturated}$ , measured in  $kPa$  with 100 % relative humidity in the interval from  $-51$  to  $52$  °C can be estimated by

$$e_{saturated} = 3.38639 \cdot ((7.38 \cdot 10^{-3} \cdot T_{air} + 0.8072)^8 - 1.9 \cdot 10^{-5} |1.8 \cdot T_{air} + 48| + 1.316 \cdot 10^{-3}) \quad (4.90)$$

The net long wave radiation,  $q_{lr,net}$ , can be calculated using empirical formulae as described above. Alternatively, the net long wave radiation can be calculated as

$$q_{lr,net} = q_{ar,net} - q_{br} \quad (4.91)$$

where the net incident atmospheric radiation,  $q_{ar,net}$ , is specified by the user and the back radiation,  $q_{br}$ , is given by

$$q_{br} = (1 - r) \varepsilon \sigma_{sb} T_k^4 \quad (4.92)$$

where  $r = 0.03$  is the reflection coefficient and  $\varepsilon = 0.985$  is the emissivity factor of the atmosphere. The net long wave radiation can also be specified by the user.

#### 4.12.5 Ground heat

The heat conduction at the bed is a function of the difference between the temperature at the bed and at an equilibrium ground temperature which will be some distance below the bed. The heat flux,  $q_g$ , through the bed is given by

$$q_d = K_g \frac{(T_g - T_w)}{\Delta z_g} \Delta z \quad (4.93)$$

where  $K_g$  (Watt/m/°C) is the thermal conductivity of the bed material (etc. soil, sand or rock),  $T_g$  is the ground equilibrium temperature,  $T_w$  is the water temperature at the bed/water interface and  $\Delta z_g$  is distance from the bed/ground level to the level where the equilibrium ground temperature is specified.





## 5 Structures

The horizontal dimension of structures is usually much smaller than the element (cell) sizes used in the computational grid. Therefore, the effect of structures is modeled by a subgrid technique. Six types of structures are included in the model

- Weirs
- Culverts
- Dikes
- Gates
- Piers
- Turbines

In addition, a composite structure can be used. A composite structure is a combination of a number of weirs and culverts.

Weirs, culverts, dikes and gates are defined as line sections. The location in the domain of a line section is given by a number of geo-referenced points which together make up a polyline. This is illustrated in Figure 5.1. The polyline defines the width of the cross section perpendicular to the flow direction. A minimum of two points is required. The polyline is composed of a sequence of line segments. The line segments are straight lines between two successive points. The polyline (line section) in the numerical calculations is defined as a section of element faces. The face is included in the section when the line between the two element centers of the faces crosses one of the line segments. If two faces in a triangular element are part of the same face section, the face section is corrected so that these two faces are excluded from the face section and instead the third face in the triangle is applied. The left and right side of the of the line section is defined by positioning at the start point and looking forward along the line section.

Piers and turbines are defined as points in the domain

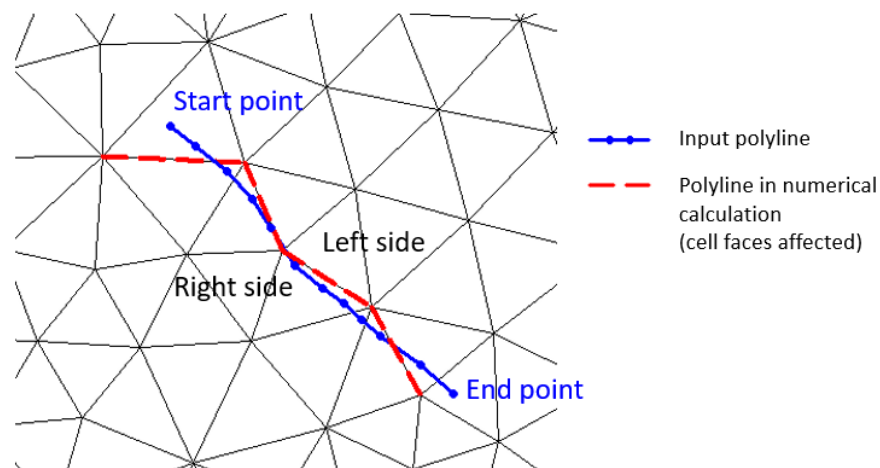


Figure 5.1 The location of a line section.

### 5.1 Weirs

A weir is defined as a cross (line) section where the total discharge across the cross section is calculated using empirical formulas and distributed along the cross section. In the numerical calculations the cross section is defined as a section of element faces

which is treated as an internal discharge boundary (weak formulation). However, the flux contribution to the continuity equation is corrected to secure mass conservation.

The total discharge is calculated based on the mean water level in the real wet elements to the left and right of the section of faces. The mean level is calculated using the length of the element faces as the weighting factor. Real wet elements are elements where the water depth is larger than the wetting depth. The upstream water level is then the highest of the two water levels and the downstream water level the smallest. The distribution of the calculated total discharge along the section faces can be specified in two ways

- Uniform
- Non-uniform

The discharge is in both cases distributed to the faces for which the element to the left and right of the face are both a wet element and else the discharge is distributed to the faces for which the upstream elements are wet elements. When non-uniform distribution is applied the discharge will be distributed as it would have been in a uniform flow field with the Manning resistance law applied, i.e. relative to  $h^{5/3}$ , where  $h$  is the total water depth. This distribution is, in most cases, a good approximation. This does not apply if there are very large variations over the bathymetry or the geometry. A uniform distribution is applied for the vertical distribution.

When the difference between the upstream and downstream water level for a weir is small the corresponding gradient of the discharge with respect to the water levels is large. This in turn may result in a very rapid flow response to minor changes in the water level upstream and downstream. As a way of controlling this effect an Alpha zero value has been introduced. The Alpha zero value defines the water level difference below which the discharge gradients are suppressed. The default setting is 0.01 meter.

For weirs a valve regulation is applied. Four different valve regulation types are available

- None. No valve regulation applies (flow is not regulated).
- Only Negative Flow. Only flow in negative flow direction is allowed. Valve regulation does not allow flow in positive flow direction and the flow through the structure will be zero in this case.
- Only Positive Flow. Only flow in positive flow direction is allowed. Valve regulation does not allow flow in negative flow direction and the flow through the structure will be zero in this case.
- No Flow. No flow is allowed in the structure. Valve regulation closes completely the structure.

The flow direction is positive when the flow occurs from the right of the line structure to the left (see Figure 5.1)

Three formulas are available for calculation of the discharge through a weir

- Broad Crested Weir formula
- Weir formula 1
- Weir formula 2 (Honma formula)

#### Broad Crested Weir

For a broad crested weir the shape of the "hole" is described through a level/width table (see Figure 5.2 and Figure 5.3). Levels are defined relative to the datum (starting from the crest or sill level and up). A datum value for the weir may be used to shift the levels by a

constant amount. This is typically used if the weir geometry has been surveyed with respect to a local benchmark.

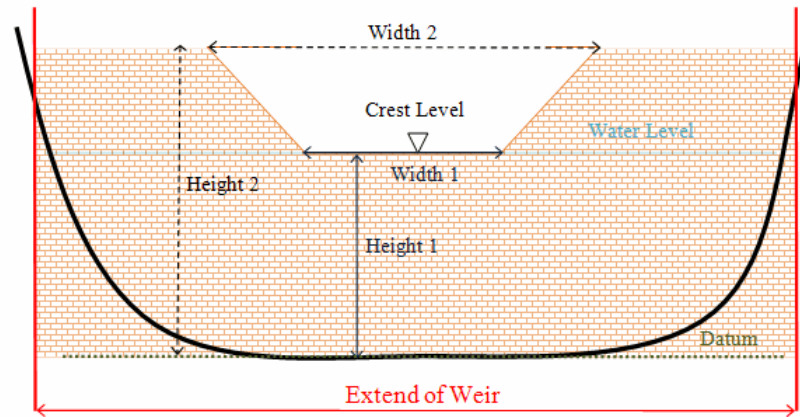


Figure 5.2 Setup definitions of contracted weir.

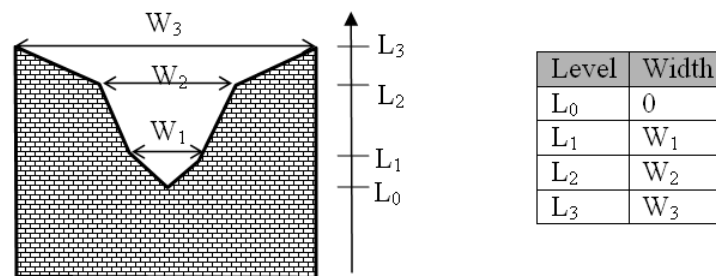


Figure 5.3 Definition sketch for broad crested weir geometry.

The standard formulations for flow over a broad crested weir are established on the basis of the weir geometry and the specified head loss and calibration coefficients. These formulations assume a hydrostatic pressure distribution on the weir crests. Different algorithms are used for drowned flow and free overflow, with an automatic switching between the two.

The energy loss over a weir is given by

$$q = \zeta_t \frac{V_s}{2g} \quad (5.1)$$

where  $\zeta_t$  is the total head loss coefficient and  $V_s$  is the mean cross sectional velocity at the structure. The total head loss coefficient,  $\zeta_t$ , is composed of entrance,  $\zeta_1$ , and exit,  $\zeta_2$ , loss coefficients. The coefficients are generally related to the input parameters for inflow,  $\zeta_{in}$ , and outflow,  $\zeta_{out}$ , and the changes in velocity,  $V$ , and area,  $A$

$$\zeta_t = \zeta_1 + \zeta_2 = \zeta_{in} \left( \frac{V_1}{V_s} \right) + \zeta_{out} \left( \frac{A_s}{A_2} \right)^2 \quad (5.2)$$

where suffix '1' and '2' represents velocity and area on inflow and outflow side of the structure respectively, and 's' represents the velocity and area in the structure itself. However, in the present implementation, upstream and downstream cross sections are not extracted and accordingly, tabulated relations on cross section areas as function of

water levels are not known. Instead, upstream and downstream areas are set to a large number resulting in a full loss contribution from the head loss factors defined

$$\zeta_t = \zeta_1 + \zeta_2 = \zeta_{in} + \zeta_{out} \quad (5.3)$$

Care must be taken when selecting loss coefficients, particularly in situations where both subcritical and supercritical flow conditions occur. When flow conditions change from subcritical to supercritical (or the Froude number, FR, becomes greater than 1), the loss coefficients  $\zeta_{in}$  and  $\zeta_{out}$  are modified:

- If  $FR > 1$  for upstream conditions, then  $\zeta_{in} = \zeta_{in}/2$
- If  $FR > 1$  for downstream conditions, then  $\zeta_{out} = \zeta_{out}/2$

The critical flows are multiplied by the critical flow correction factor,  $\alpha_c$ , specified as the free overflow head loss factor. Typically, a value of 1.0 is used.

#### Weir formula 1

For the Weir formula 1 description the parameters are given by Figure 5.4. The width is perpendicular to the flow direction. Typically, the invert level coincides with the overall datum. Weir formula 1 is based on a standard weir expression, reduced according to the Villemonte formula

$$q = C(\eta_{US} - z_W)^k \left(1 - \frac{\eta_{DS} - z_W}{\eta_{US} - z_W}\right)^{-0.385} W \quad (5.4)$$

where  $q$  is the discharge through the structure,  $W$  is the width,  $C$  is the weir coefficient,  $k$  is the weir exponential coefficient,  $\eta_{US}$  is the upstream water level,  $\eta_{DS}$  is the downstream water level and  $z_W$  is the weir level (see Figure 5.4). The invert level is the lowest point in the inlet or outlet section respectively.

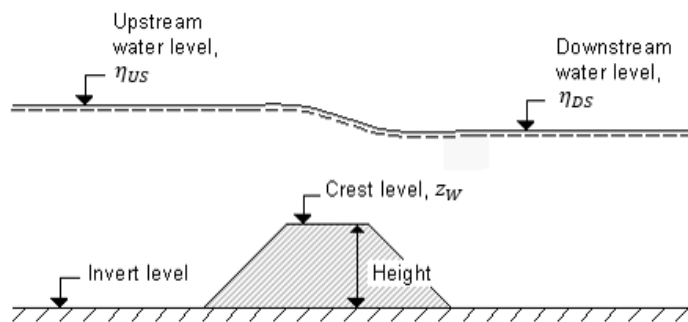


Figure 5.4 Definition sketch for weir flow.

#### Weir formula 2

For the Weir formula 2 the geometry is given by a crest level and a width. The crest level is taken with respect to the global datum. The width is perpendicular to the flow direction. Weir formula 2 is the Honma formula

$$q = \begin{cases} C_1(\eta_{US} - z_W)\sqrt{\eta_{US} - z_W} W & \frac{(\eta_{DS} - z_W)}{\eta_{US}} < \frac{2}{3} \\ C_2(\eta_{DS} - z_W)\sqrt{\eta_{US} - \eta_{DS}} W & \frac{(\eta_{DS} - z_W)}{\eta_{US}} \geq \frac{2}{3} \end{cases} \quad (5.5)$$

where  $q$  is the discharge through the structure,  $W$  is the width,  $C_1$  and  $C_2 = 1.5\sqrt{3}C_1$  are the two weir coefficients,  $\eta_{US}$  is the upstream water level,  $\eta_{DS}$  is the downstream water level and  $z_W$  is the weir level (see Figure 5.4).

## 5.2 Culverts

A culvert can be modelled either as a short or a long culvert.

A short culvert is defined as a cross (line) section where the total discharge across the cross section is calculated using empirical formulas and distributed along the cross section. In the numerical calculations the cross section is defined as a section of element faces which is treated as an internal discharge boundary (weak formulation). However, the flux contribution to the continuity equation is corrected to secure mass conservation.

A long culvert is defined by a longitudinal line as shown in Figure 5.5 where the inlet and outlet location are defined as two extent lines at the ends of the transversal line. The polyline (line section) in the numerical calculations for each of the two extent lines is defined as a section of element faces. A long culvert is treated as two connected area sources where the total discharge is calculated using empirical formulas. For each of the two extent lines, the area is determined at the area of the elements to the right of the section of element faces. At the outlet location it is possible to take into account the contribution to the momentum equation. This contribution is estimated as the discharge multiplied by a velocity. Here the magnitude of the velocity is calculated as the discharge divided by the local total water depth. The direction used for the two extent lines is the direction of the first and last segment of the longitudinal polyline. If the longitudinal polyline only contains one segment (two points), the direction is determined as the direction perpendicular to the line given by the first and last point of the extent line.

For a short culvert the total discharge is calculated based on the mean water level in the real wet elements to the left and right of the section of faces. For a long culvert the total discharge is calculated based on the mean water level in the real wet elements to the right of the section of faces for the two extent lines. The mean level is calculated using the length of the element faces as the weighting factor. Real wet elements are elements where the water depth is larger than the wetting depth. The upstream water level is then the highest of the two water levels and the downstream water level the smallest.

The distribution of the calculated total discharge along the section faces can be specified in two ways

- Uniform
- Non-uniform

For a short culvert the discharge is in both cases distributed to the faces for which the element to the left and right of the face are both a wet element and else the discharge is distributed to the faces for which the upstream elements are wet elements. When non-uniform distribution is applied the discharge will be distributed as it would have been in a uniform flow field with the Manning resistance law applied, i.e. relative to  $h^{5/3}$ , where  $h$  is the total water depth. For a long culvert the discharge is in both cases distributed to the faces for which the element to the right of the extent line is a wet element. If no elements

are wet the discharge is distributed uniformly to all faces in the section. When non-uniform distribution is applied the same approach as for short culverts is used. The non-uniform distribution is, in most cases, a good approximation. This does not apply if there are very large variations over the bathymetry or the geometry. A uniform distribution is applied for the vertical distribution.

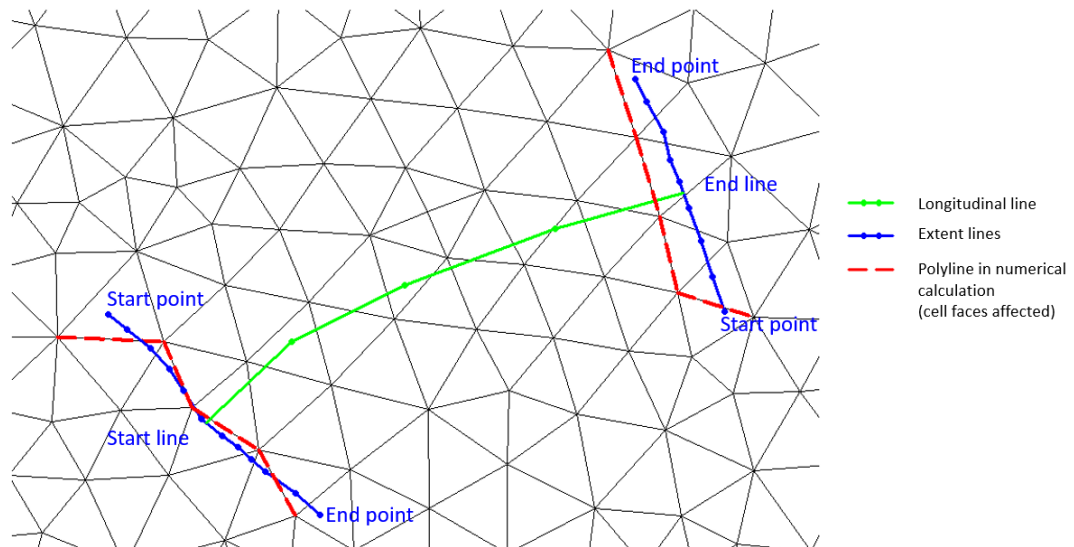


Figure 5.5 Setup definitions for a long culvert.

When the difference between the upstream and downstream water level for both a short and long culvert is small the corresponding gradient of the discharge with respect to the water levels is large. This in turn may result in a very rapid flow response to minor changes in the water level upstream and downstream. As a way of controlling this effect an Alpha zero value has been introduced. The Alpha zero value defines the water level difference below which the discharge gradients are suppressed. The default setting is 0.01 meter.

For both short and long culverts a valve regulation is applied. Four different valve regulation types are available

- None. No valve regulation applies (flow is not regulated).
- Only Negative Flow. Only flow in negative flow direction is allowed. Valve regulation does not allow flow in positive flow direction and the flow through the structure will be zero in this case.
- Only Positive Flow. Only flow in positive flow direction is allowed. Valve regulation does not allow flow in negative flow direction and the flow through the structure will be zero in this case.
- No Flow. No flow is allowed in the structure. Valve regulation closes completely the structure.

For a short culvert the flow direction is positive when the flow occurs from the right of the line structure to the left (see Figure 5.1). For a long culvert the flow direction is positive when flow is from the start line to the end line (Figure 5.5).

The culvert geometry defines the geometrical shape of the active flow area of the culvert, see Figure 5.6. The cross sectional geometry of a culvert can be specified as

- Rectangular. The width and height specify the geometry.
- Circular. The geometry is specified by the diameter.
- Irregular Level-Width Table. The geometry is specified using a level/width table. The Level/Width table defines the culvert shape as a set of corresponding levels and flow widths (see Figure 5.7).

A culvert structure can be modelled as either an open section or a closed section. If set to open the culvert will never run full or partially full, therefore only those flow conditions which represent a free water surface are modelled. When the water level is higher than the soffit the hydraulic parameters are calculated based on a section extended vertically upwards with a width equal to that at the soffit. For example, in the case of a rectangular section the height value is essentially redundant as the cross-section will be modeled as an open section of constant width. A circular culvert is always a treated as a closed section.

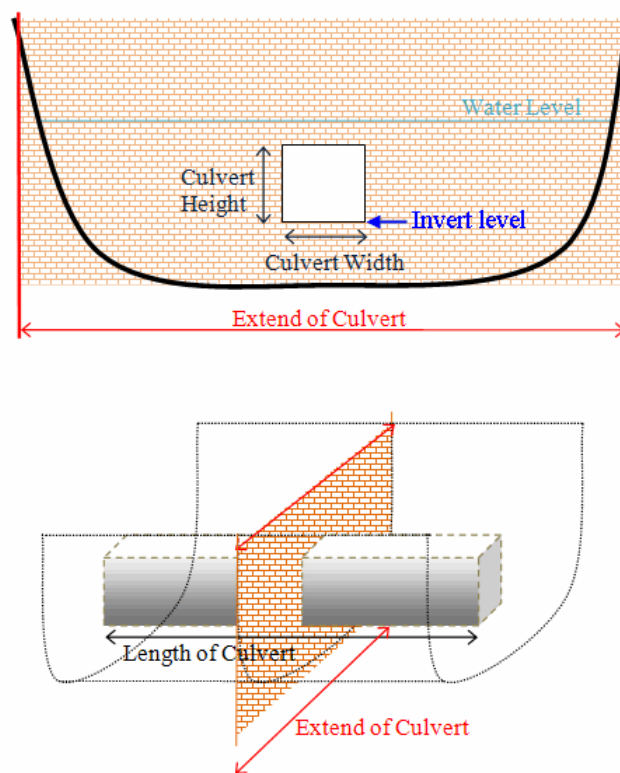


Figure 5.6 Setup definitions of culverts.

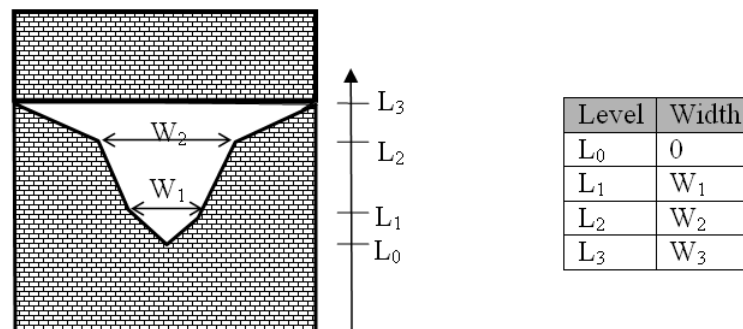


Figure 5.7 Definition sketch for irregular culvert geometry.



The total head loss,  $\Delta H_{loss}$  through a culvert is given by

$$\Delta H_{loss} = \frac{q^2}{2g} \left( \frac{\zeta_1}{A_{s_1}^2} + \frac{\zeta_f + \zeta_b}{A_{s_A}^2} + \frac{\zeta_2}{A_{s_2}^2} \right) \quad (5.6)$$

where  $A_{s_1}$ ,  $A_{s_A}$  and  $A_{s_2}$  are the mean cross section areas along the length of the culvert and  $q$  is the discharge,  $\zeta_1$  is the entrance or contraction loss coefficient,  $\zeta_2$  is the outlet or expansion loss coefficient,  $\zeta_f$  is the friction loss and  $\zeta_b$  is the bend loss coefficient.  $\zeta_1$  and  $\zeta_2$  are calculated by

$$\zeta_1 = \zeta_{in} \left( 1 - \frac{A_s}{A_1} \right) \quad (5.7)$$

$$\zeta_2 = \zeta_{out} \left( 1 - \frac{A_s}{A_2} \right)^2 \quad (5.8)$$

The upstream and downstream cross section areas,  $A_1$  and  $A_2$  are not processed and extracted in the present implementation and hence, defined as an infinite value. Contraction and expansion losses are therefore assumed to be applied in full using the defined inflow and outflow loss coefficients,  $\zeta_{in}$  and  $\zeta_{out}$ . The friction loss coefficient is calculated using the Manning formula

$$\zeta_f = \frac{2gLn^2}{R^{4/3}} \quad (5.9)$$

where  $L$  is the culvert length,  $n$  is Manning's coefficient and  $R$  is the mean hydraulic radius along the culvert. The Manning's  $n$ -value depends on the interior surface of the culvert. Table values can be found in literature. For example, a concrete culvert  $n$  would typically range from 0.011 to 0.017.

The bend loss coefficient,  $\zeta_b$ , is provided for situations where head losses other than from the above occur, for example bends, damaged culverts, trapped debris. For straight culverts in good condition a value of zero would apply. The critical flows (and orifice flows for culverts as well) are multiplied by the critical flow correction factor,  $\alpha_c$ , specified as the free overflow head loss factor. Typically, a value of 1.0 is used.

### 5.3 Composite structures

A composite structure is a combination of a number of weirs and short culverts (see Figure 5.8). A composite structure is defined as a cross section where total discharge across the cross section is calculated using empirical formulas for weirs and culverts and distributed along the cross section. In the numerical calculations the cross section is defined as a section of element faces which is treated as an internal discharge boundary (weak formulation). However, the flux contribution to the continuity equation is corrected to secure mass conservation. The approach for calculating the mean water level and for distribution of the total discharge are the same as the approach used for weirs and culverts.

The total discharge across the combined structures is calculated by iteration until a stable flow is achieved. During the iteration, the energy headloss of the structures is modified; thus, only structures that apply an energy description are modified in the iteration



process. These include culverts and broad Crested Weirs. If none of these structures are present in a composite structure, then no iterations are performed.

A set of structures forming a composite structure are recognized from the location definitions. Locations must be completely identical for all the structures forming the composite structure. That is, the table of coordinates defining the structure locations must be exactly identical (number of coordinates and coordinate values) for all structures defined.

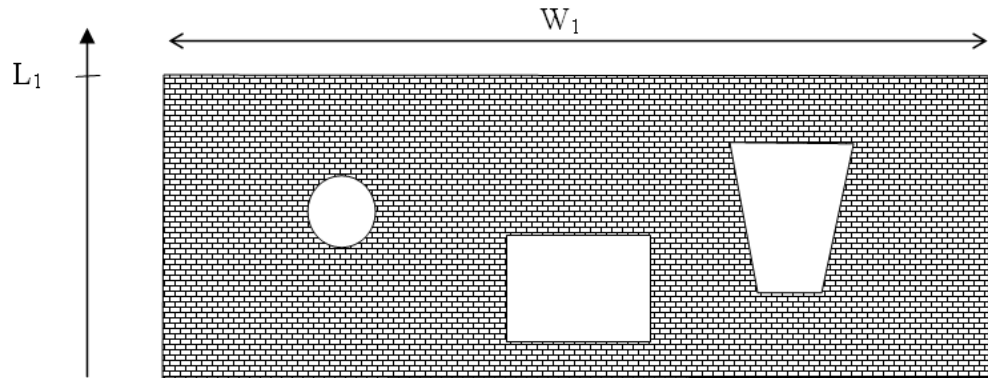


Figure 5.8 Setup definitions of a composite structure. Here the structure consists of one weir with a constant crest level  $L_1$  and three short culverts (a circular, a rectangular and a irregular).

## 5.4 Dikes

A dike is defined as a cross section and in the numerical calculations the cross section is defined as a section of element faces which is treated as an internal discharge boundary (weak formulation). However, the flux contribution to the continuity equation is corrected to secure mass conservation. The discharge across each face in the section is calculated using an empirical formula or specified as input. A uniform distribution is applied for the vertical distribution.

When the empirical formulation is used the discharge,  $q$ , over an element face with the length (width),  $\Delta l$ , is calculated based on the water level in the elements to the left and right of the face. The upstream water level is then the highest of the two water levels and the downstream water level the smallest. A standard weir expression, reduced according to the Villemonte formula, is applied

$$q = C(\eta_{US} - z_W)^k \left(1 - \frac{\eta_{DS} - z_W}{\eta_{US} - z_W}\right)^{-0.385} \Delta l \quad (5.10)$$

where  $C$  is the weir coefficient,  $k$  is the weir exponential coefficient,  $\eta_{US}$  is the upstream water level,  $\eta_{DS}$  is the downstream water level and  $z_W$  is the weir level taken with respect to the global datum (see Figure 5.9). The value of the weir exponent is 1.5 and the default value of the weir coefficient is 1.838.

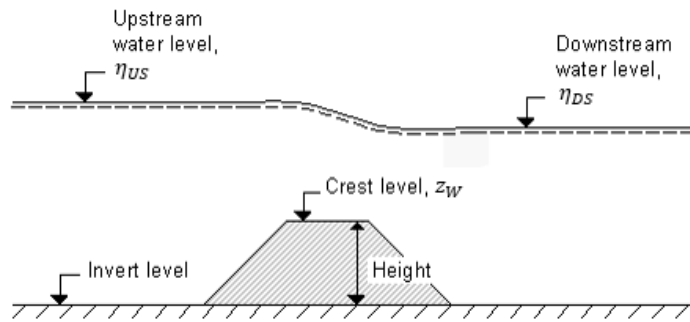


Figure 5.9 Definition sketch for dike flow.

## 5.5 Gates

A gate is defined as a cross section and in the numerical calculations the cross section is defined as a section of element faces. At an element face with the length,  $\Delta l$ , the normal flux is calculated as the sum of the normal flux for a solid wall, where the length is determined as  $(1 - c)\Delta l$ , and the normal flux for a standard wet face, where the length is  $c\Delta l$ . Here,  $c$  is a weighting factor with a value between 0 and 1, where 0 corresponds to a closed gate and 1 corresponds to an open gate.

If the gate is defined as the full water column,  $c$  is equal to the user-defined gate control factor,  $c_{input}$ . If the gate geometry is defined as a subset of the water column the vertical location of the gate is defined by the top level,  $z_{top}$ , and bottom level of the gate,  $z_{bottom}$ , (see Figure 5.7). In this case  $c$  is calculated as

$$c = f c_{input} + (1 - f) \quad (5.11)$$

where  $f$  is the fraction of the element face, which is blocked by the gate.

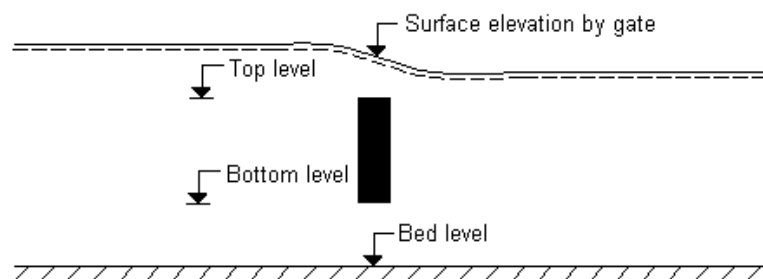


Figure 5.10 Definition sketch for gate flow.

## 5.6 Piers

The effect of piers is modelled as sub-grid structures by an additional volume force to the momentum equation in the column of cells where the pier is located. A simple drag-law is used to capture the increasing resistance imposed by the piers as the flow speed increases.

The effective current induced drag force,  $F_D$ , is determined from

$$F_D = \frac{1}{2} \rho_0 \gamma C_D A_e V^2 \quad (5.12)$$

where  $\gamma$  is the streamline factor,  $C_D$  is the drag coefficient,  $A_e$  is the effective area of the pier exposed to current and  $V$  is the current speed. The sign of  $F_D$  is such that a positive force acts against the current direction. The streamline factor is a factor that is multiplied on the total drag force to take into account the increased flow velocity due to the blocking of piers. The velocity is the velocity in the cell, where the pier is located.

A pier is defined as a number of pier segments, which are vertical sections with different geometrical layout (see Figure 5.11 and Figure 5.12). The geometrical layout can be

- Circular
- Rectangular
- Elliptical

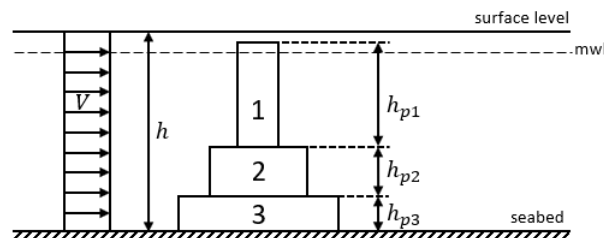


Figure 5.11 Pier with 3 sections with heights  $h_{p1}$ ,  $h_{p2}$  and  $h_{p3}$ .

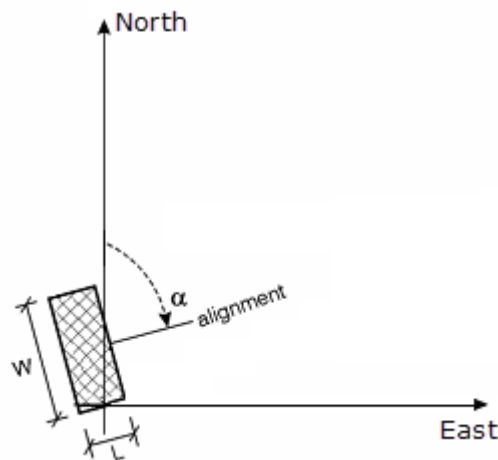


Figure 5.12 Definition of pier angles.  $w$  is the width of the pier section,  $L$  is the length of the pier section,  $\alpha$  is the angle between projection north and the alignment.

## 5.7 Turbines

The effect of tidal turbines is modelled as sub-grid structures by an additional volume force to the momentum equation in the column of cells where the turbine is located. A simple drag-law is used to capture the increasing resistance imposed by the turbine blades as the flow speed increases. Turbines are assumed always to have their axis aligned with the flow direction.

The effect to the flow due to the turbines is modeled by calculating the current induced drag and lift force on each individual layer (see Figure 5.13). The effective drag force,  $F_D$ , and lift force,  $F_L$ , are determined from

$$F_D = \frac{1}{2} \rho_0 \alpha C_D A_e V^2 \quad (5.13)$$

$$F_L = \frac{1}{2} \rho_0 \alpha C_L A_e V^2 \quad (5.14)$$

where  $\alpha$  is a correction factor,  $C_D$  is the drag coefficient,  $C_L$  is the lift coefficient,  $A_e$  is the effective area of the turbine exposed to current and  $V$  is the upstream current speed. For three-dimensional calculations the current speed used to determine the force is the average current speed over the water column covered by the turbine and the shear stress is equally distributed over water column covered by the turbine.

When no current correction is applied the upstream current velocity is approximated by the local velocity,  $V_{local}$ . The local velocity is the velocity in the cell, where the turbine is located. When current correction is included the upstream current speed is approximated by

$$V_0 = \frac{2}{1 + \sqrt{1 - \gamma}} V_{local} \quad (5.15)$$

where  $\gamma = \alpha C_D A_e / (h \Delta s)$ . Here  $h$  is the water depth and  $\Delta s$  is grid distance. When the drag coefficient is specified as a function of the upstream current speed the corrected current speed is determined by iteration. The grid distance is determined as the width perpendicular to the flow direction of the element, where the turbine is located. For more detail see (Kramer et al. (2014)).

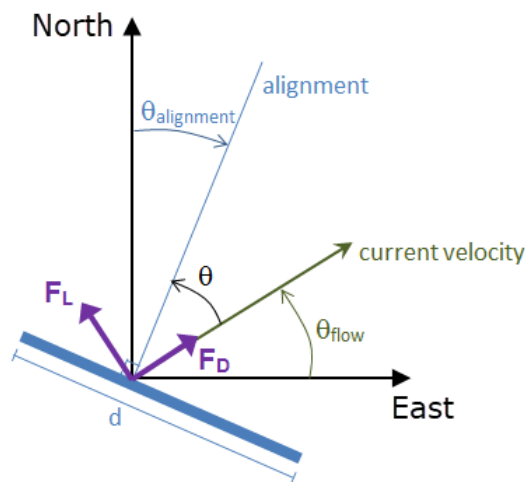


Figure 5.13 Definition of turbine angles.  $d$  is the diameter of the turbine,  $\theta_{flow}$  is the current direction,  $\theta_{alignment}$  is the angle between projection north and the alignment and  $\theta$  is the angle between alignment and flow.

## 6 Parallelization

The MIKE 3 Flow Model FM utilizes the following parallelization techniques in a hybrid manner

- OpenMP computing approach
- MPI computing approach
- GPU computing approach

The MIKE 3 Flow Model FM is parallelized for shared-memory multiprocessor/multicore computers using OpenMP. This parallelization is performed by adding compiler directives to the code.

To improve performance and to be able to perform simulations on large massively parallel distributed-memory computers and clusters, MIKE 3 Flow Model FM has also been parallelized using the domain decomposition concept and Message Passing Interface (MPI). Given the number of processor cores allocated to a simulation, the computational mesh is partitioned into subdomains, and the workload associated with each domain is distributed between the allocated cores. The data exchange between domains is performed by message passing using the Intel MPI Library, which has multi fabric message passing capabilities. It allows the use of mixed communication between the domains. Thus, domains will exchange data via the fastest communication interface – in ranked order: shared memory, InfiniBand, Ethernet, etc..

The GPU computing approach uses the computers graphics card to perform the computational intensive calculations. This approach is based on CUDA™ by NVIDIA and can be executed on NVIDIA graphic cards with Compute Capability 3.0 or higher. Only the computational intensive part of the calculations solving the flow equations and transport equations (temperature and salinity, turbulence and transport of a scalar quantity) are performed on the GPU. The additional calculations (e.g. input and output handling) are for each sub-domain performed on the CPU and these calculations are parallelized based on the OpenMP computing approach. The GPU acceleration is only possible when the shallow water equations are used.

### 6.1 The domain decomposition

The domain partitioning is performed using the METIS graph partitioning library (Karypis and Kumar, (1998, 1999)). The computational mesh is converted into a graph, and then METIS uses a multi-level graph partitioning scheme to split the graph into subgraphs, representing the partitioned subdomains, which are distributed among the allocated cores. METIS computes a balanced partitioning that minimizes the connectivity of the subdomains. This partitioning is performed based on the 2D (horizontal) mesh. Using a 2D mesh to partition a 3D domain can cause unbalanced partitioning. When combined sigma/z-level discretization is used in 3D flow calculations, the number of vertical elements can vary significantly across the domain. This difference in the number of vertical elements can lead to an unbalanced partitioning. To get a balanced partitioning for a 3D mesh, weights corresponding to the actual number of vertical elements associated to each vertex of the graph are used. The partitioning is then made so that the sum of vertex-weights is the same for all subdomains. Hence, with both 2D and 3D meshes, the partitioning strategy ensures that the difference in the number of elements in all subdomains is minimized.

The chosen numerical scheme for the discretization in the spatial domain requires an overlapping domain decomposition. It is based on the halo-layer ("ghost"-cells) approach,

where each subdomain contains elements from connected subdomains. This overlap is needed, because calculations require values from the connecting elements. Thus, calculations of some elements at the border between subdomains require values from the connected subdomains.

## 6.2 Data exchange

The data exchange between processes is based on the aforementioned halo-layer ("ghost"-cells) approach with overlapping elements. The extension of the halo-layer area depends on the numerical scheme used for the discretization in the spatial domain and which variables are chosen to be exchanged between subdomains. Here a two-element wide halo-layer is applied. The data exchanges are performed via asynchronous communication when possible, and synchronous communications are used in different parts of the system to ensure correct execution. The MIKE 3 Flow Model FM uses a dynamic time step in the time integration scheme. To ensure that the calculations are performed with the same time step in all subdomains, time step information is exchanged between processes and thereby synchronizing the processes of each time step. Several special features require additional data exchange. These special interest points cause synchronization of two or more subdomains during the data exchange. The case of input and output data exchange is mentioned in the next subsection. Finally, information is exchanged between subdomains in connection with error handling. When the system encounters an error in the model, the error is distributed to the other processes when the time step is finished and the simulation is stopped.

## 6.3 Input and output

The input and output (I/O) is handled using a parallel I/O approach. The master process reads the global mesh information, performs the partitioning of the mesh and distributes the information about the individual subdomains to the slave processes. Each process then reads the additional input specifications using the generic specification file. The input data (wind maps, initial condition maps, etc.) are read by each process using the global data files. Since the individual processes perform I/O locally, the simulation data files must be accessible by each process. This access could be through a network-attached storage system or locally on each computer. The output data files from the simulations are written to private files for each subdomain. At the end of the simulation, the data files are merged to obtain data files containing global information.

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## APPENDICES



## APPENDIX A – Governing equations in spherical coordinates



## A Governing equations in spherical coordinates

In spherical coordinates the independent variables in the horizontal domain are the longitude,  $\lambda$ , and the latitude,  $\phi$ . The horizontal velocity field  $(u, v)$  is defined by

$$u = R \cos \phi \frac{d\lambda}{dt} \quad v = R \frac{d\phi}{dt} \quad (\text{A1.1})$$

where  $R$  is the radius of the earth.

### A.1 Governing equations in spherical coordinate system and z-coordinates

#### A.1.1 Flow equations

The Navier-Stokes equations are given as

$$\frac{1}{R \cos \phi} \left( \frac{\partial u}{\partial \lambda} + \frac{\partial v \cos \phi}{\partial \phi} \right) + \frac{\partial w}{\partial z} = 0 \quad (\text{A1.2})$$

$$\begin{aligned} \frac{\partial u}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u^2}{\partial \lambda} + \frac{\partial v u \cos \phi}{\partial \phi} \right) + \frac{\partial w u}{\partial z} = \\ \left( f + \frac{u}{R} \tan \phi \right) v - \frac{1}{R \cos \phi} \left( \frac{1}{\rho_0} \frac{\partial q}{\partial \lambda} + g \frac{\partial \eta}{\partial \lambda} + \frac{1}{\rho_0} \frac{\partial p_A}{\partial \lambda} + \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \lambda} \right) + F_u \\ + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial u}{\partial z} \right) \end{aligned} \quad (\text{A1.3})$$

$$\begin{aligned} \frac{\partial v}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u v}{\partial \lambda} + \frac{\partial v^2 \cos \phi}{\partial \phi} \right) + \frac{\partial w v}{\partial z} = \\ - \left( f + \frac{u}{R} \tan \phi \right) u - \frac{1}{R \cos \phi} \left( \frac{1}{\rho_0} \frac{\partial q}{\partial \phi} + g \frac{\partial \eta}{\partial \phi} + \frac{1}{\rho_0} \frac{\partial p_A}{\partial \phi} + \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \phi} \right) + F_v \\ + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial v}{\partial z} \right) \end{aligned} \quad (\text{A1.4})$$

$$\frac{\partial w}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u w}{\partial \lambda} + \frac{\partial v w \cos \phi}{\partial \phi} \right) + \frac{\partial w^2}{\partial z} = - \frac{1}{\rho_0} \frac{\partial q}{\partial z} + F_w + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial w}{\partial z} \right) \quad (\text{A1.5})$$

The shallow water equations are given as

$$\frac{1}{R \cos \phi} \left( \frac{\partial u}{\partial \lambda} + \frac{\partial v \cos \phi}{\partial \phi} \right) + \frac{\partial w}{\partial z} = 0 \quad (\text{A1.6})$$

$$\begin{aligned} \frac{\partial u}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u^2}{\partial \lambda} + \frac{\partial v u \cos \phi}{\partial \phi} \right) + \frac{\partial w u}{\partial z} = \\ \left( f + \frac{u}{R} \tan \phi \right) v - \frac{1}{R \cos \phi} \left( g \frac{\partial \eta}{\partial \lambda} + \frac{1}{\rho_0} \frac{\partial p_A}{\partial \lambda} + \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \lambda} \right) + F_u + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial u}{\partial z} \right) \end{aligned} \quad (\text{A1.7})$$

$$\begin{aligned} \frac{\partial v}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uv}{\partial \lambda} + \frac{\partial v^2 \cos \phi}{\partial \phi} \right) + \frac{\partial wv}{\partial z} = \\ - \left( f + \frac{u}{R} \tan \phi \right) u - \frac{1}{R \cos \phi} \left( g \frac{\partial \eta}{\partial \phi} + \frac{1}{\rho_0} \frac{\partial p_A}{\partial \phi} + \frac{g}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \phi} \right) + F_v + \frac{\partial}{\partial z} \left( \nu_t^v \frac{\partial v}{\partial z} \right) \end{aligned} \quad (\text{A1.8})$$

### A.1.2 Transport equations

The transport equation for temperature and salinity are given as

$$\frac{\partial T}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uT}{\partial \lambda} + \frac{\partial vT \cos \phi}{\partial \phi} \right) + \frac{\partial wT}{\partial z} = F_t + \frac{\partial}{\partial z} \left( D_{ts}^v \frac{\partial T}{\partial z} \right) + \hat{H} \quad (\text{A1.9})$$

$$\frac{\partial S}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uS}{\partial \lambda} + \frac{\partial vS \cos \phi}{\partial \phi} \right) + \frac{\partial wS}{\partial z} = F_s + \frac{\partial}{\partial z} \left( D_{ts}^v \frac{\partial S}{\partial z} \right) \quad (\text{A1.10})$$

The transport equations for the  $k$ - $\varepsilon$  model are given as

$$\frac{\partial k}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uk}{\partial \lambda} + \frac{\partial vk \cos \phi}{\partial \phi} \right) + \frac{\partial wk}{\partial z} = F_k + \frac{\partial}{\partial z} \left( \nu_{t0}^v \frac{\partial k}{\partial z} \right) + P_k + B_k - \varepsilon \quad (\text{A1.11})$$

$$\frac{\partial \varepsilon}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u\varepsilon}{\partial \lambda} + \frac{\partial v\varepsilon \cos \phi}{\partial \phi} \right) + \frac{\partial w\varepsilon}{\partial z} = F_\varepsilon + \frac{\partial}{\partial z} \left( \frac{\nu_{t0}^v}{\sigma_\varepsilon^v} \frac{\partial \varepsilon}{\partial z} \right) + P_\varepsilon + B_\varepsilon - c_{2\varepsilon} \frac{\varepsilon^2}{k} \quad (\text{A1.12})$$

The transport equations for the  $k$ - $\omega$  model are given as

$$\frac{\partial k}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uk}{\partial \lambda} + \frac{\partial vk \cos \phi}{\partial \phi} \right) + \frac{\partial wk}{\partial z} = F_k + \frac{\partial}{\partial z} \left( \frac{\nu_{t0}^v}{\sigma_k^v} \frac{\partial k}{\partial z} \right) + P_k + B_k - \beta_k \omega k \quad (\text{A1.13})$$

$$\frac{\partial \omega}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial u\omega}{\partial \lambda} + \frac{\partial v\omega \cos \phi}{\partial \phi} \right) + \frac{\partial w\omega}{\partial z} = F_\omega + \frac{\partial}{\partial z} \left( \frac{\nu_{t0}^v}{\sigma_\omega^v} \frac{\partial \omega}{\partial z} \right) + F_{\omega c} + P_\omega - \beta_\omega \omega^2 \quad (\text{A1.14})$$

The transport equation for a scalar quantity is given as

$$\frac{\partial c}{\partial t} + \frac{1}{R \cos \phi} \left( \frac{\partial uc}{\partial \lambda} + \frac{\partial vc \cos \phi}{\partial \phi} \right) + \frac{\partial wc}{\partial z} = F_c + \frac{\partial}{\partial z} \left( D_c^v \frac{\partial c}{\partial z} \right) - k_p C \quad (\text{A1.15})$$

## A.2 Governing equations in spherical coordinate system and sigma coordinates

### A.2.1 Flow equations

The Navier-Stokes equations are given as

$$\frac{\partial h}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial hu}{\partial \lambda'} + \frac{\partial hv \cos \phi}{\partial \phi'} \right) + \frac{\partial w}{\partial \sigma} = 0 \quad (\text{A1.16})$$



$$\begin{aligned} \frac{\partial hu}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial hu^2}{\partial \lambda'} + \frac{\partial hv u \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega u}{\partial \sigma} = \\ \left( f + \frac{u}{R} \tan \phi \right) hv - \frac{1}{R \cos \phi} \left( \frac{h}{\rho_0} \left( \frac{\partial q}{\partial \lambda} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial \lambda} \right) + gh \frac{\partial \eta}{\partial \lambda} + \frac{h}{\rho_0} \frac{\partial p_A}{\partial \lambda} + \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \lambda} \right) \\ + h F_u + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial u}{\partial \sigma} \right) \end{aligned} \quad (A1.17)$$

$$\begin{aligned} \frac{\partial hv}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial huv}{\partial \lambda'} + \frac{\partial hv^2 \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega v}{\partial \sigma} = \\ - \left( f + \frac{u}{R} \tan \phi \right) hu - \frac{1}{R} \left( \frac{h}{\rho_0} \left( \frac{\partial q}{\partial \phi} + \frac{\partial q}{\partial \sigma} \frac{\partial \sigma}{\partial \phi} \right) + gh \frac{\partial \eta}{\partial \phi} + \frac{h}{\rho_0} \frac{\partial p_A}{\partial \phi} + \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \phi} \right) + h F_v \\ + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial v}{\partial \sigma} \right) \end{aligned} \quad (A1.18)$$

$$\begin{aligned} \frac{\partial hw}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial huw}{\partial \lambda'} + \frac{\partial hvw \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega w}{\partial \sigma} = \\ - \frac{1}{\rho_0} \frac{\partial q}{\partial \sigma} + h F_w + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial w}{\partial \sigma} \right) \end{aligned} \quad (A1.19)$$

The shallow water equations are given as

$$\frac{\partial h}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial hu}{\partial \lambda'} + \frac{\partial hv \cos \phi}{\partial \phi'} \right) + \frac{\partial \omega}{\partial \sigma} = 0 \quad (A1.20)$$

$$\frac{\partial hu}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial hu^2}{\partial \lambda'} + \frac{\partial hv u \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega u}{\partial \sigma} = \quad (A1.21)$$

$$\left( f + \frac{u}{R} \tan \phi \right) hv - \frac{1}{R \cos \phi} \left( gh \frac{\partial \eta}{\partial \lambda} + \frac{h}{\rho_0} \frac{\partial p_A}{\partial \lambda} + \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \lambda} \right) + h F_u + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial u}{\partial \sigma} \right)$$

$$\frac{\partial hv}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial huv}{\partial \lambda'} + \frac{\partial hv^2 \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega v}{\partial \sigma} = \quad (A1.22)$$

$$- \left( f + \frac{u}{R} \tan \phi \right) hu - \frac{1}{R} \left( gh \frac{\partial \eta}{\partial \phi} + \frac{h}{\rho_0} \frac{\partial p_A}{\partial \phi} + \frac{hg}{\rho_0} \int_z^\eta \frac{\partial \rho}{\partial \phi} \right) + h F_v + \frac{\partial}{\partial \sigma} \left( \frac{v_t^v}{h} \frac{\partial v}{\partial \sigma} \right)$$

The modified vertical velocity,  $\omega$ , is given by

$$\omega = \frac{1}{h} \left( w + \frac{u}{R \cos \phi} \frac{\partial d}{\partial \lambda} + \frac{v}{R} \frac{\partial d}{\partial \phi} - \sigma \left( \frac{\partial h}{\partial t} + \frac{u}{R \cos \phi} \frac{\partial h}{\partial \lambda} + \frac{v}{R} \frac{\partial h}{\partial \phi} \right) \right) \quad (A1.23)$$

## A.2.2 Transport equations

The transport equation for a temperature and salinity are given as

$$\frac{\partial hT}{\partial t'} + \frac{1}{R \cos \phi} \left( \frac{\partial huT}{\partial \lambda'} + \frac{\partial hvT \cos \phi}{\partial \phi'} \right) + \frac{\partial h \omega T}{\partial \sigma} = h F_t + \frac{\partial}{\partial \sigma} \left( \frac{D_{ts}^v}{h} \frac{\partial T}{\partial \sigma} \right) + h \hat{H} \quad (A1.24)$$

$$\frac{\partial hS}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial huS}{\partial \lambda'} + \frac{\partial hvS\cos\phi}{\partial \phi'} \right) + \frac{\partial h\omega S}{\partial \sigma} = hF_s + \frac{\partial}{\partial \sigma} \left( \frac{D_{ts}^v}{h} \frac{\partial S}{\partial \sigma} \right) \quad (\text{A1.25})$$

The transport equations for the  $k$ - $\epsilon$  model are given as

$$\begin{aligned} \frac{\partial hk}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial huk}{\partial \lambda'} + \frac{\partial hvk\cos\phi}{\partial \phi'} \right) + \frac{\partial h\omega k}{\partial \sigma} \\ = hF_k + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \right) + h(P_k + B_k - \epsilon) \end{aligned} \quad (\text{A1.26})$$

$$\begin{aligned} \frac{\partial h\epsilon}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial hu\epsilon}{\partial \lambda'} + \frac{\partial hv\epsilon\cos\phi}{\partial \phi'} \right) + \frac{\partial h\omega\epsilon}{\partial \sigma} \\ = hF_\epsilon + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_\epsilon^v} \frac{\partial \epsilon}{\partial \sigma} \right) + h \left( P_\epsilon + B_\epsilon - c_{2\epsilon} \frac{\epsilon^2}{k} \right) \end{aligned} \quad (\text{A1.27})$$

The transport equations for the  $k$ - $\omega$  model are given as

$$\begin{aligned} \frac{\partial hk}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial huk}{\partial \lambda'} + \frac{\partial hvk\cos\phi}{\partial \phi'} \right) + \frac{\partial hw_s k}{\partial \sigma} \\ = hF_k + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_k^v} \frac{\partial k}{\partial \sigma} \right) + h(P_k + B_k - \beta_k \omega k) \end{aligned} \quad (\text{A1.28})$$

$$\begin{aligned} \frac{\partial h\omega}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial hu\omega}{\partial \lambda'} + \frac{\partial hv\omega\cos\phi}{\partial \phi'} \right) + \frac{\partial hw_s \omega}{\partial \sigma} \\ = hF_\omega + \frac{\partial}{\partial \sigma} \left( \frac{v_{t0}^v}{h\sigma_\omega^v} \frac{\partial \omega}{\partial \sigma} \right) + hF_{\omega c} + h(P_\omega - \beta_\omega \omega^2) \end{aligned} \quad (\text{A1.29})$$

Note that in eqs. (A1.28)-(A1.29), the modified vertical velocity in the sigma coordinate system is called  $w_s$  (instead of  $\omega$ ). This is to distinguish it from the specific dissipation rate,  $\omega$ , of turbulent kinetic energy which was introduced in section 2.1.4.

The transport equation for a scalar quantity is given as

$$\frac{\partial hc}{\partial t'} + \frac{1}{R\cos\phi} \left( \frac{\partial huc}{\partial \lambda'} + \frac{\partial hvcc\cos\phi}{\partial \phi'} \right) + \frac{\partial h\omega c}{\partial \sigma} = hF_c + \frac{\partial}{\partial \sigma} \left( \frac{D_c^v}{h} \frac{\partial c}{\partial \sigma} \right) - hk_p C \quad (\text{A1.30})$$